# **Hydrogen Research & Innovation Days** 24-25 November 2025





DESIGN, LABORATORY CHARACTERIZATION, ACCEPTANCE TESTS, COMMISSIONING AND START-UP OF A 2.6 MW HIGH TEMPERATURE STEAM ELECTROLYSIS SYSTEM IN A REFINERY

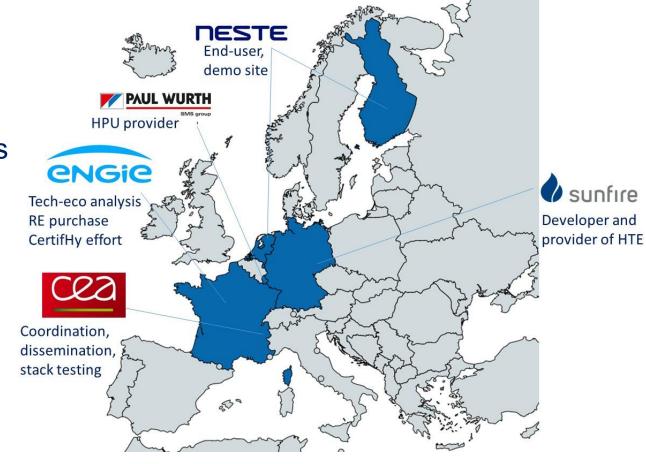




## MULTIPLHY project at a glance



- EU funded project
  - Call FCH-02-2-2019: Multi megawatt hightemperature electrolyser for valorisation as energy vector in energy intensive industry
- Project start: 01/2020 ; duration: 72 months
- Partners:
  - CEA(F),
  - NESTE (FI, NL),
  - SUNFIRE (D),
  - PAUL WURTH (L),
  - ENGIE (F)



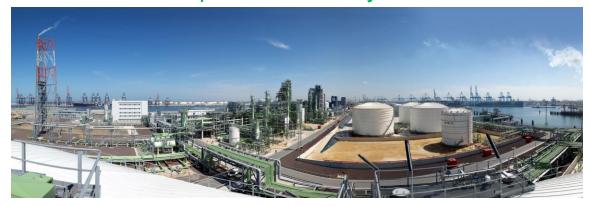


# MULTIPLHY project main objectives



#### Goal:

- Manufacturing, installation and integration of the world's first multi-MW high-T electrolyser (HTE) system
- At a renewable products refinery located in Rotterdam / The Netherlands

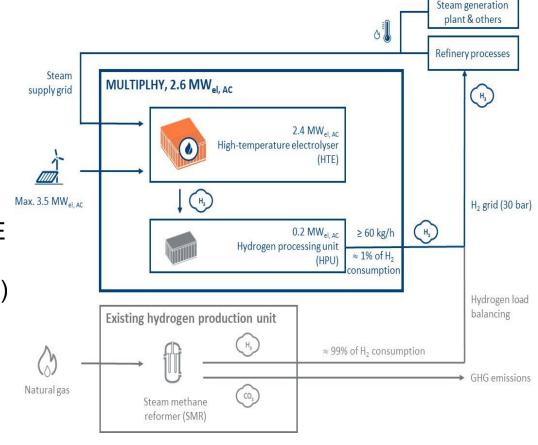


### • Key figures:

- Electrical rated nominal power of ~ 2.6 MWel,AC (HTE & Hydrogen Processing Unit (HPU))
- Hydrogen production rate of ≥ 60 kgH2/h (≥ 670 Nm³/h)

#### Technical objectives:

- Electrolyser electrical efficiency of up to 85%<sub>el,LHV</sub>
- Nominal Electricity consumption: 39 kWh/kg<sub>H2</sub>
- H<sub>2</sub> Production loss rate: ≤ 1.2% / 1000 h

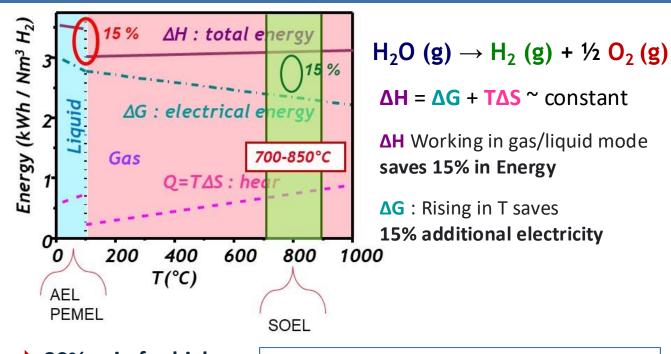




### Benefits of High T Electrolysis

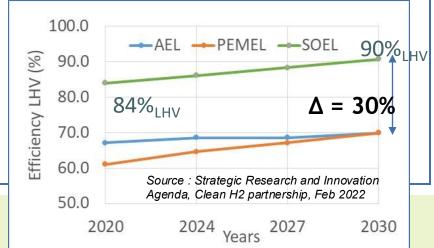


#### HIGH EFFICIENCY TECHNOLOGY

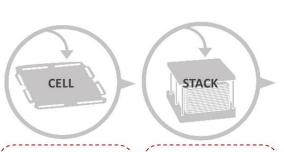


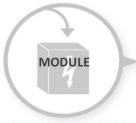
30% gain for high temperature steam electrolysis

When coupled to a heat source (~ 150°C) to produce steam



#### **MODULAR TECHNOLOGY** WITH NO NOBLE CATALYSTS







Electrolysis cell composed of

- · 2 electrodes (anode and cathode)
- One electrolyte
- · Need of electricity (and

Integration of stacks into a Stacking of several module electrolysis cells to increase the power

Can/will include several stacks into a module

Integration of modules into an electrolysis system/plant including all Balance of Plant components = electrolyser Can/will include several modules into the electrolysis system/plant



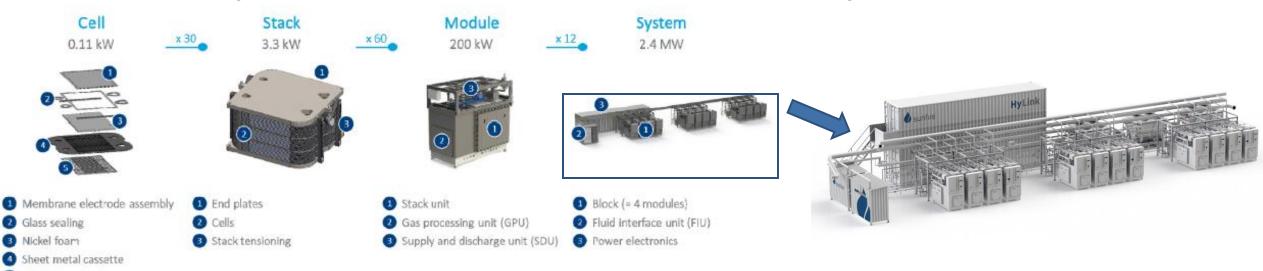


### MULTIPLHY Demonstration unit



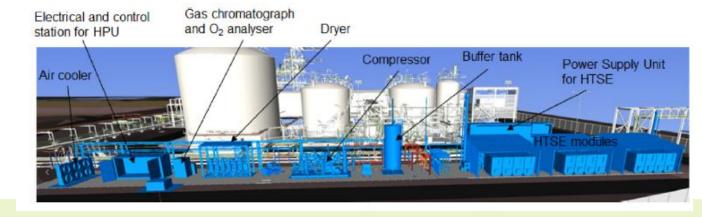
#### High temperature electrolyser (HTE):

- Large upscaling step compared to previous projects: X 17 vs GrinHy (150 kW), X 3.6 vs GrinHy 2.0 (720 kW), installed in Salzgitter steel plant
- Modular design of the HTE part: 3 blocks of 4 modules each comprising 60 stacks of 30 cells



### Hydrogen Processing Unit (HPU)

- to meet quality (at least 3.0) and pressure (30 bar) criteria of the refinery process
- Comprises several components:





Cathode contact

### Factory acceptance test



#### For each HTE module

- Cold commissioning + Leakage test+Operation test:
   rated and maximum load
- All modules passed FAT at first time → Could be shipped on site
- 65.7 Nm³/h H₂ production achieved per module
- Very homogenous temperatures and voltages in stacks
- Module efficiency :
  - above 86 % <sub>el,LHV</sub> at full load
  - up to 89 % <sub>el,LHV</sub> at part load

#### For HPU components

- Mechanical/pressure tests, leakage tests, visual inspection, coupling
- Components passed → Could be shipped on site





Electrical Module efficiency ---- H2 production flow

## Site preparation



- Civil and structural works
- Piping
- Electrical substation
- Instrumentation, automation and conti
- Safety approval
- Installation of the different elements
- Interface connections



Compressor



HTE module









### Validation steps before startup



#### HTE unit:

- Cold commissioning (N<sub>2</sub> and instrument air as media)
  - I/O checks; Purging and flushing of lines; Calibration of sensors and gas detectors
  - Equipment and group functional testing
- Start-up (H<sub>2</sub> and steam as media)
  - Leakage tests
  - Bringing power supply unit online
  - Heat up -> All modules taken from cold state to hot idling mode
  - SOEC operation -> First production of Hydrogen by modules in singular and blockwise manner

#### HPU unit:

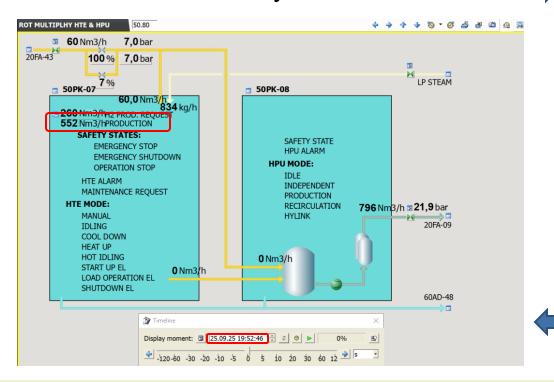
- Cold commissioning (N<sub>2</sub> as media)
  - I/O check; Equipment function tests; Group function tests
- Start-up (H2 as media)
  - Leakage test
  - Running HPU in Independent mode compressing up to 30 barg
- Coupling of Hydrogen from modules to HPU system

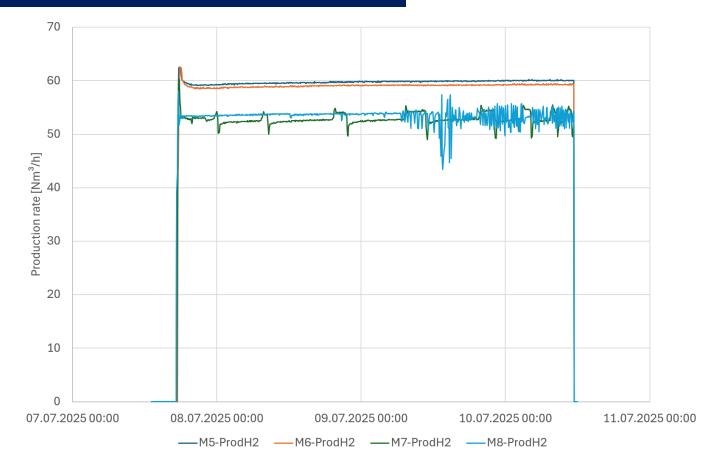


### Start-up



- HTE system capable of operation since mid 2024
- Delays due to repairs on auxiliary equipments with long lead times
- Example of 4 days of operation of block 2 in July 2025





Injection of H2 in the refinery process performed on 25 September 2025



### Long term stack tests





- Sunfire: Electrolyte supported cells (ESC)
- CEA: Cathode supported cells (CSC)

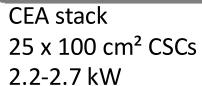
#### ■ 2 power ranges:

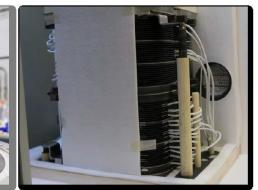
- ~ 3-6 kW
- ~ 8-19 kW

#### Harmonized test protocol:

- Performance maps at BoL and EoL
- Several steps at constant current in thermoneutral conditions
- Load point and thermal cycles
- For long term operation:
  - Fixed current density for fixed H<sub>2</sub> production: 0.65 A/cm<sup>2</sup> as ref., up to 0.9 A/cm<sup>2</sup> on latest/large stacks
  - Constant steam conversion (SC): ≥ 60%
  - Stack voltage maintained at 1.3V to reduce thermal gradients in the stack and maximize efficiency.
  - Stack T increased to compensate for the degradation and maintain the cells in (near) thermoneutral voltage







Sunfire pile of 2 stacks 2 x 30 x 128 cm<sup>2</sup> ECSs 2x2.5 kW

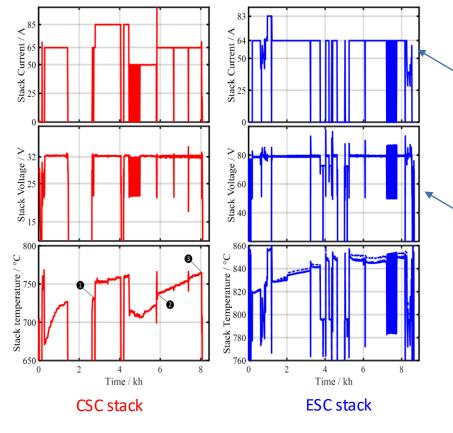


### Long term stack tests



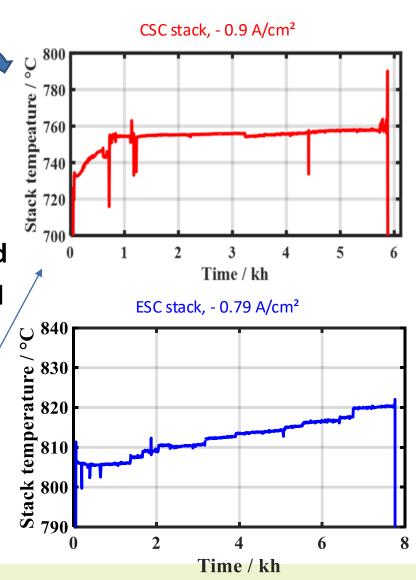


- Tests ranging between 7 and 8 kh for 3-6 kW stacks
- Tests ranging between 6 and 8 kh for 8-19 kW stacks



Constant I → No H2
 production loss over the whole duration thanks to the smart strategy adopted

- Constant U (thermoneutral voltage) → maximum efficiency and minimum thermal gradient
  - > 3 tons of H<sub>2</sub> generated by one single stack over the test duration





### Conclusion



### Largest HTE electrolyser installed in an industrial environement

- Key figures:
  - 2.6 MW<sub>el,AC</sub> (HTE and HPU)
  - Hydrogen production rate of ≥ 60 kg<sub>H2</sub>/h (≥ 670 Nm³/h)
  - electrolyser electrical efficiency of up to 86%<sub>el.LHV</sub>
  - Smart operating strategy for the stacks to avoid hydrogen production loss over the time of operation
- Successful FAT of HTE and HPU
- Site preparation
- Commissionning
- Startup completed

### Long term stack testing

- Extensive study on 2 types of stacks of 2 power ranges
- Durability evaluated over periods of up to 8000h
- Total accumulated testing time > 42000 h
- Operation at zero hydrogen production loss validated



## Acknowledgements



This project has received funding from the Fuel Cells and Hydrogen 2 Joint Undertaking (now Clean Hydrogen Partnership) under grant agreement No 875123. This Joint Undertaking receives support from the European Union's Horizon 2020 research and innovation programme, Hydrogen Europe and Hydrogen Europe research.



### Thank you for your attention

- Please visit MULTIPLHY website for latest results and publications: <a href="https://multiplhy-project.eu/">https://multiplhy-project.eu/</a>
- Read: https://doi.org/10.1016/j.ijhydene.2025.02.070



