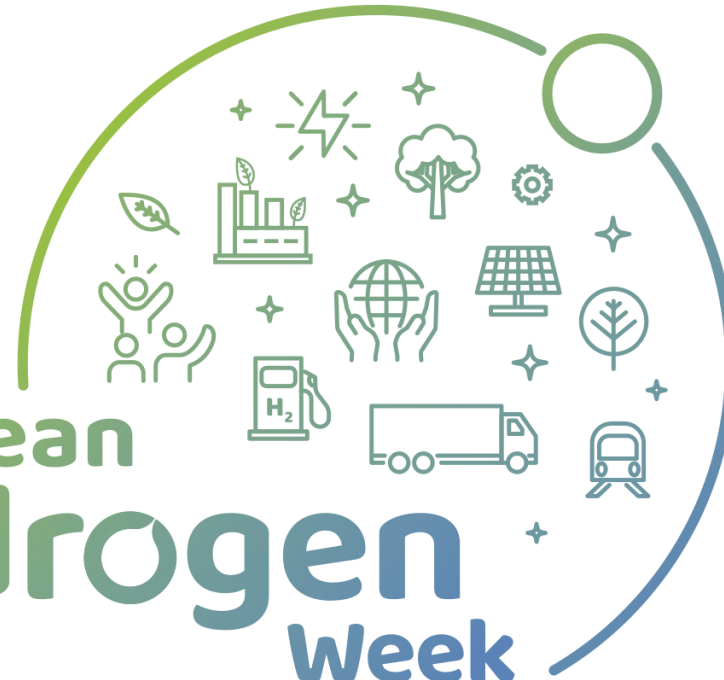


**BioRobur<sup>plus</sup>**

Advanced direct biogas fuel  
processor for robust and cost-  
effective decentralised  
hydrogen production



European  
**Hydrogen**  
Week

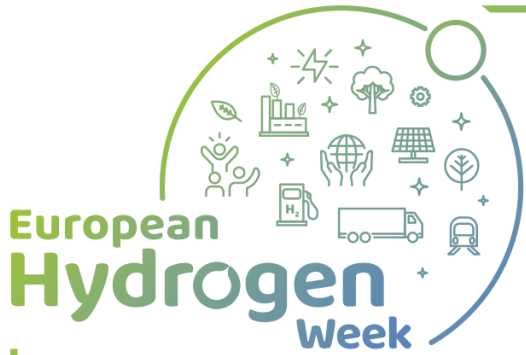


Sorani Montenegro  
Hysytech Srl

<https://www.bioroburplus.org/>  
[debora.fino@polito.it](mailto:debora.fino@polito.it)

#PRD2020  
#CleanHydrogen





# Project Overview

**Call year:** 2016

**Call topic:**

FCH-02-2-2016  
Development of compact reformers for distributed bio-hydrogen production

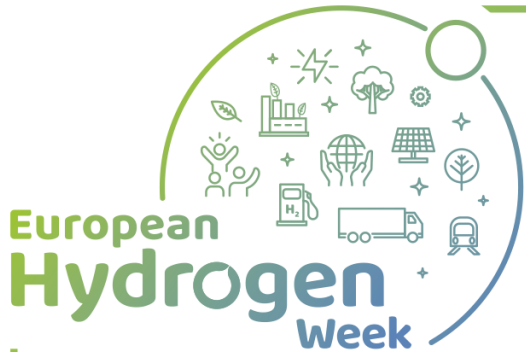
**Project dates:**  
01/01/2017 - 30/06/2021

**Total project budget:**  
3 813 536,24 €

**BioRobur<sup>plus</sup>**

**% stage of implementation**  
01/11/2019: 65 %

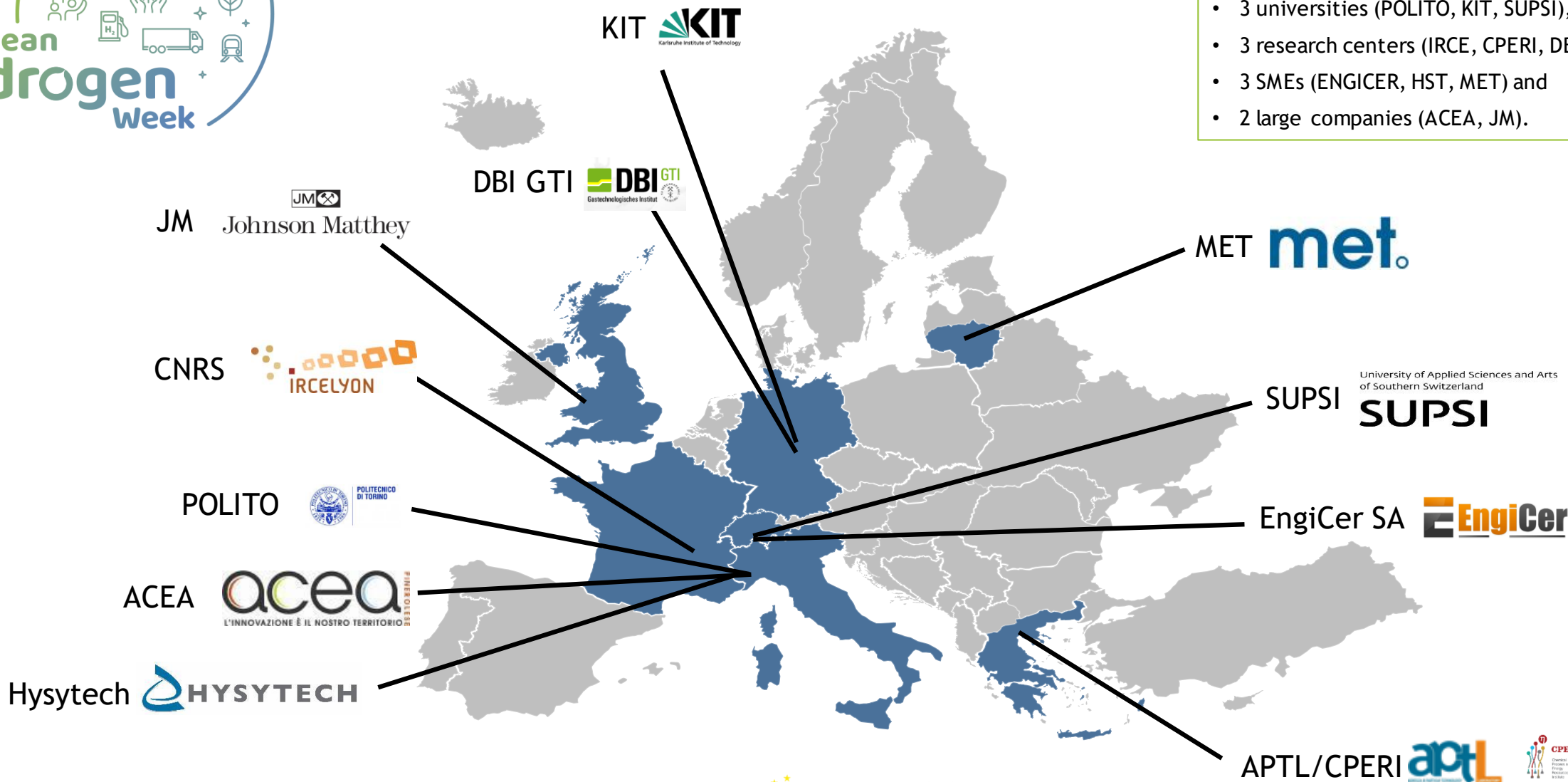
**FCH JU max. contribution:**  
2 996 248,74 €  
**Other financial contribution:**  
817 287.50 € (Swiss government)

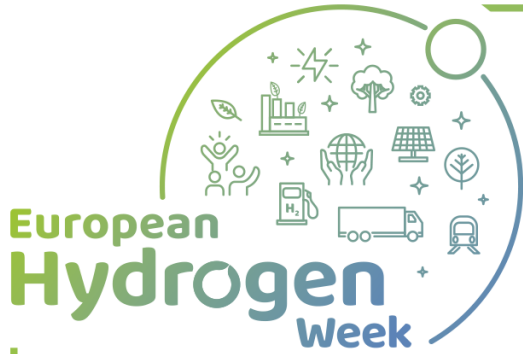


# Partners

A consortium that involves the whole society/stakeholders with complimentary expertise:

- 3 universities (POLITO, KIT, SUPSI),
- 3 research centers (IRCE, CPERI, DBI),
- 3 SMEs (ENGICER, HST, MET) and
- 2 large companies (ACEA, JM).





# Project Summary

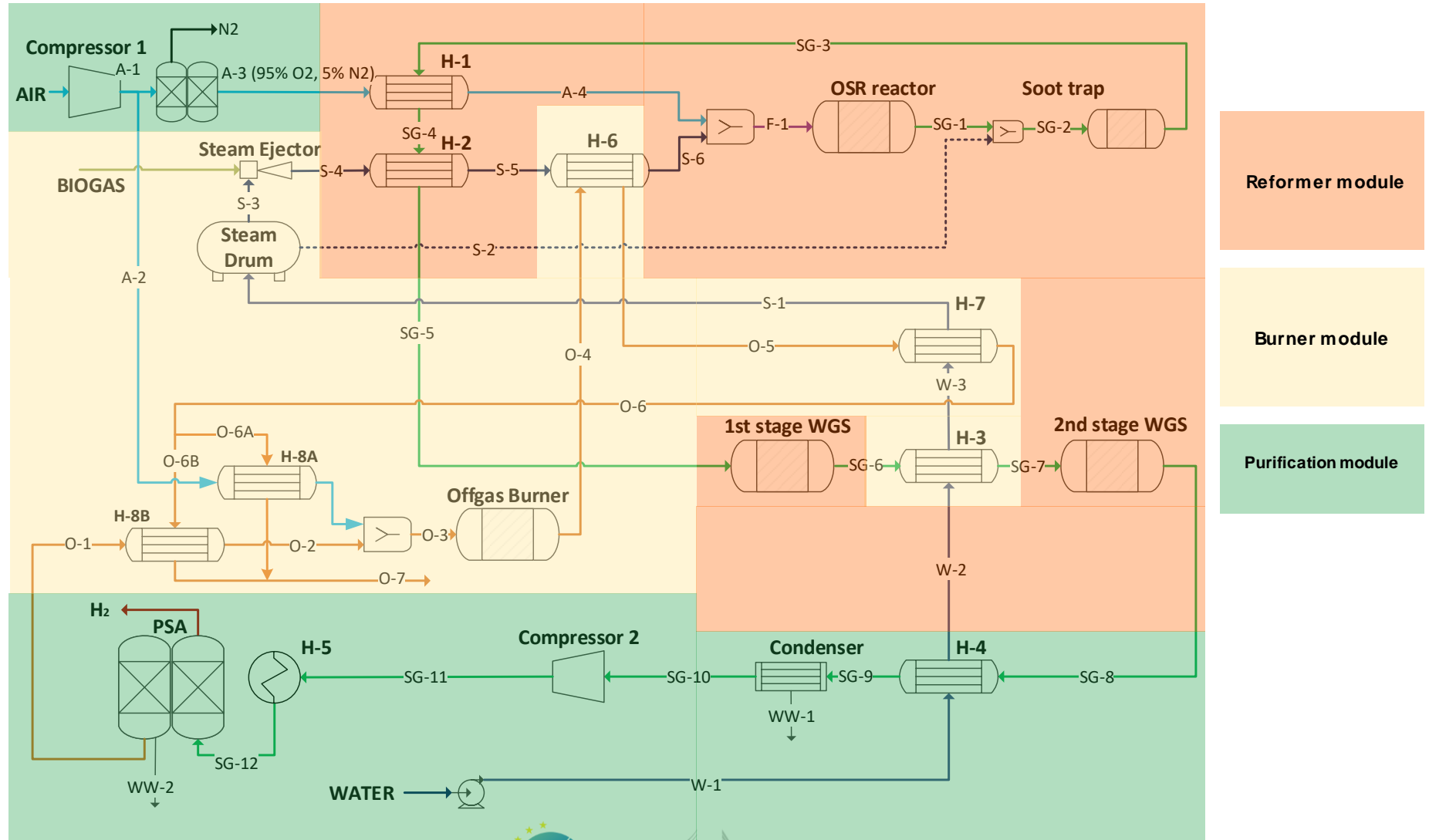
The BioRoburplus project will develop a pre-commercial oxidative steam reformer (OSR) for sustainable and **decentralized hydrogen production from biogas**. The TRL6 demo-plant will deliver at least 50 Nm<sup>3</sup>/h (107 kg/day) of H<sub>2</sub> at 99.9% purity and 1.5 bar with an energy efficiency conversion of 81% on a HHV basis.

These targets will be achieved by pursuing the following new developments and concepts:

1. A high thermal integration.
2. A tailored innovative purification system to drive H<sub>2</sub> separation from syngas.
3. A recuperative burner based on cellular ceramics capable of exploiting the low enthalpy hydrogen purification off-gas for the reformer feed preheating.
4. A robust OSR structured catalyst.

A dedicated TRL6 demo campaign will be carried out integrating the processor with an anaerobic digester plant in a real industrial site (ACEA).

# Project Summary



# Project Progress/Actions - Range/TRL

Unit under manufacturing. It has been designed to produce 50Nm<sup>3</sup>/h H<sub>2</sub> 99.9%

**Achievement to-date**

TRL3

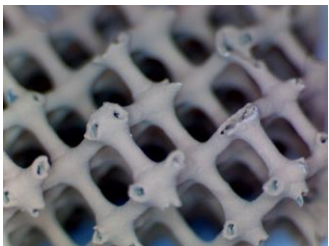


TRL6  
50Nm<sup>3</sup>/h  
99.9%

M18



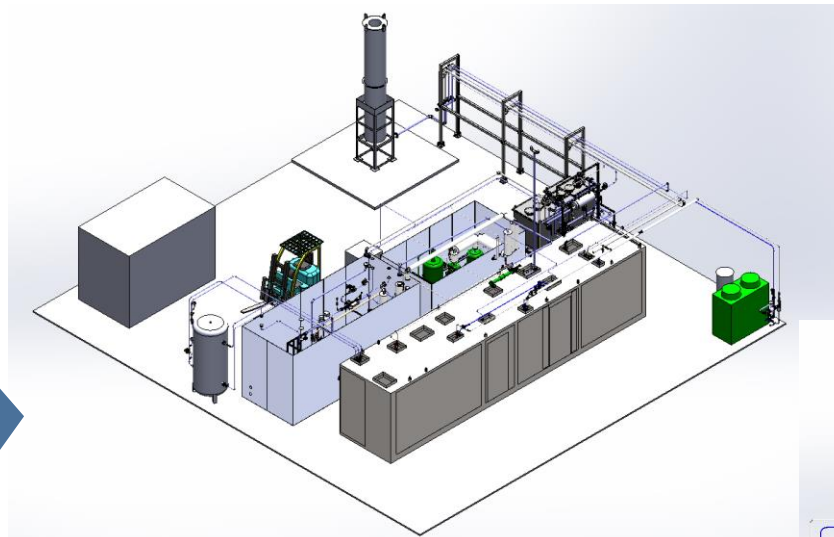
OSR Catalyst



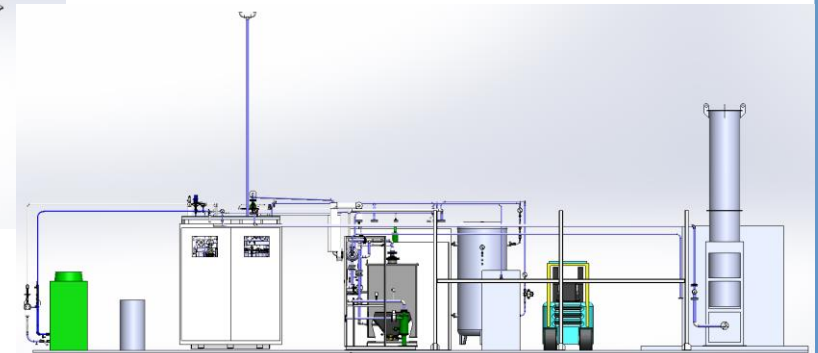
M24



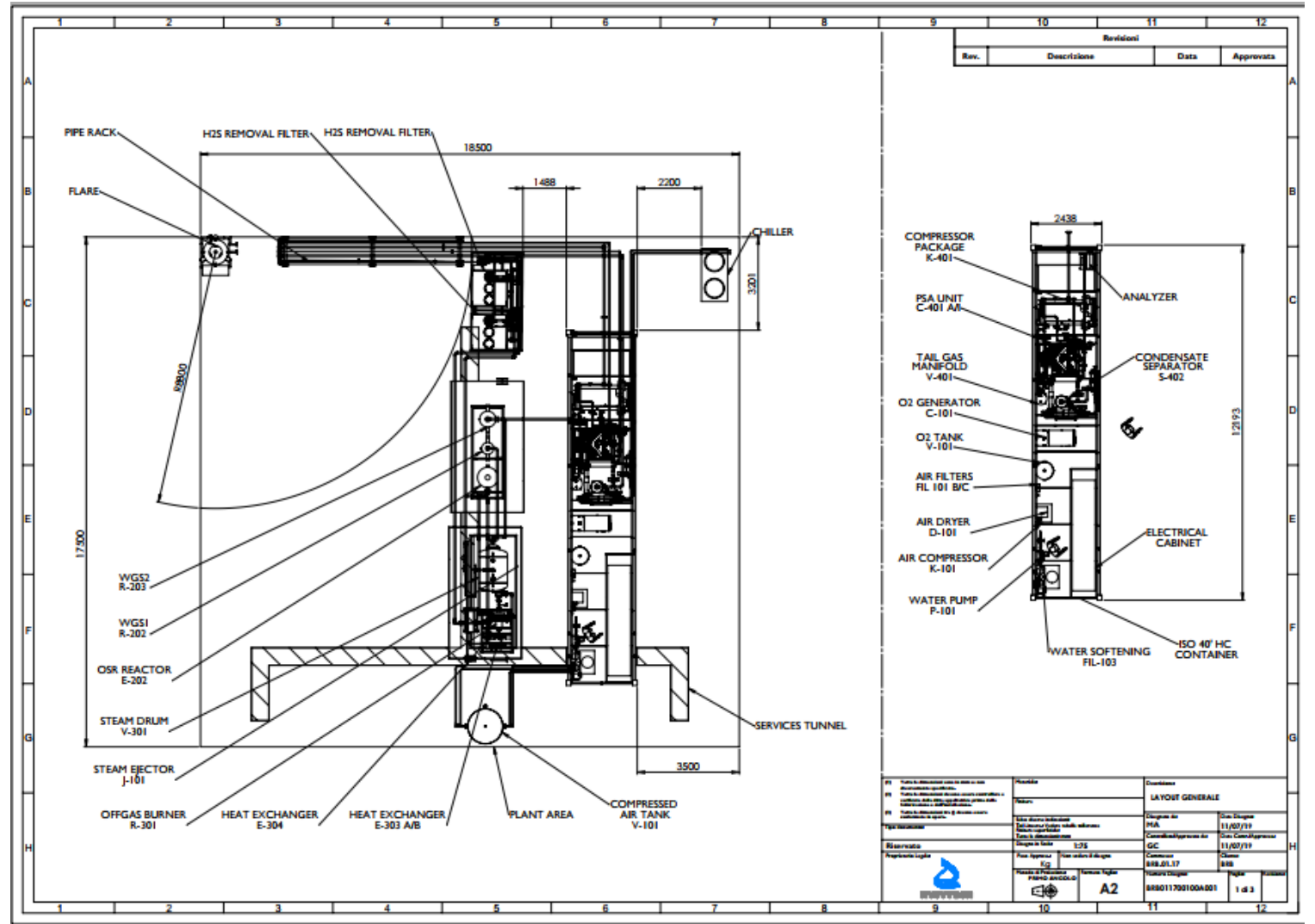
M39



M40

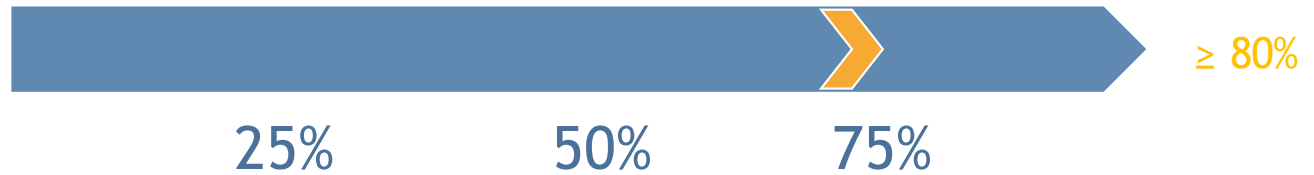


# Project Progress/Actions - Range/TRL

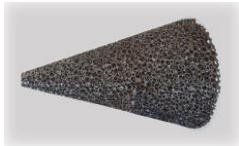


# Project Progress/Actions - Overall plant efficiency.

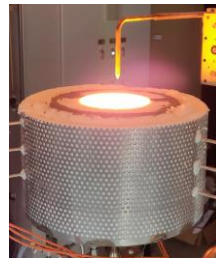
**Achievement to-date** 65%



Off-gas burner enthalpy valorisation



M24

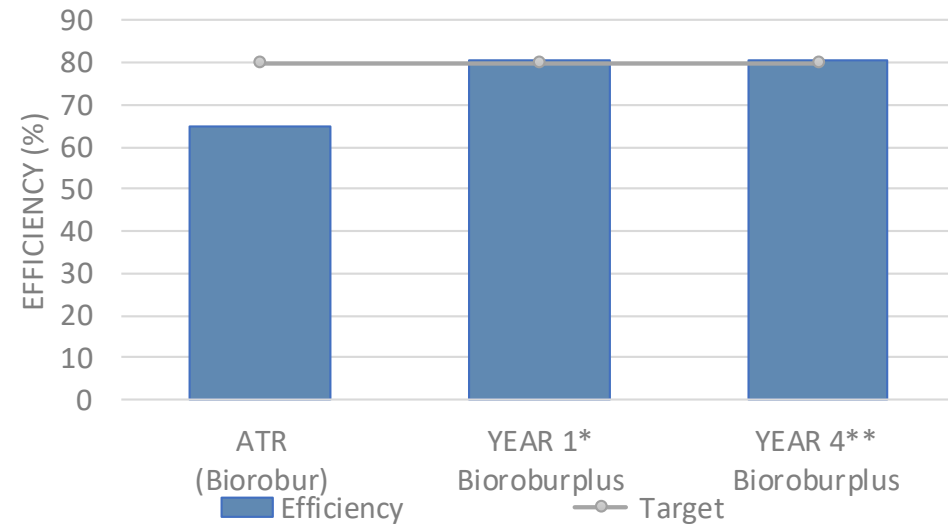


H<sub>2</sub> Purification

- Purification module efficiency: 85%,
- $\eta_{plant} = 80.7\%$
- Hydrogen Purity: 99,9%



M18





# Project Progress/Actions - Durability



Achievement to-date

250 h  
2 %

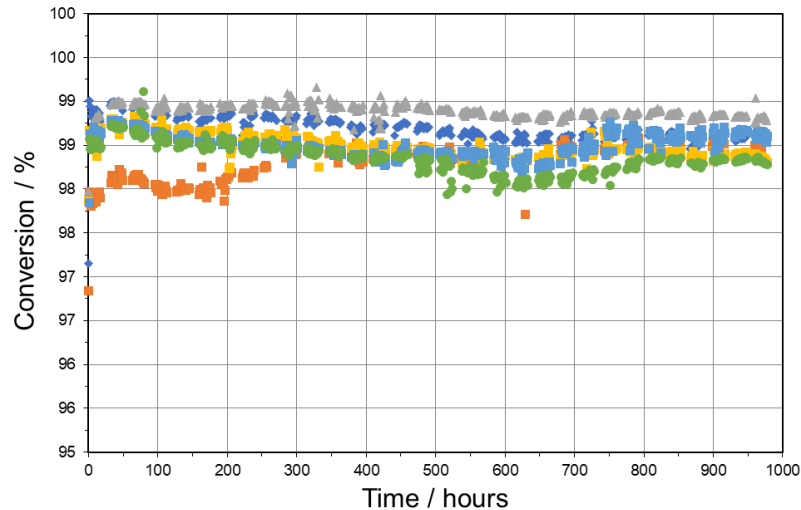


25%

50%

75%

1000h  
2 %



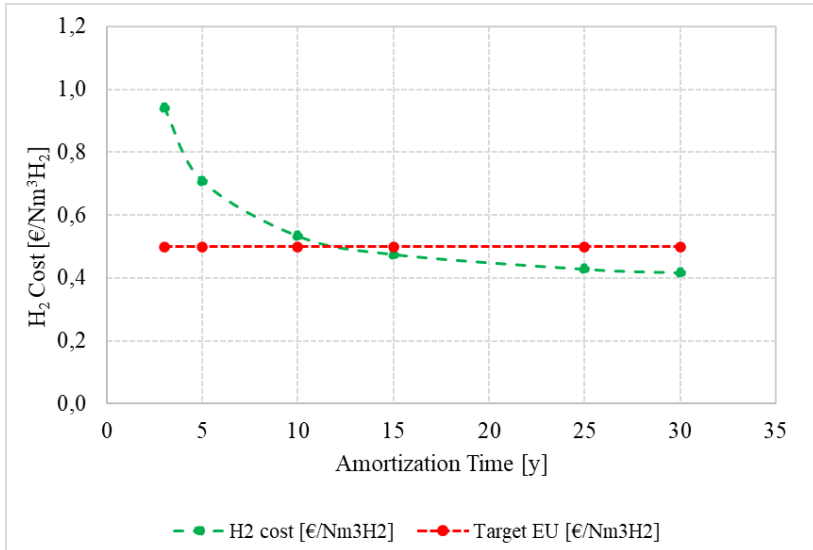
Durability - 6 Powder catalyst samples

- Catalyst activity stable over 1000 hours
- No catalyst regeneration was required
- MS2.1 reached: target is <2% deactivation over 1000 hours ✓

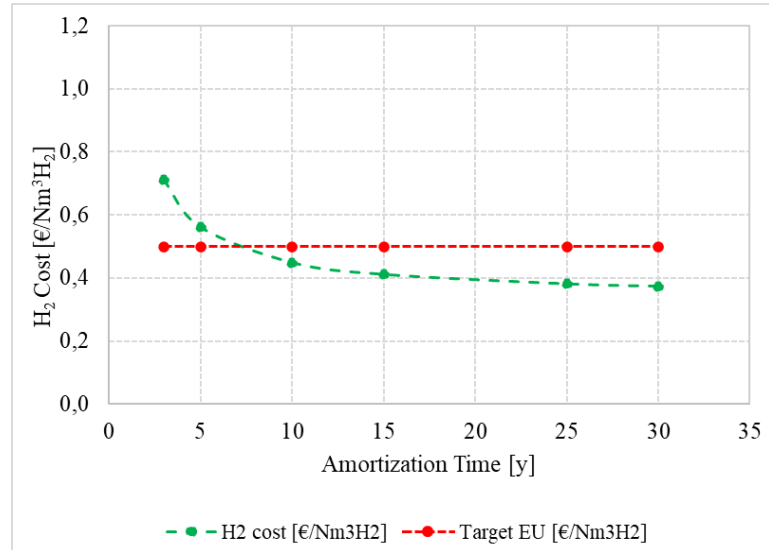
# Project Progress/Actions - H<sub>2</sub> cost

TARGET: Total cost of H<sub>2</sub> (including CAPEX, OPEX) between 0.3-0.5 €/Nm<sup>3</sup>

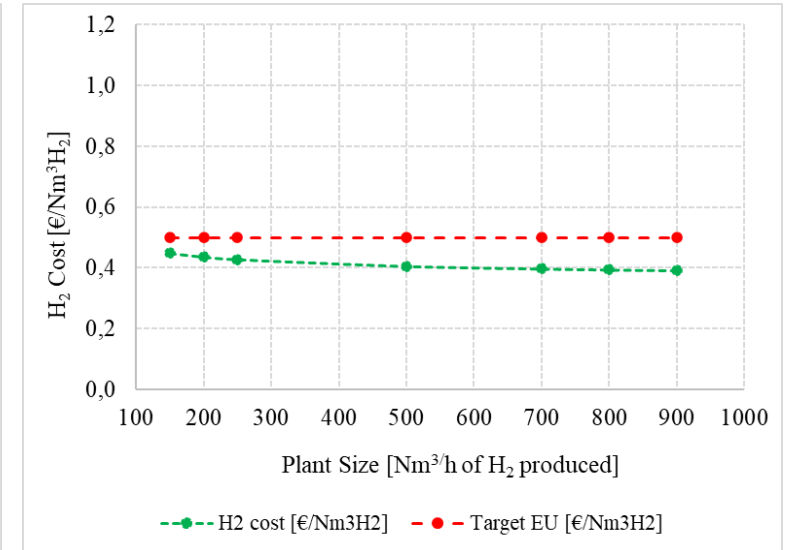
Total actual cost of H<sub>2</sub> produced with the BioRobur<sup>plus</sup> demo (including CAPEX, OPEX)



BioRobur<sup>plus</sup> plant: 50 Nm<sup>3</sup>/h



Considering a plant size of 150 Nm<sup>3</sup>/h



Effect of the size of the plant on the H<sub>2</sub> cost.

Taking as size reference 150 Nm<sup>3</sup>/h and considering 10 years of amortization time

# Risks, Challenges and Lessons Learned

- **Challenges:**
  - High degree of process integration.
  - Catalysts and support development, coating optimization, sub-units construction and interconnecting
  - Final testing campaign
- **Lessons learned:**
  - Thanks to the combination of different partners know-how, experiences and ideas, potential solutions for the currently H<sub>2</sub> production challenges can be developed.
  - This kind of R&D projects are a great opportunity to strengthening the innovation capacity of the SME.
  - Lessons learned for replication of detailed engineering, construction, installation and commissioning.
  - It is important to avoid delays in the early stages of the project and to spend more time for testing and for data collection to optimize and drive future scaleup of the technologies. In addition, a large testing campaign is of great importance when several units are interconnected in order optimize the overall plant.

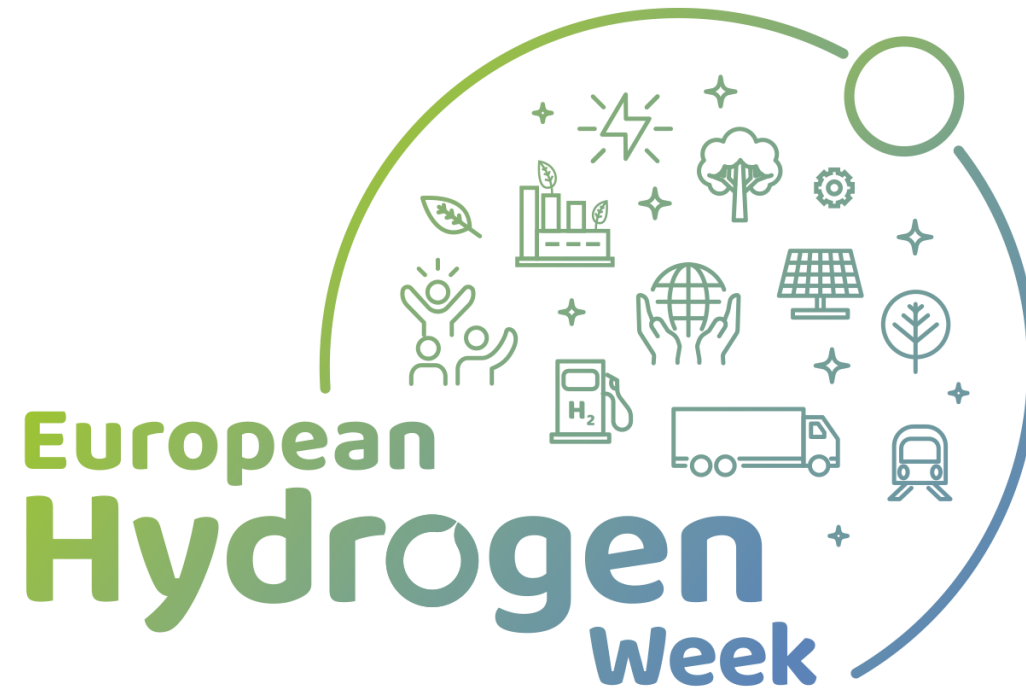
# Exploitation Plan/Expected Impact

## Exploitation

1. Ceramic media with continuous porosity gradient
2. Reforming catalyst stable under biogas reforming conditions
3. Cost-effective and efficient technology for hydrogen purification.

## Impact

1. It could be implemented in gas-fired IR burners and catalyst supports. Sales of the ceramic materials could be generated in the medium/long-term.
2. IP protection under biogas reforming conditions being considered. Catalyst development samples will be made available to customers.
3. This innovation can be implemented in the transportation and industry feedstock sectors for Hydrogen purification applications.



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