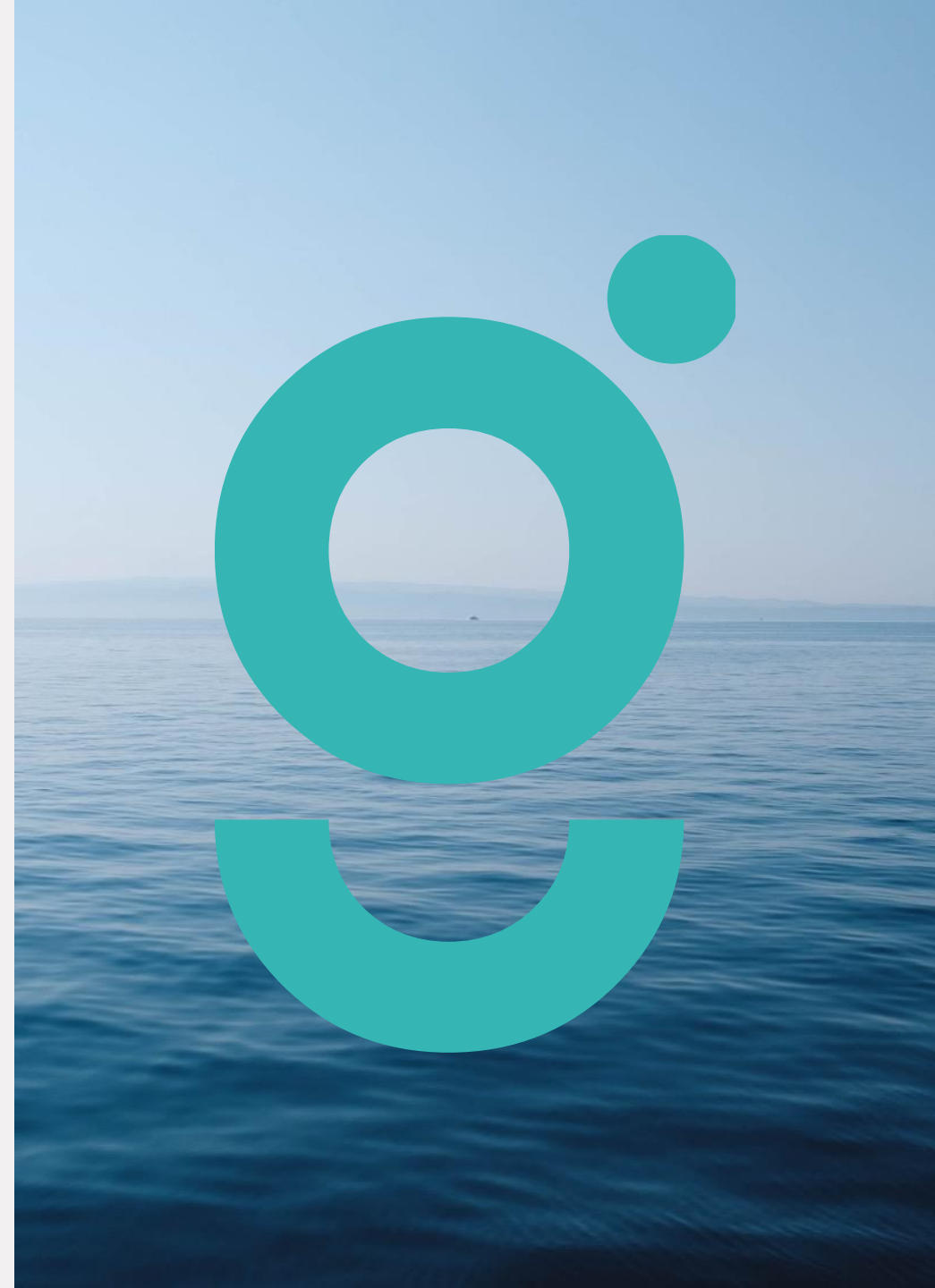




DEGRADATION PHENOMENA  
AND TEST METHODOLOGY  
**PEM Water Electrolysis**

P. Millet, Sept. 29, 2023



## 1. PEM Water Electrolysis: general features

- *the PEM Water Electrolysis unit cell*
- *the PEM Water Electrolysis stack of cells*
- *PEM Water electrolysis durability data*

## 2. Review of main cell ageing processes

- *the PEM Water Electrolysis  $iV$  curve*
- *cell voltage contributing terms*
- *$iV$  curve degradation phenomena*

## 3. ASTs : Ageing Stress Tests

- *chronopotentiometric analysis*
- *EIS analysis*

## 4. Conclusions & Perspectives

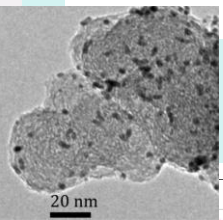
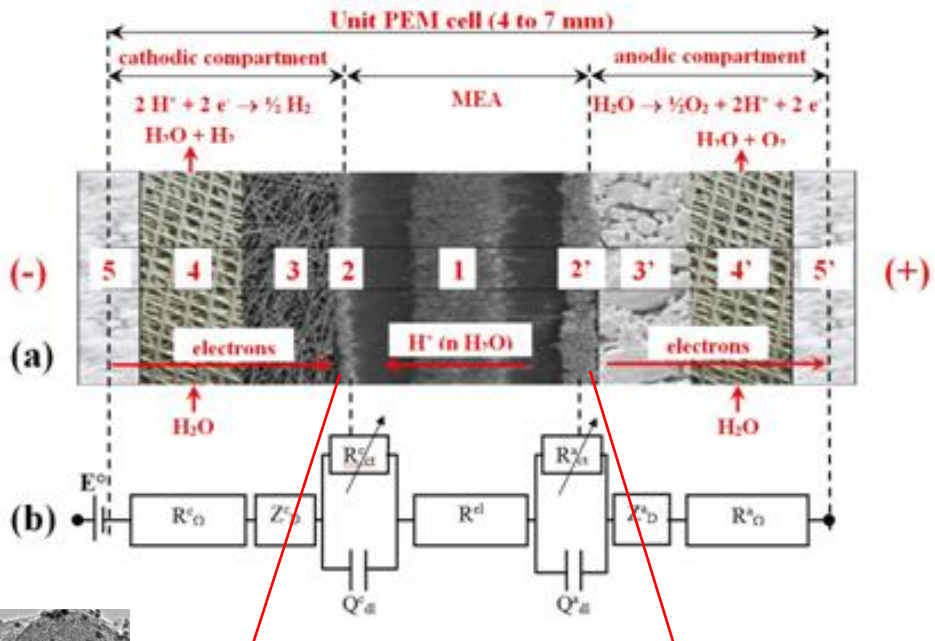
Section 1



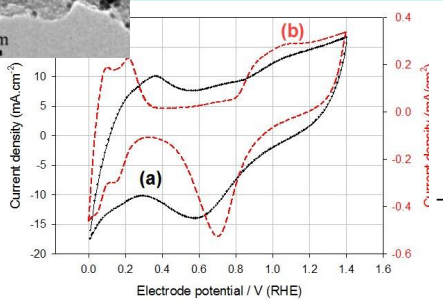
# PEM Water electrolysis **general features**



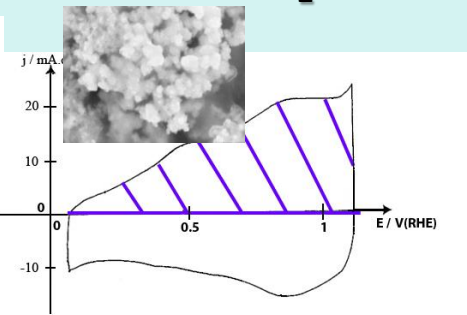
# The PEM Water Electrolysis unit cell



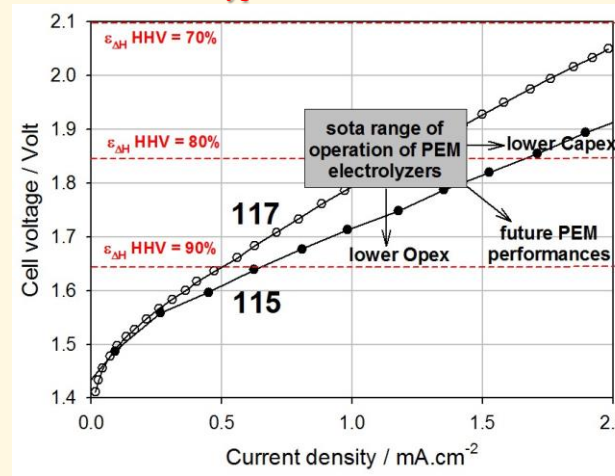
**HER: Pt/C**



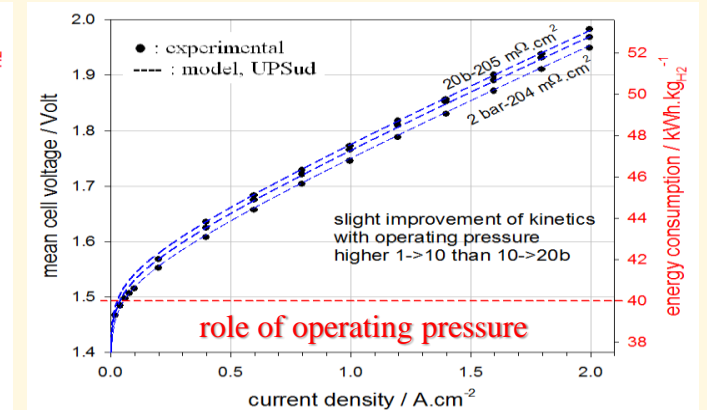
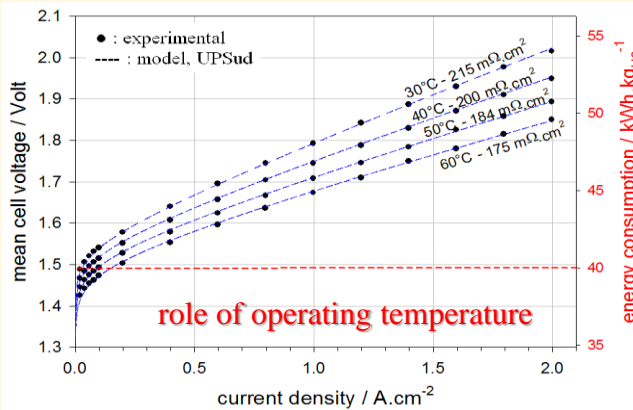
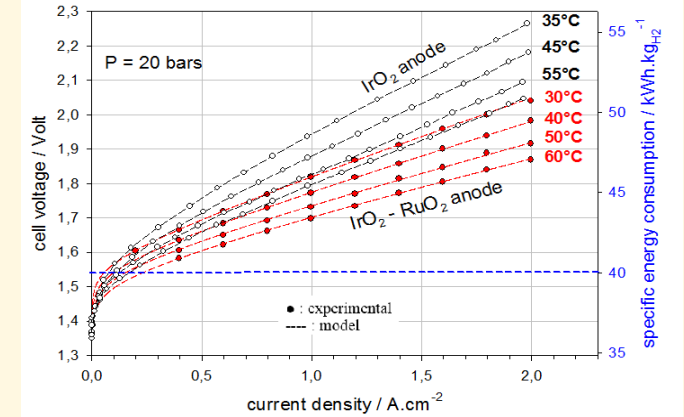
**OER: IrO<sub>2</sub>**



**typical iV curves**



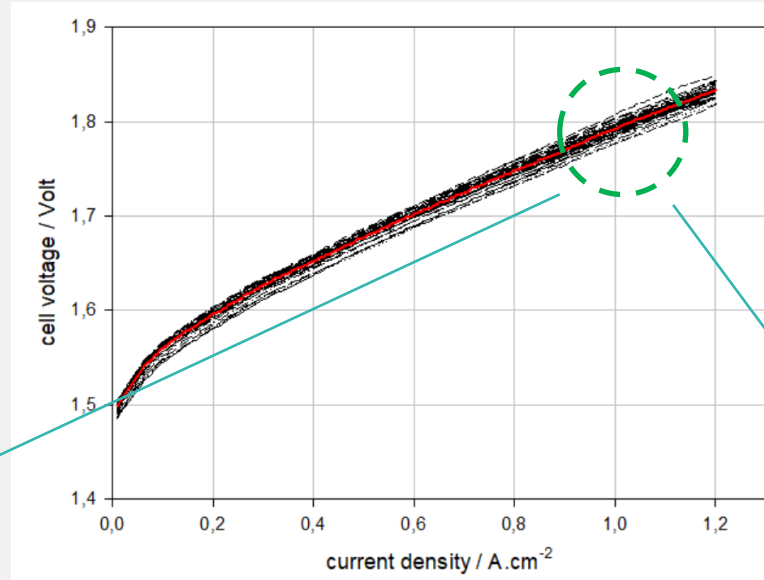
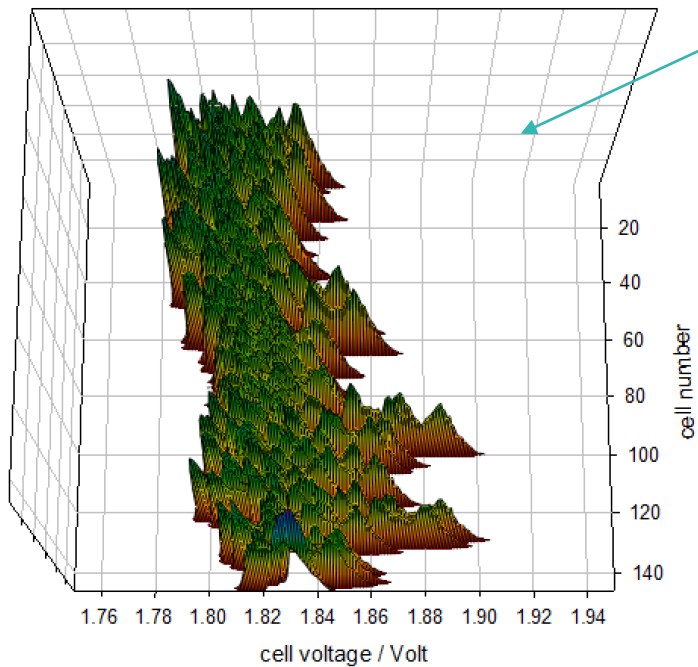
**role of electrocatalysts**



# The PEM Water Electrolysis stack of cells

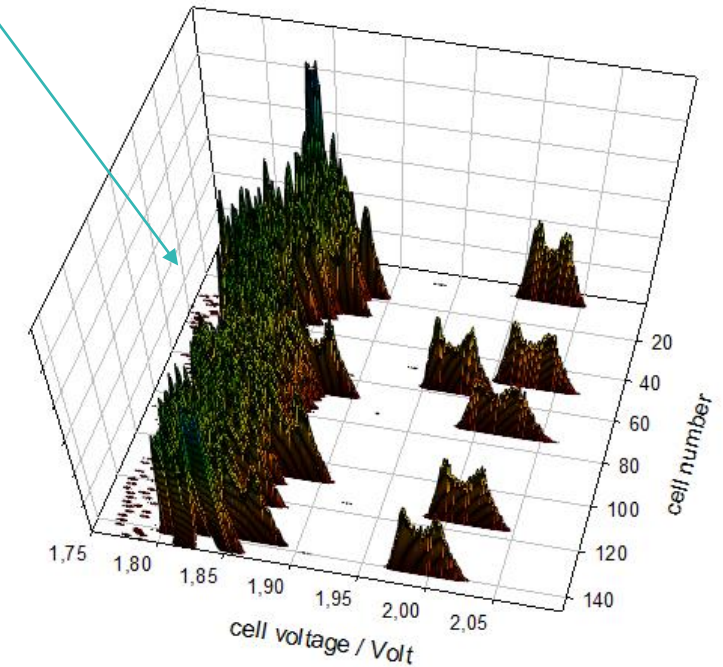


early age stack distributions



Stacks in operation are more stressed than laboratory cells ...

aged stack distributions

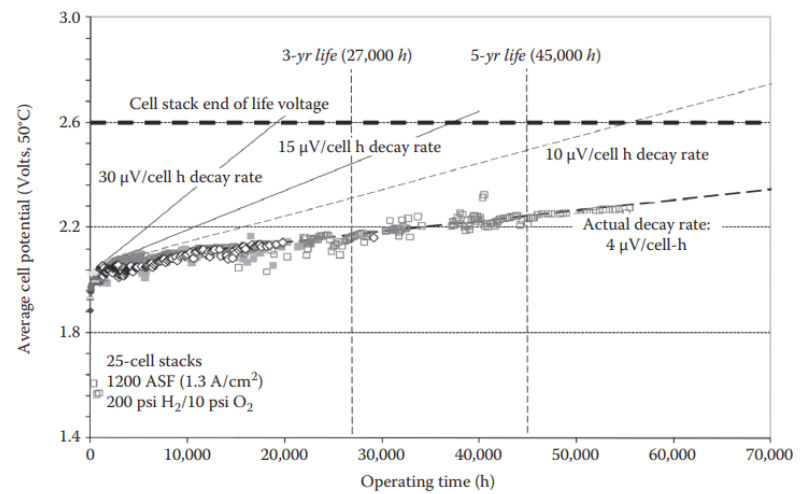
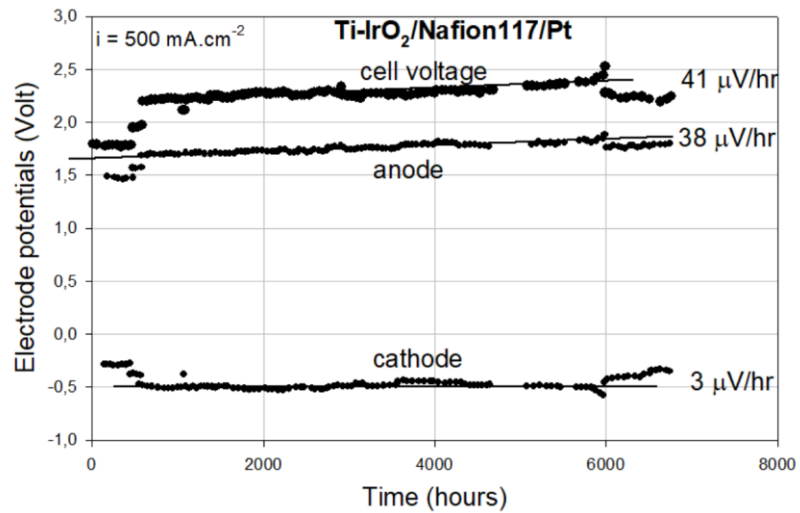


- under stationary operating conditions, individual cell voltages are not constants.
- better to use cell voltage distributions.
- the homogeneity of cell voltage distributions is the KPI of interest
- aged cells see their mean voltage increase faster than others.

# Durability data

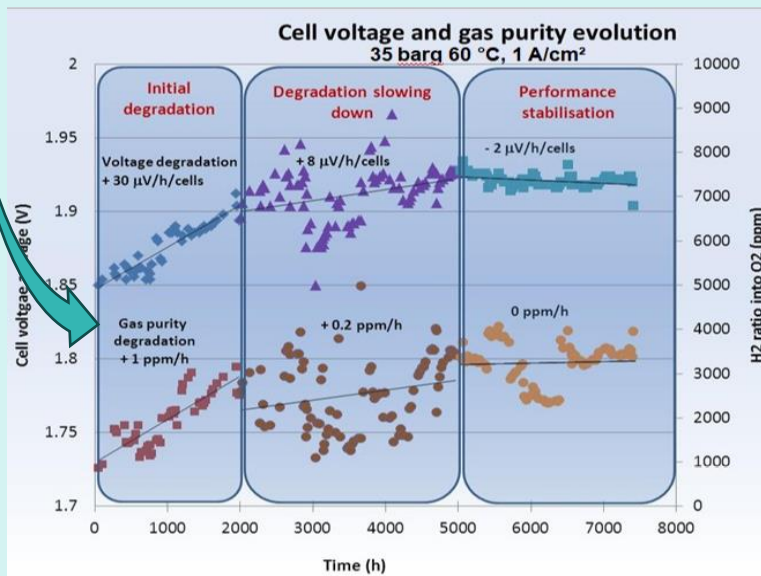
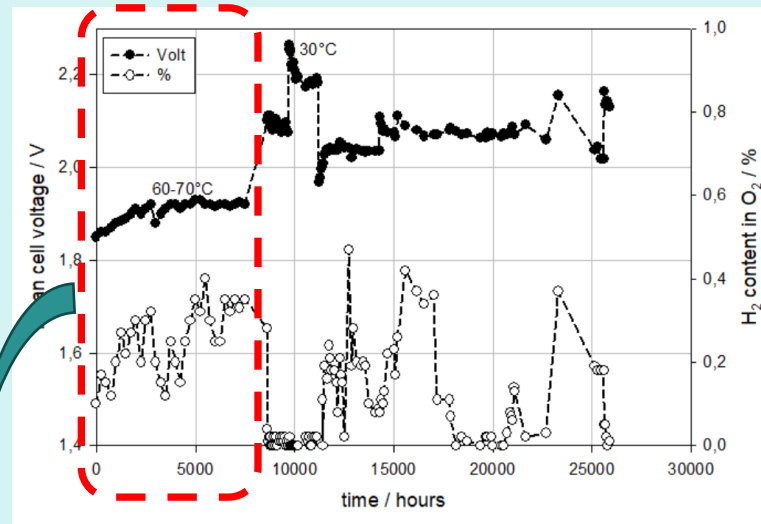


## some literature data



J. Renner et al., in: 'PEM water Electrolysis for hydrogen production: Principles and Applications', D. Bessarabov, H. Wand, H. Li, N. Zhao, CRC Press (2015).

## some corporate data



## some key facts

- PEM water electrolyzers can be operated up to **70-80 khrs.**
- the mean cell voltage increases with time.
- as a result, the mean energy consumption in kWh/kg<sub>H<sub>2</sub></sub> also increases.
- some cells age quicker than others.
- the H<sub>2</sub> content in O<sub>2</sub> also tends to increase if not properly mitigated.
- the cell voltage at which the stack is stopped and replaced depends on several technical/cost factors.

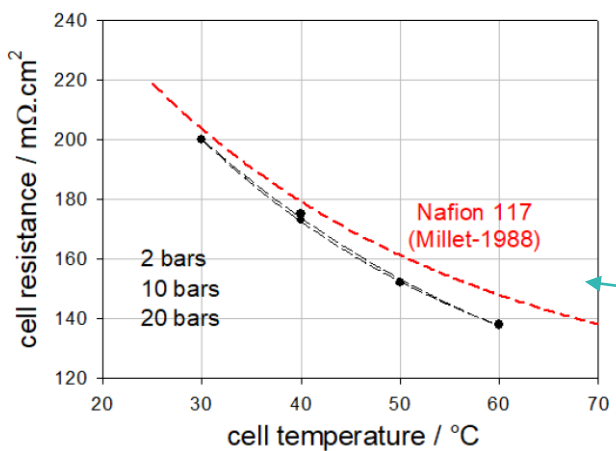
Section 2



# Review of main cell **ageing processes**



# The PEM Water Electrolysis iV curve (simple 1D model)



ohmic losses

$$i \sum_{k=1}^n R_k = \lim_{\omega \rightarrow 10kHz} Z^{cell}(\omega, T, P)$$

OER overvoltage

$$\eta_{O_2} \approx \frac{R T}{\alpha_a F} \ln \left( \frac{j^a}{j_0^a r_f^a} \right)$$

$$U_{cell}(T, P, j) = E_{T,P} + i \sum_{k=1}^n R_k(T, P, j) + \eta_{H_2}(T, P, j) + \eta_{O_2}(T, P, j) + \eta_{H_2O}(T, P, j)$$

mass transport

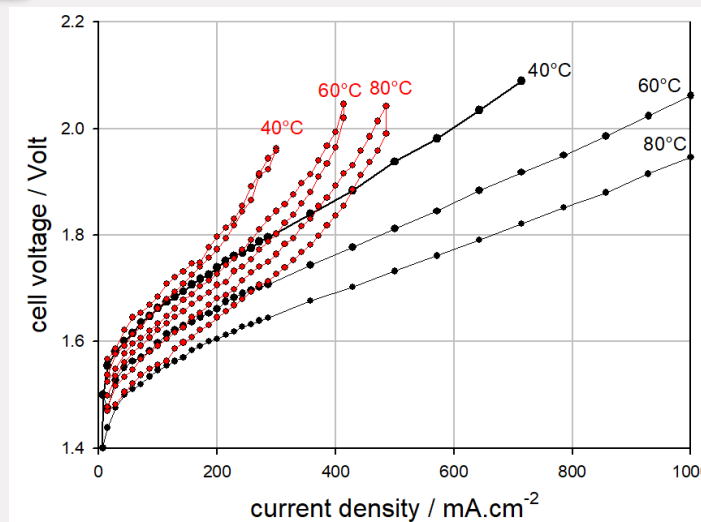
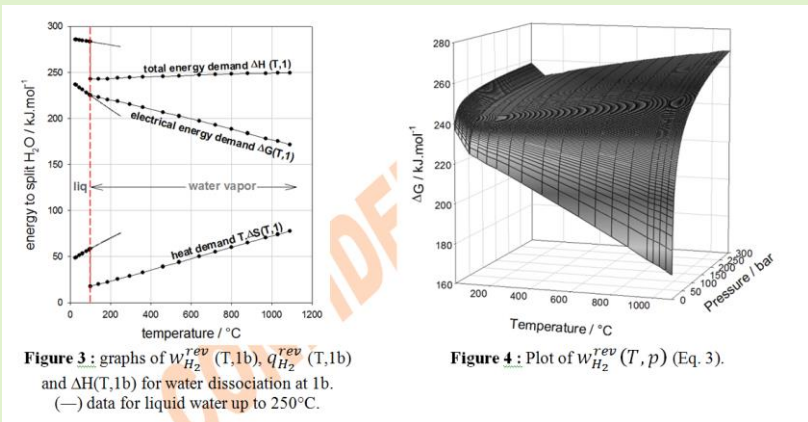
$$\eta_{H_2O} \approx \frac{R T}{n F} \ln \left( \frac{j}{j_L - j} \right)$$

thermodynamics

$$E_{T,P} = \frac{\Delta G(T, P)}{2F}$$

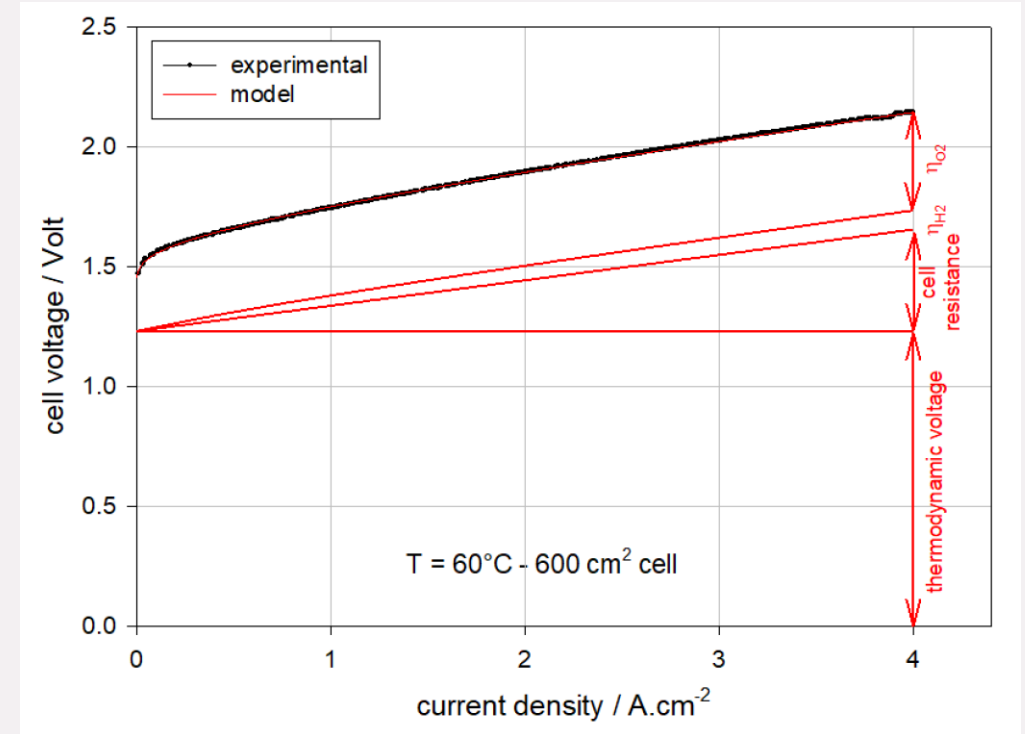
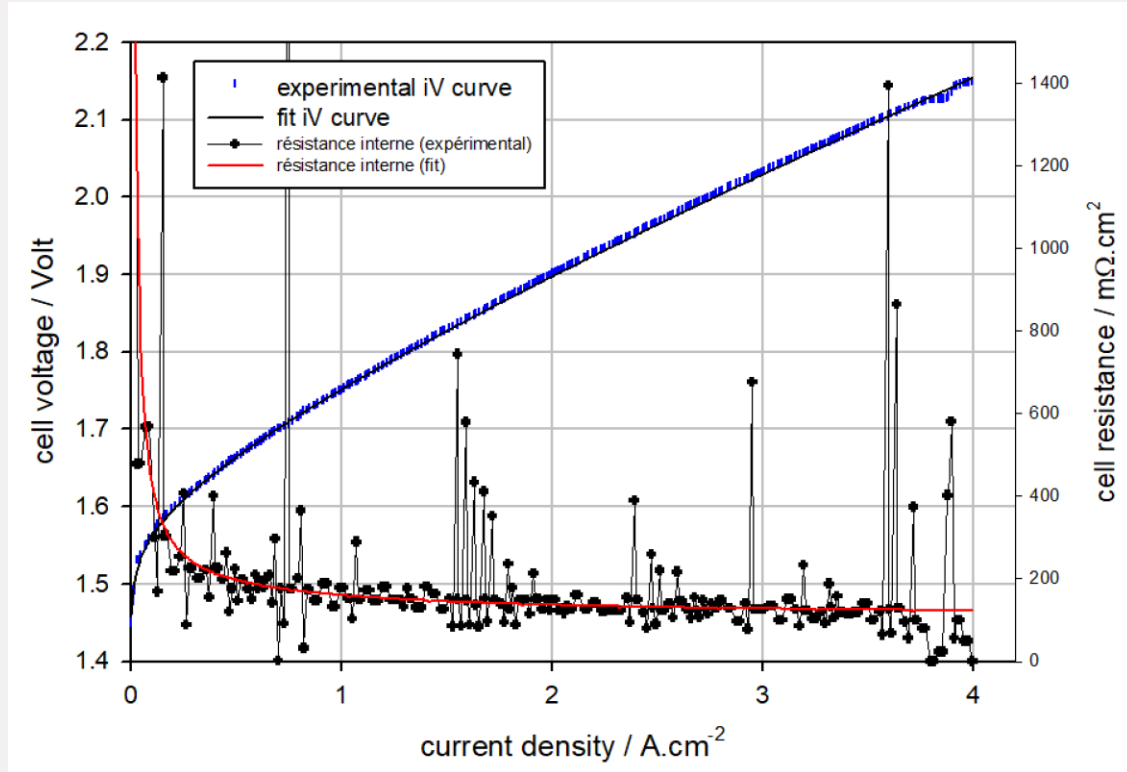
$$\eta_{H_2} \approx \frac{R T}{\alpha_c F} \ln \left( \frac{-j^c}{j_0^c r_f^c} \right)$$

HER overvoltage





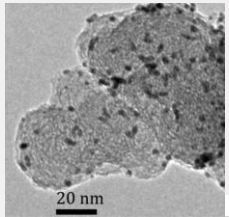
# Cell voltage contributing terms



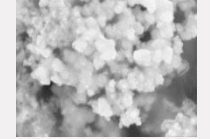
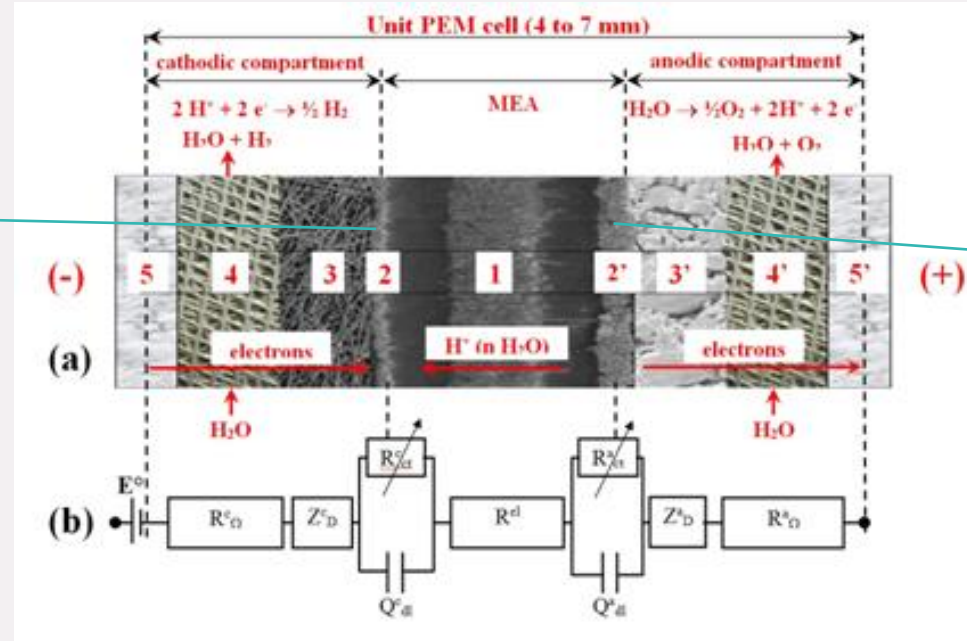
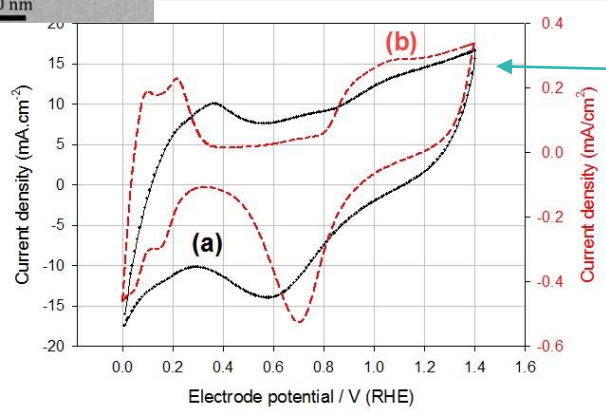
Ranking cell voltage terms in descending order (using Nafion 115, without mass transport issues):

1. the thermodynamic cell voltage ( $E^\circ = 1.23 \text{ V}$ )
2. the OER overvoltage
3. the ohmic cell resistance (metallic + ionic)
4. the HER overvoltage

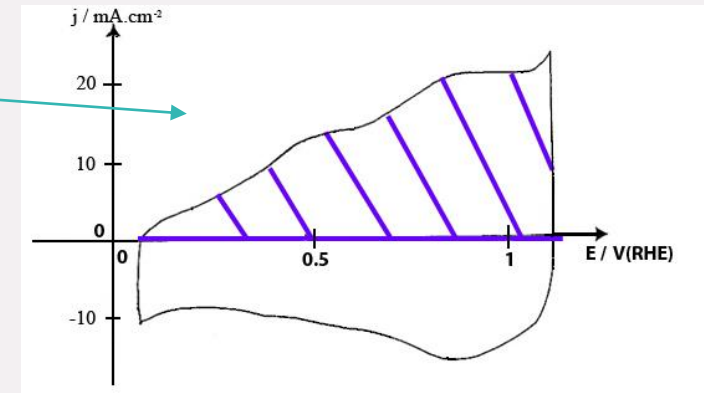
# iV curve degradation phenomena



HER: Pt or Pt/C



OER: IrO<sub>2</sub>



## type of ageing process

- external CCM contamination, ion-exchange
- oxidation of internal cell components
- loss of HER active sites
- loss of OER active sites
- PFSA membrane degradation
- mass transport issues
- deactivation of H<sub>2</sub> recombiner (pressurized)

## ageing mechanism & consequences

- increased resistivity and HER overvoltage
- increasing contact resistance and  $Z_{cell}$
- increasing HER overvoltage
- increasing OER overvoltage
- impact on conductivity, stability, H<sub>2</sub> cross-over
- reduced water supply, limiting current density
- dissolution/contamination

## possible mitigation measures

- monitoring of process water quality
- use of protective coatings
- *increase initial loadings*
- *increase initial loadings*
- use of additives
- management of cell design/hydrodynamics

Section 3

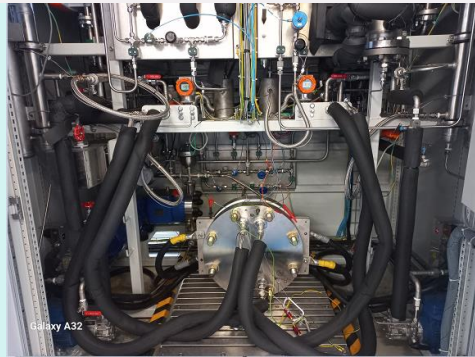


# ASTs ageing stress tests

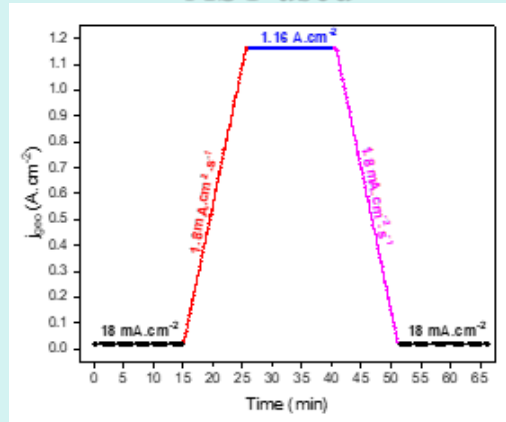


# Chronopotentiometric analysis

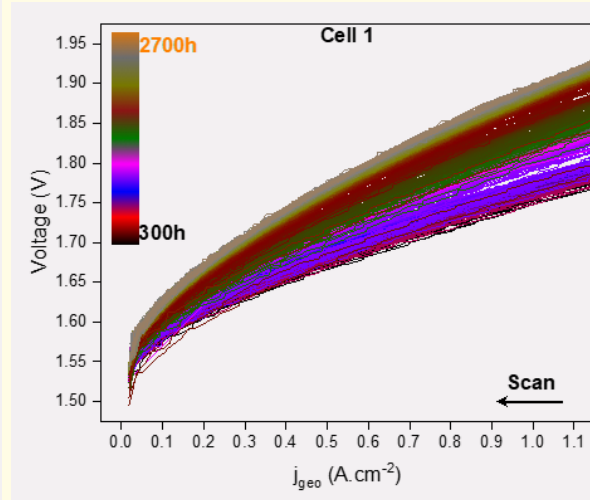
ASTs can be used for R&D or business purposes; business ASTs reflect power input conditions.



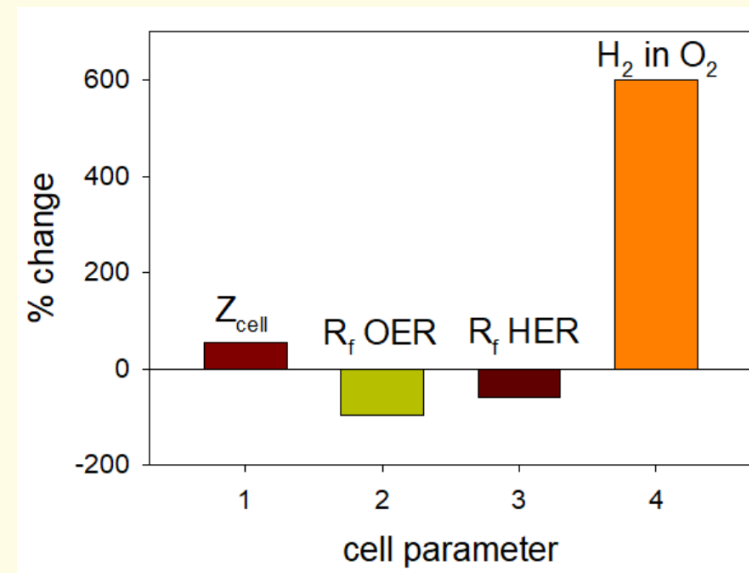
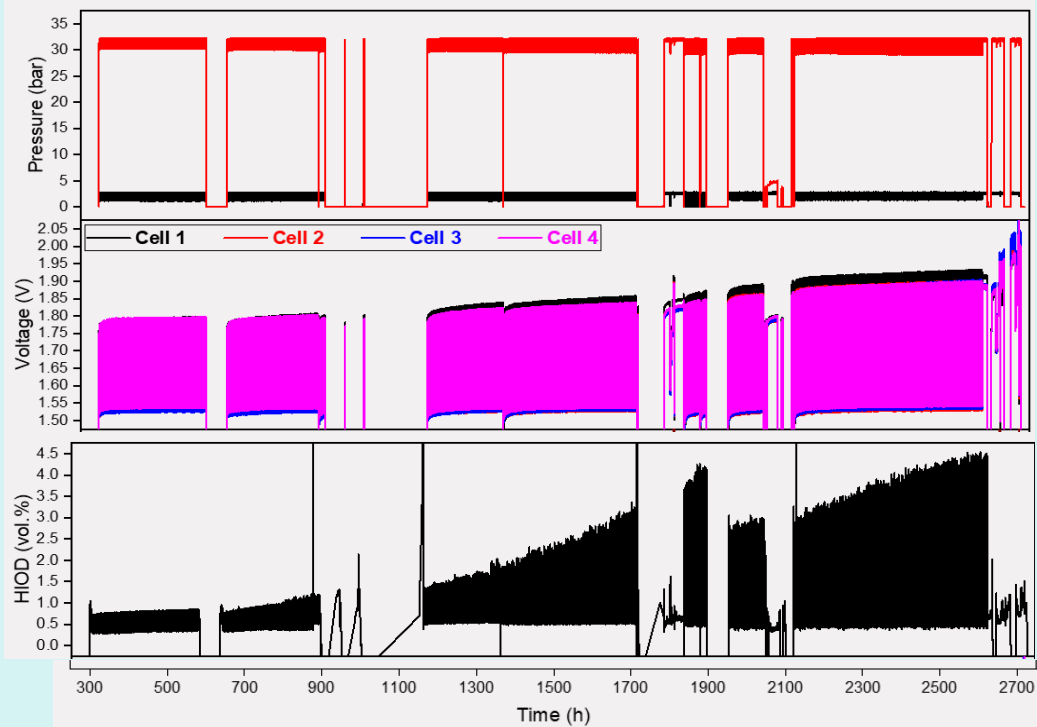
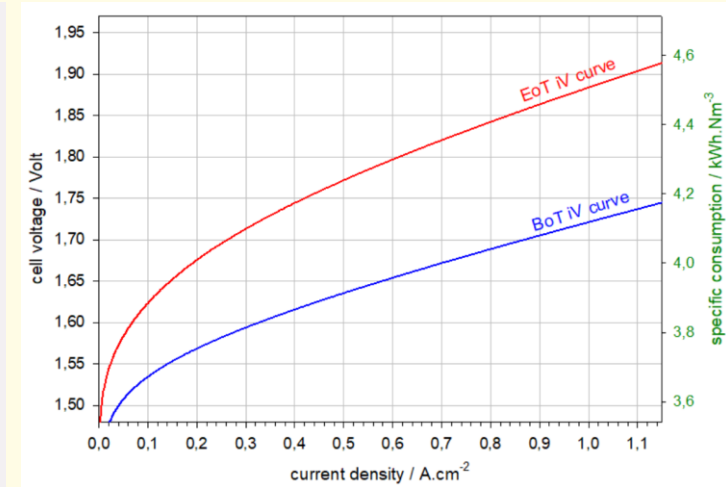
AST used



iV curve ageing



BoT -> EoT iV curves



H<sub>2</sub> in O<sub>2</sub> has increased by a factor of 6

Section 4



# Conclusions & perspectives



# Conclusions & perspectives

## Conclusions

1. some degradation phenomena are reversible (eg, contamination) while some others are irreversible.
2. for individual cells, the analysis of iV curve provides all the necessary information to identify degradation phenomena.
3. complementary techniques (eg, EIS, CV) can also be used but not routinely for stacks.
4. all microkinetic parameters tend to deteriorate with time, in proportions which depend on the operating conditions
5. metallic cations from various sources (eg, process piping) induce low-noise contamination of CCMs:
6. this leads to a progressive increase in membrane resistance, but also to increasing HER overvoltage.
7. **IrO<sub>2</sub> corrosion/dissolution can lead to large OER overvoltage increases.**

## Perspectives

1. PFSA membranes and Pt are highly sensitive to trace amounts of metallic cations that tend to accumulate inside CCMs.
2. degradation mechanisms need to be investigated by taking into account the type of electrical profile used by customers.
3. reducing IrO<sub>2</sub> contents for cost reasons comes up against corrosion processes which tend to consume IrO<sub>2</sub>.
4. the ongoing procedures to ban the use of PFAS in the European area pose a threat to investments and the future of the PEM sector.
5. R&D on alternative proton conductors and HER/OER electrocatalysts for acidic media is still needed.

# Thank you for your attention

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**elogen**

