

CFD models and predictions for hydrogen fire hazards

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European Hydrogen Safety Panel (EHSP)
Clean Hydrogen JU Webinar "Computational Fluid Dynamics (CFD)
for hydrogen safety analysis" 07 December 2022



In-house CFD codes for hydrogen fire and explosion hazards

HyFOAM

Modified from open source
CFD code OpenFOAM for:

- Research
- Consultancy
- Fee paying development for sponsors

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- Predictive tools for LOC scenarios of gaseous hydrogen (GH₂) during transportation
 - Hydrogen spontaneous ignition
 - **Hydrogen jet fires**
 - Hydrogen deflagrations
- Predictive tools for LOC scenarios of liquid hydrogen (LH₂) during transportation
 - LH₂ vapour cloud from sudden catastrophic release
 - LH₂ vapour cloud from jet release
 - Hydrogen jet fires at cryogenic conditions
 - Vapour cloud explosions (VCE)

Hydrogen jet fires – model outline(1/2)

- HyFOAM code with own modified eddy dissipation concept (EDC) for fires (Chen et al. 2014)
- Finite volume discrete ordinates model (fvDOM)
- Weighted sum of grey gas model for radiation

$$\epsilon = \sum_{i=0}^I a_{\epsilon,i}(T)(1 - e^{-\kappa_i ps})$$

$$a_{\epsilon,i} = \sum_{j=1}^J b_{\epsilon,i,j} T^{j-1}$$

Coefficients for emissivity					
i	κ_i	$b_{\epsilon,i,1} \cdot 10^1$	$b_{\epsilon,i,2} \cdot 10^4$	$b_{\epsilon,i,3} \cdot 10^7$	$b_{\epsilon,i,4} \cdot 10^{11}$
Carbon dioxide, $P_c \rightarrow 0$ atm					
1	0.3966	0.4334	2.620	-1.560	2.565
2	15.64	-0.4814	2.822	-1.794	3.274
3	394.3	0.5492	0.1087	-0.3500	0.9123
Water vapor, $P_w \rightarrow 0$ atm					
1	0.4098	5.977	-5.119	3.042	-5.564
2	6.325	0.5677	3.333	-1.967	2.718
3	120.5	1.800	-2.334	1.008	-1.454
Water vapor, $P_w = 1.0$ atm					
1	0.4496	6.324	-8.358	6.135	-13.03
2	7.113	-0.2016	7.145	-5.212	9.868
3	119.7	3.500	-5.040	2.425	-3.888
Mixture, $P_w/P_c = 1$					
1	0.4303	5.150	-2.303	0.9779	-1.494
2	7.055	0.7749	3.399	-2.297	3.770
3	178.1	1.907	-1.824	0.5608	-0.5122
Mixture, $P_w/P_c = 2$					
1	0.4201	6.508	-5.551	3.029	-5.353
2	6.516	-0.2504	6.112	-3.882	6.528
3	131.9	2.718	-3.118	1.221	-1.612

$P_T = 1$ atm, $0.001 \leq ps \leq 10.0$ atm-m, $600 \leq T \leq 2400$ K

Zhibin Chen, Jennifer Wen, Baopeng Xu, Siaka Dembele, Large eddy simulation of a medium-scale methanol pool fire using the extended eddy dissipation concept, *International Journal of Heat and Mass Transfer*, Volume 70, March 2014, Pages 389-408.

Zhibin Chen, Jennifer Wen, Baopeng Xu, Siaka Dembele, Extension of the eddy dissipation concept and smoke point soot model to the LES frame for fire simulations, *Fire Safety Journal*, Volume 64, February 2014, Pages 12-26.

Hydrogen jet fires – model outline(2/2)

Modelling approach

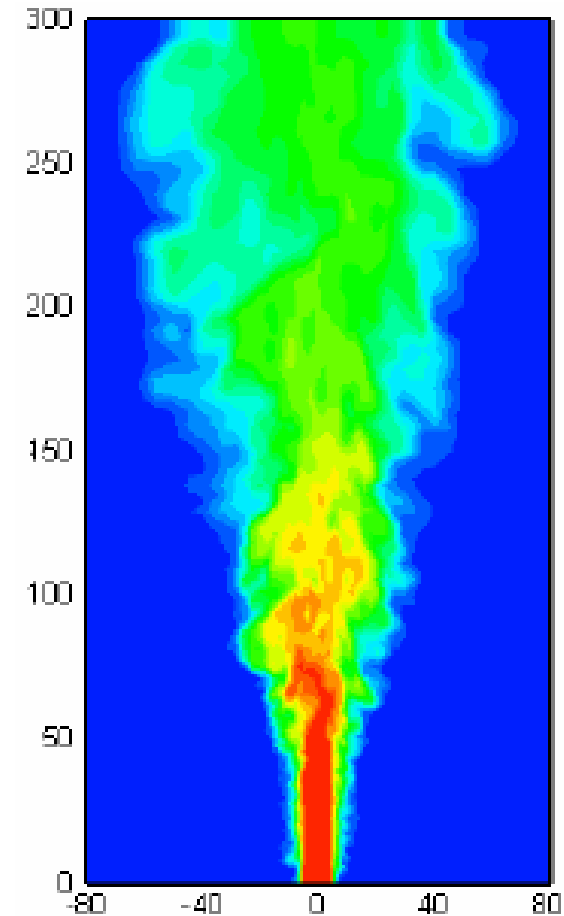
- Pseudo-source approach (Ewan and Modie 1985)
- Leak modelled from downstream as a sonic jet with the same mass flow rate

$$D_{eq} = D_j (0.536 C_D \frac{P_o}{P_a})^{0.5}$$

$$P_e = P_o \left(\frac{2}{\gamma + 1} \right)^{\gamma / \gamma - 1}$$

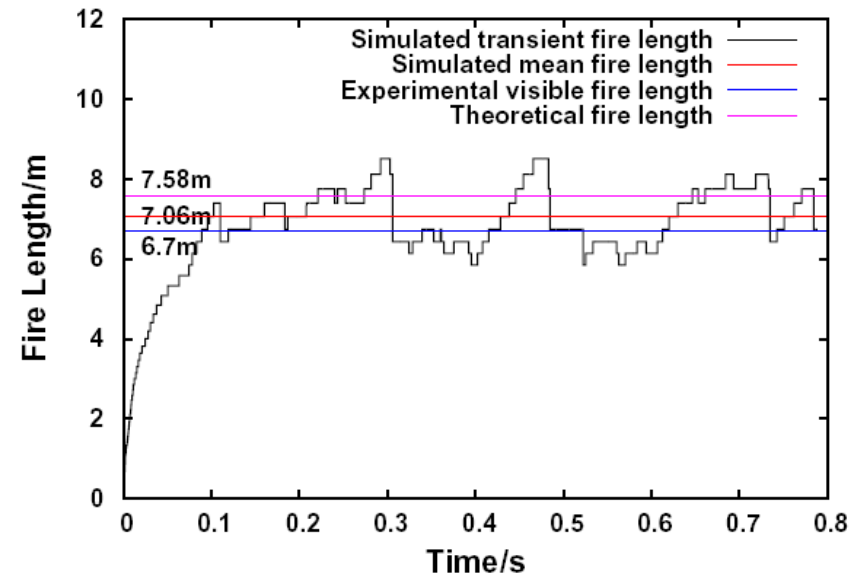
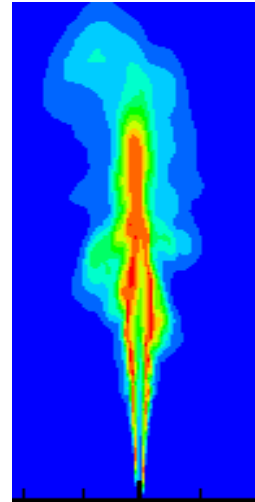
$$\rho_e = \rho_o \left(\frac{2}{\gamma + 1} \right)^{\gamma / \gamma - 1}$$

$$Y_o = \frac{4.99 D_s}{z} \left(\frac{\rho_g}{\rho_a} \right)^{1/2} C_D^{1/2}$$



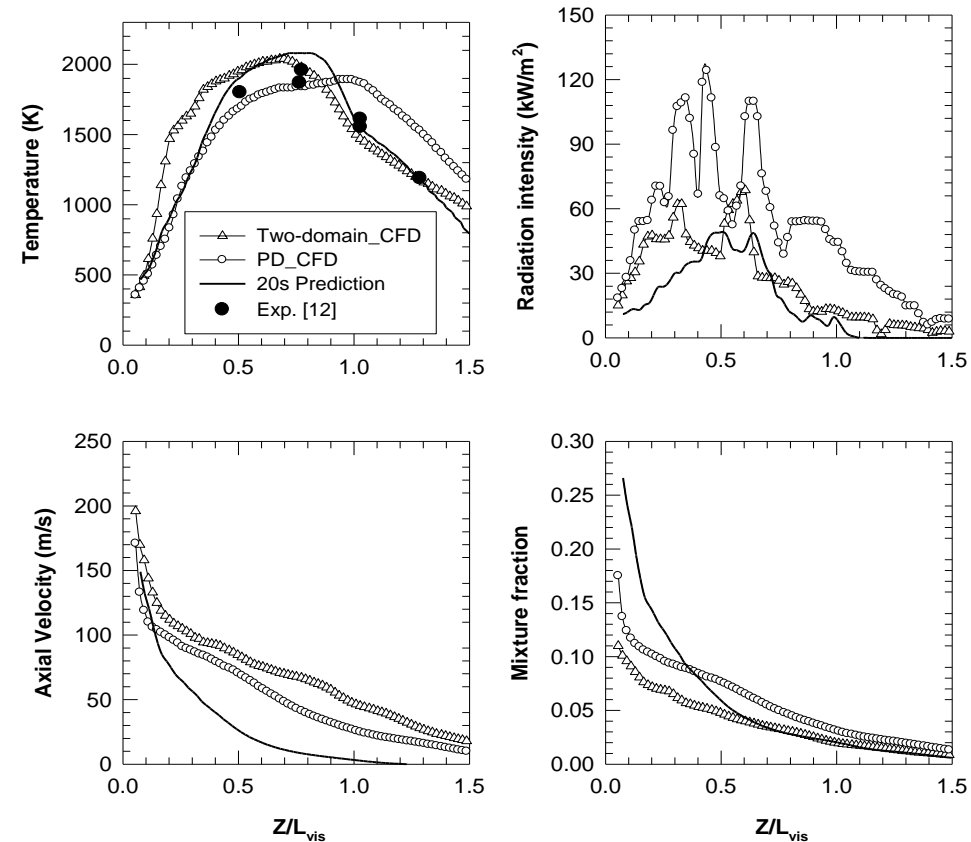
Hydrogen jet fires – validation (1/3)

Nozzle Diameter: 5.08mm
 Pressure: 104.8atm
 Tank temperature: 231.4K



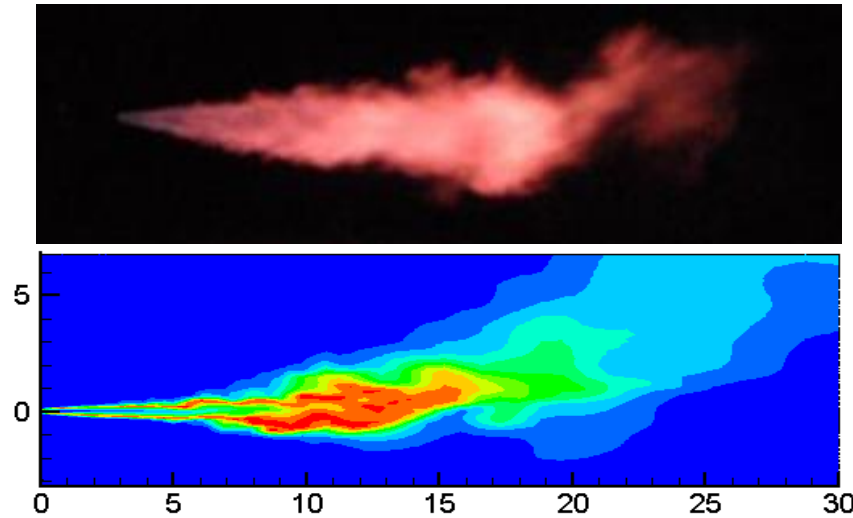
Wang, C. J., Wen, Jennifer X., Chen, Z. B. and Dembele, S. (2014) Predicting radiative characteristics of hydrogen and hydrogen/methane jet fires using FireFOAM, *Int. J of Hydrogen Energy*, 39 (35).
 Schefer, R.W., Houf, W.G., Williams, T.C., Bourne B. and Colton, J., *Characterization of High-pressure, Underexpanded Hydrogen-jet Flames*, *Int. J of Hydrogen Energy*, 32, 2007.

Simulated (m)	Experimental (m)	Theoretical (m)	Error between Simulated and Experimental values	Error between Simulated and Theoretical values
7.06	6.7	7.58	+5.4%	-6.9%

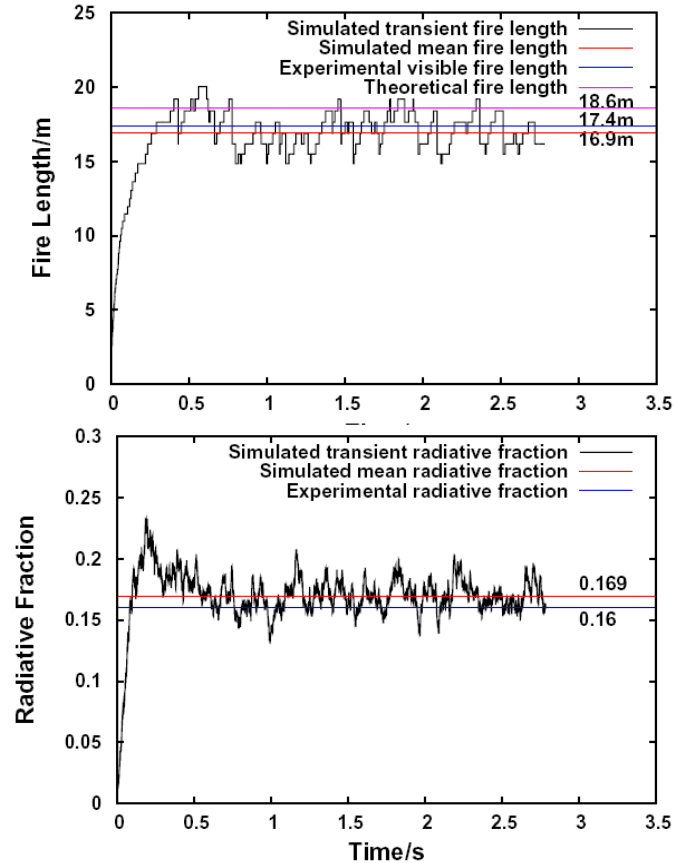


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Hydrogen jet fires – validation (3/3)



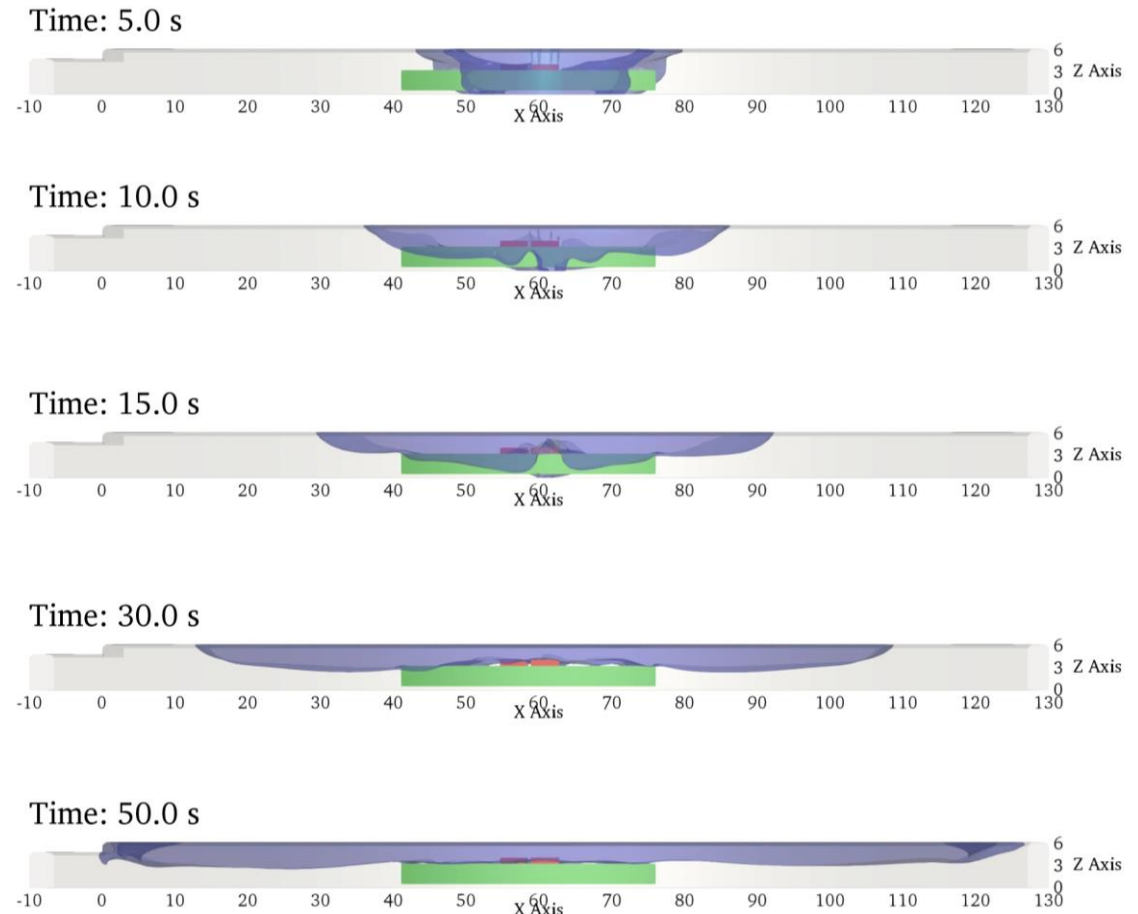
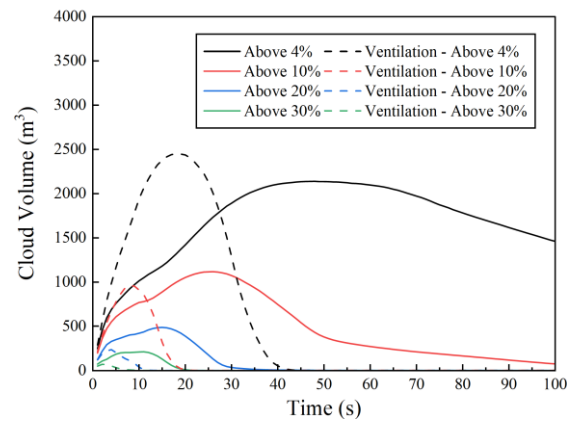
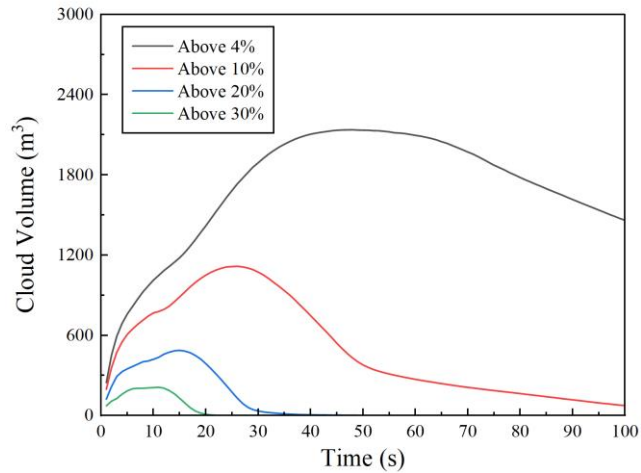
Jet	d_j [mm]	\dot{m} [kg/s]	p_0 [barg]	T_0 [K]	RH [%]	T_{amb} [K]	p_{amb} [mbar]	u_{wind} [m/s]	ϕ_{wind} [°]	L_{vis} [m]
1	20.9	1.0	59.8	308.7	94.3	280	1022	2.84	68.5	17.4



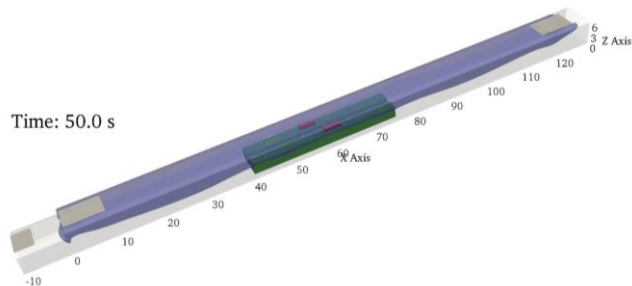
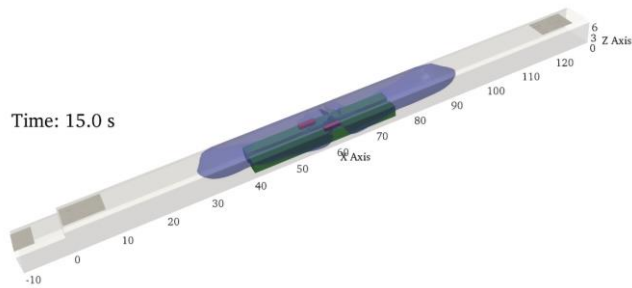
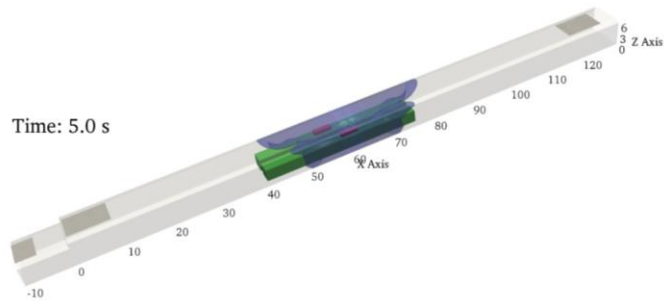
Wang, C. J., Wen, Jennifer X., Chen, Z. B. and Dembele, S. (2014) Predicting radiative characteristics of hydrogen and hydrogen/methane jet fires using FireFOAM, *Int. J of Hydrogen Energy*, 39 (35).
 Ekoto, I.W., Houf, W.G., Ruggles A.J., Creitz, L.W. and Li, J.X. (2012) Large-scale Hydrogen Jet Flame Radiant Fraction Measurements and Modelling, *Proc. 9th Int. Pipeline Conference*, Calgary, Alberta, Canada, Paper IPC2012-90535.

Dispersion simulation in preparation for modelling multiple hydrogen jet fires in a tunnel (1/5)

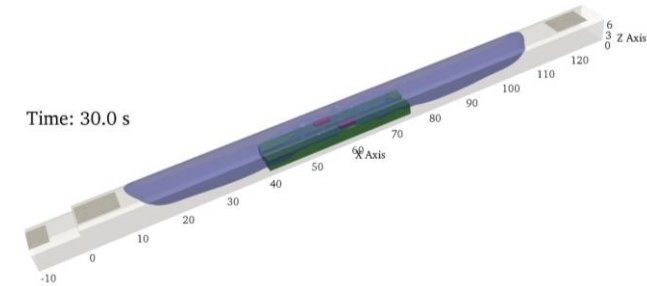
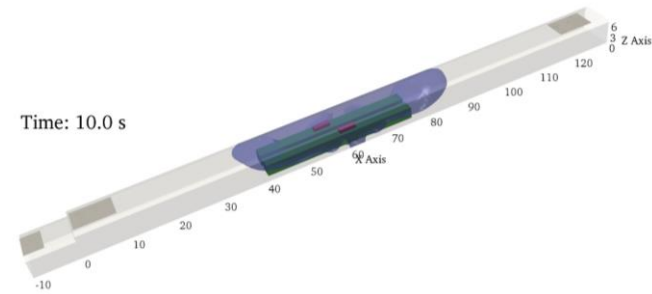
Cloud (above 4% - view 1)



Dispersion simulation in preparation for modelling multiple hydrogen jet fires in a tunnel (2/2)



Cloud (Above 4%) - view 2

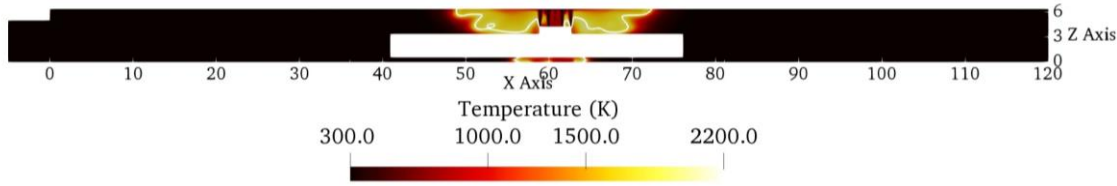


Multiple hydrogen jet fires in a tunnel (1/4)

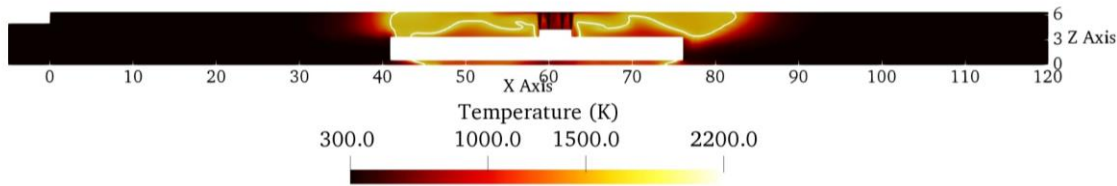
Temperature (1)

4% H₂ concentration

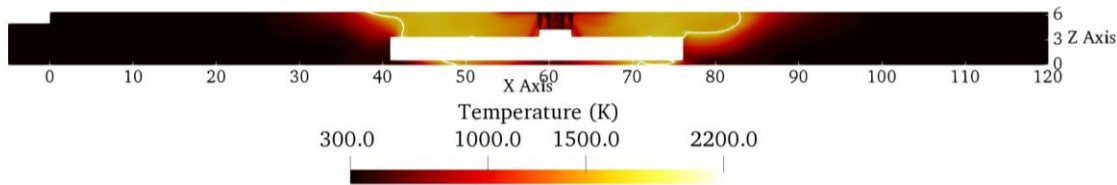
Time: 0.5 s



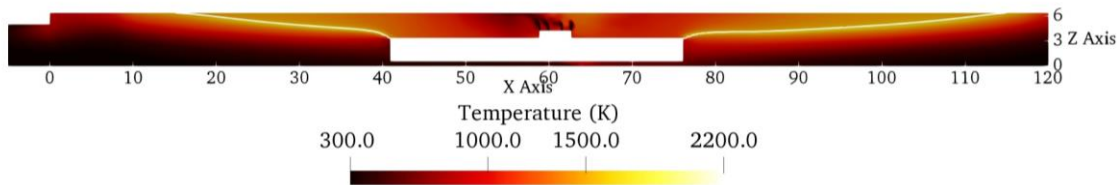
Time: 1.5 s



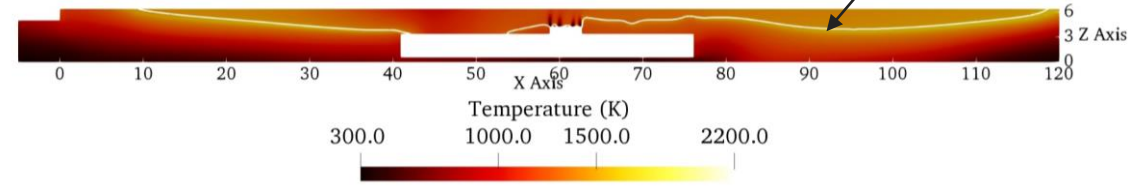
Time: 3.0 s



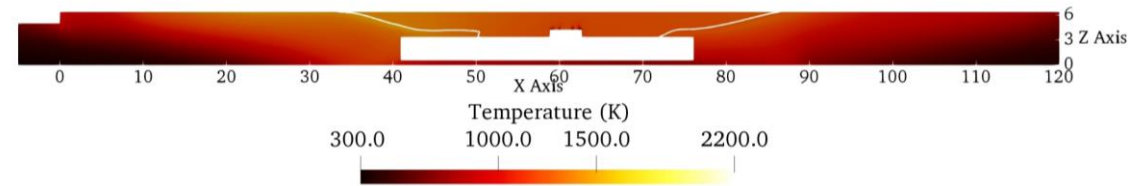
Time: 9.0 s



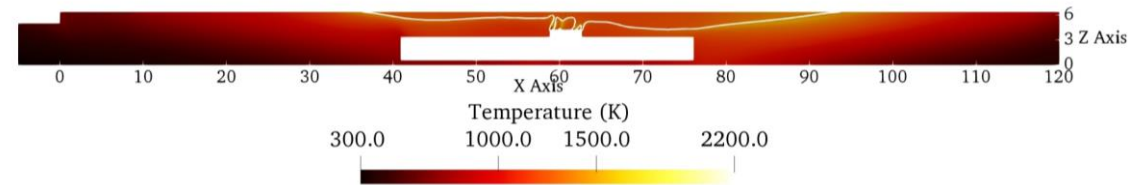
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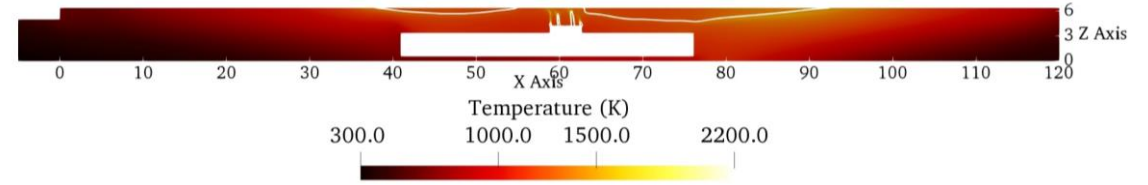
Time: 30.0 s



Time: 46.0 s

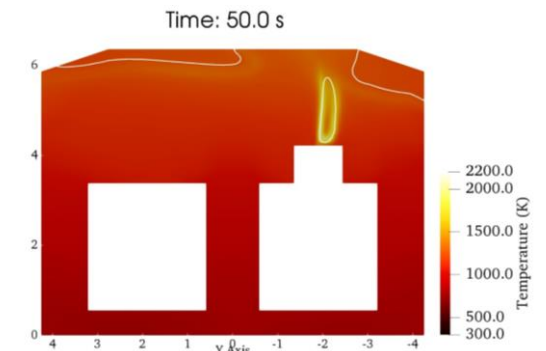
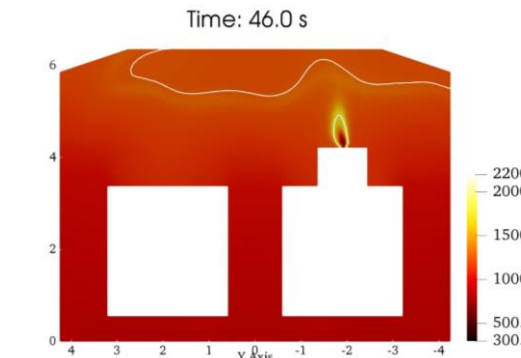
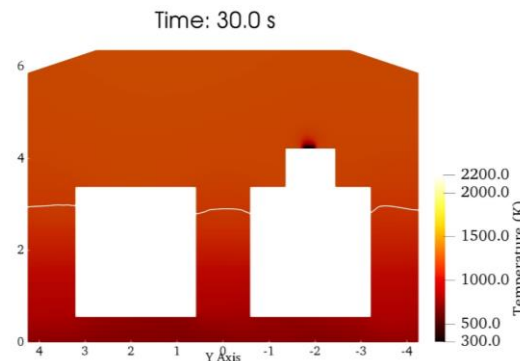
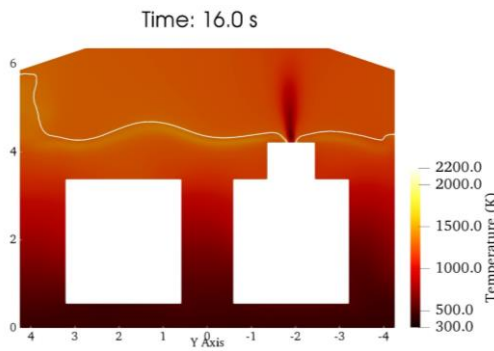
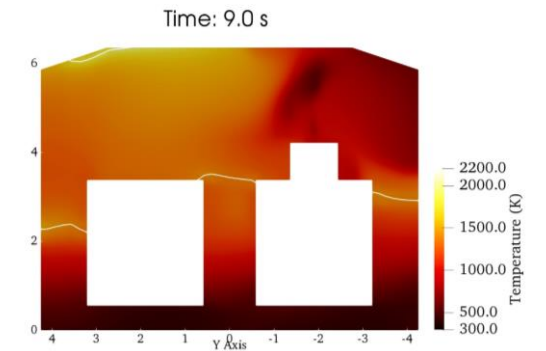
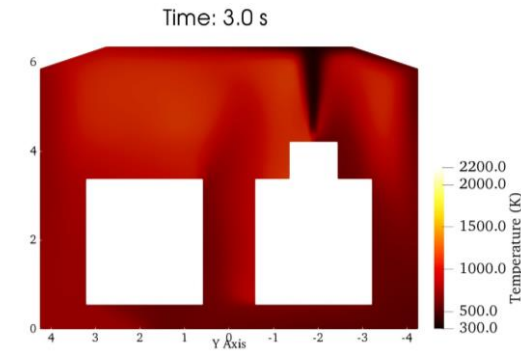
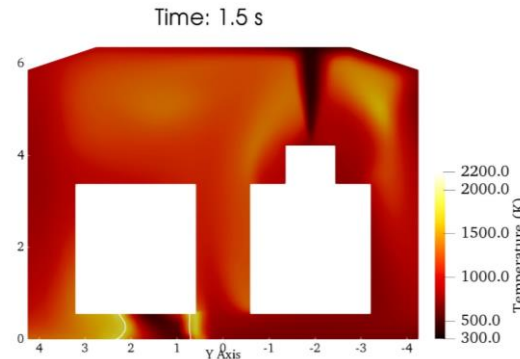
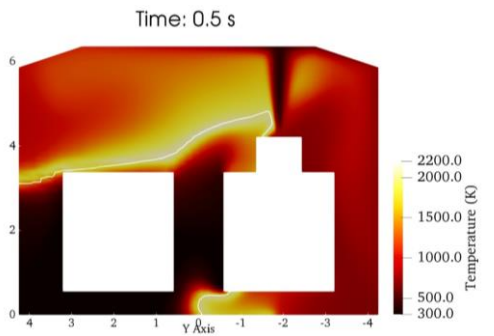
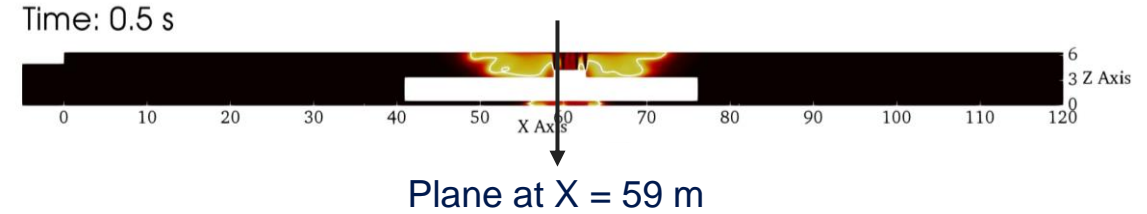


Time: 50.0 s



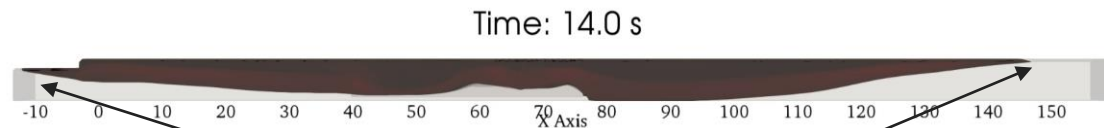
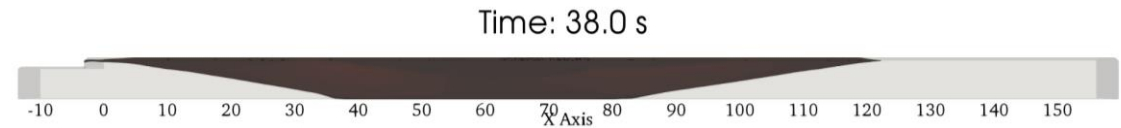
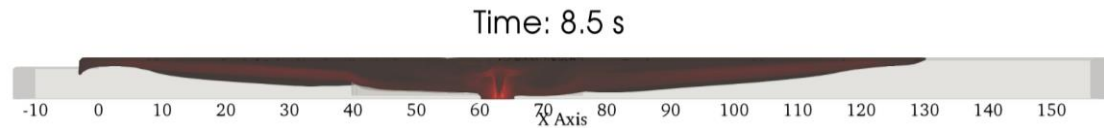
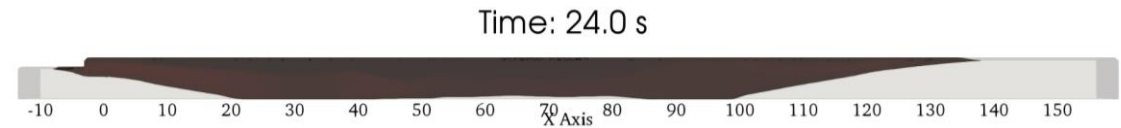
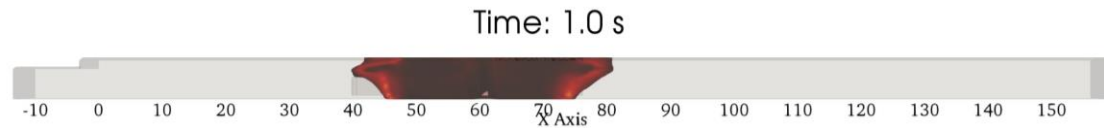
Multiple hydrogen jet fires in a tunnel (2/4)

Temperature (2)



Multiple hydrogen jet fires in a tunnel (3/4)

Cloud above 900 K

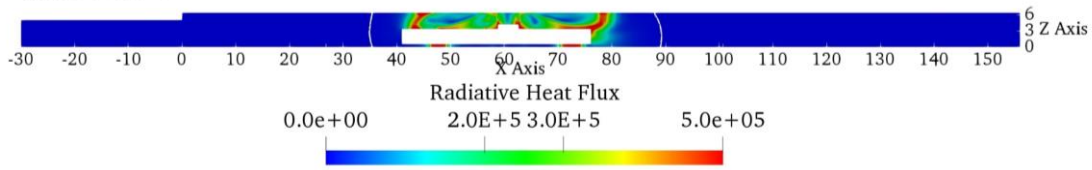


Furthest extent of 900 K

Multiple hydrogen jet fires in a tunnel (4/4)

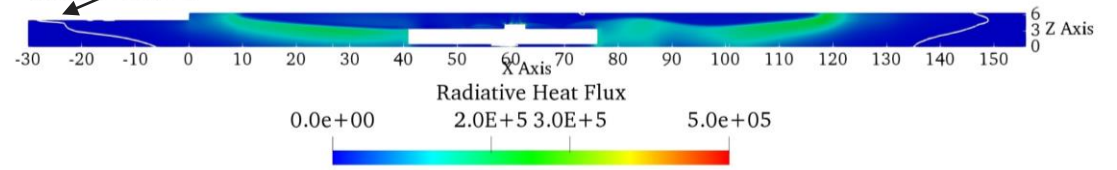
Radiative heat flux

Time: 1.0 s



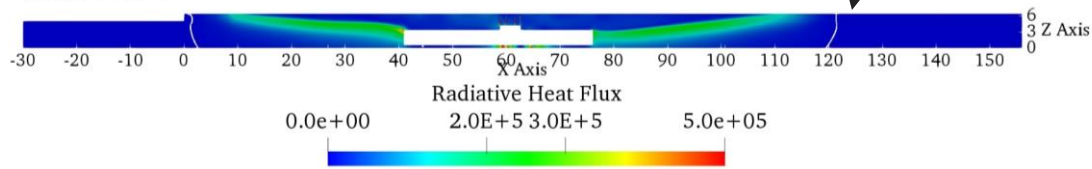
Far left of 2000 W/m²

Time: 18.0 s

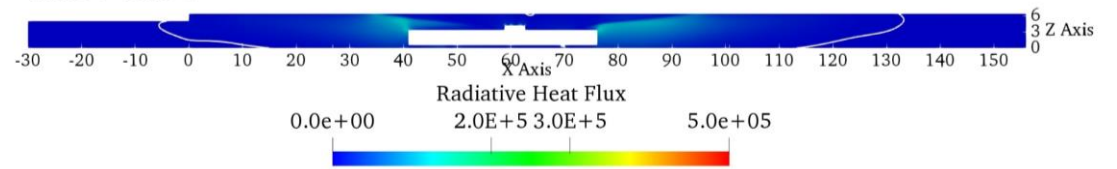


2000 W/m²

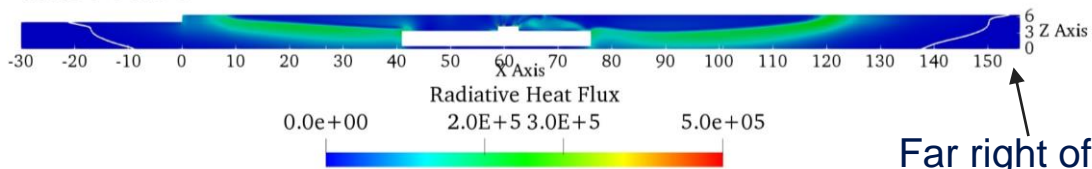
Time: 7.0 s



Time: 40.0 s

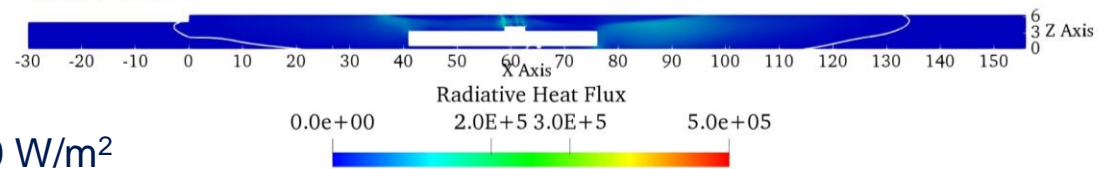


Time: 14.0 s



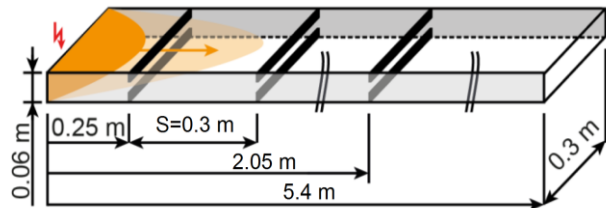
Far right of 2000 W/m²

Time: 50.0 s



Hydrogen flame acceleration and deflagration to detonation transition (DDT)

Numerical Schlieren



Time: 0.006950 sec

Temperature (K)



Time: 0.006950 sec

Pressure (pa)



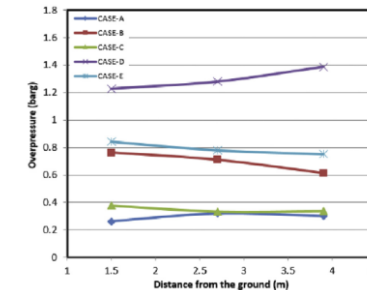
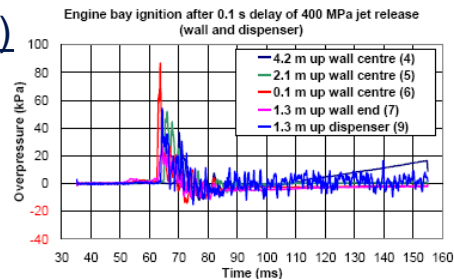
Time: 0.006950 sec

X=0.55m

X=0.85m

X=1.15m

Hydrogen explosions



DDT in a full scale tunnel (423.9 m³)

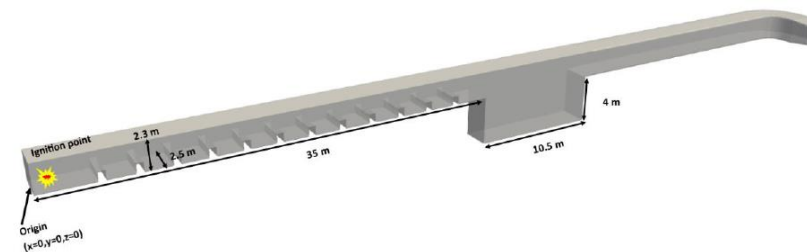
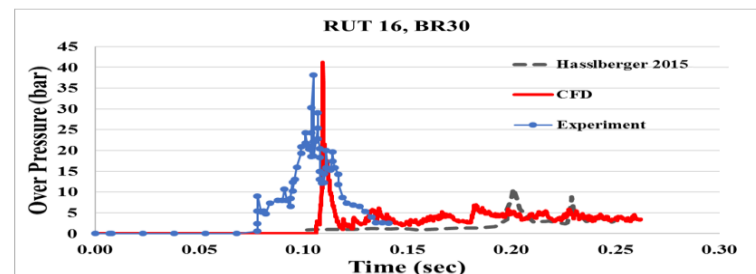


Figure 7-2: RUT 16 geometry configuration; 30% blockage ratio.



HyFOAM

Modified from open source
CFD code OpenFOAM for:

- Research
- Consultancy
- Fee paying development
for sponsors

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