

# BioRoburPlus

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#PRD2021  
#CleanHydrogen

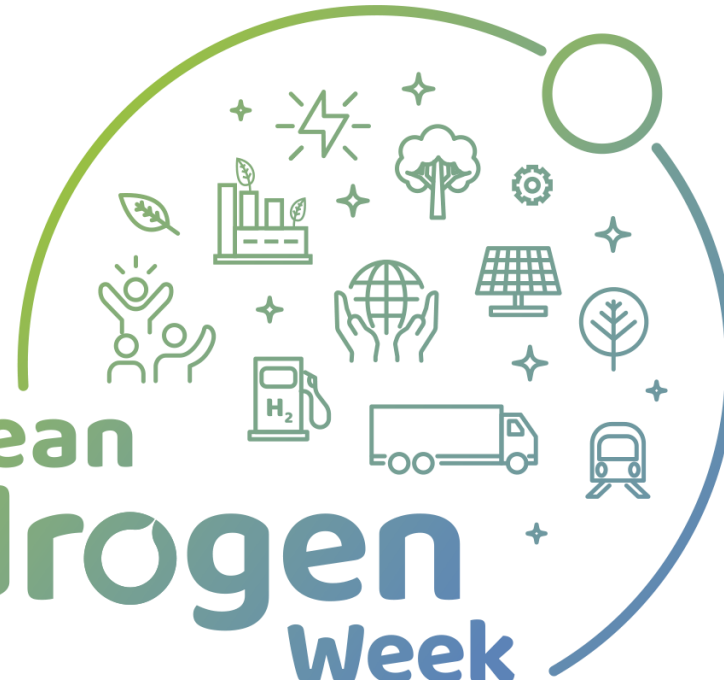


# BioRoburPlus

Advanced direct biogas fuel processor for robust and cost-effective decentralized  
hydrogen production



European  
**Hydrogen**  
Week

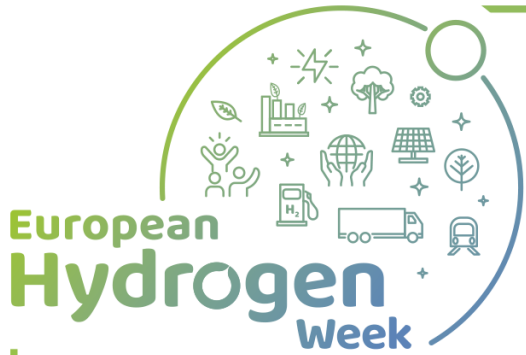


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#PRD2021  
#CleanHydrogen



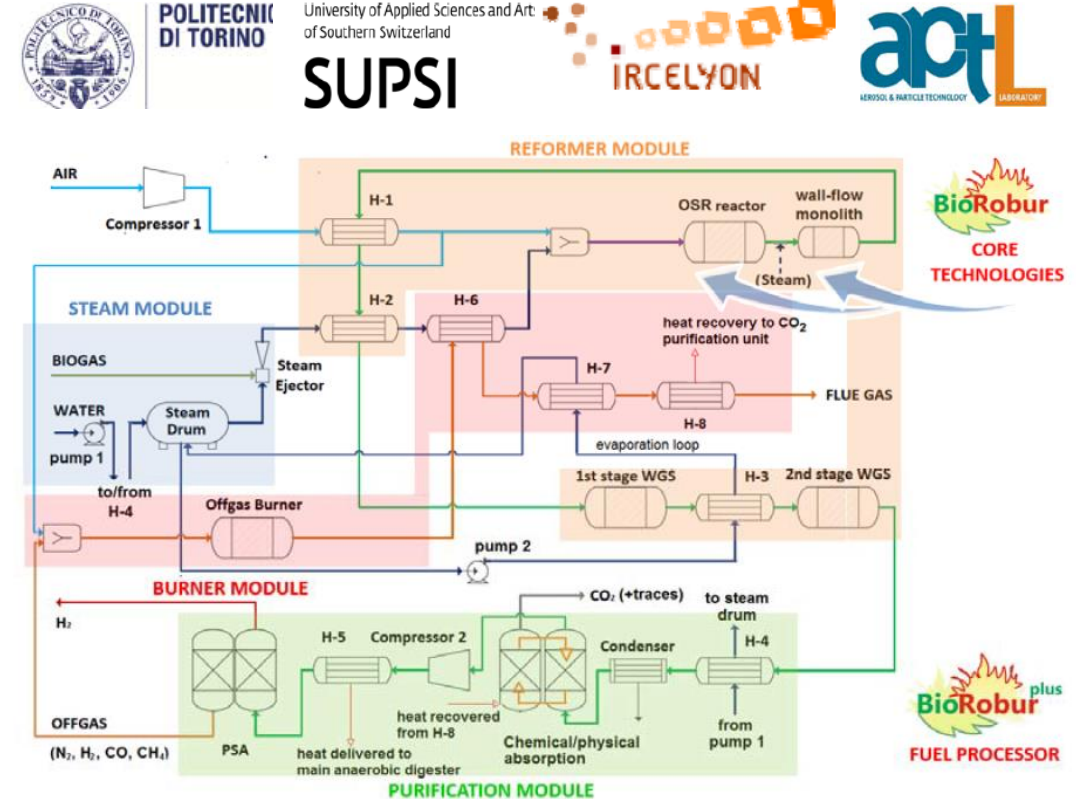


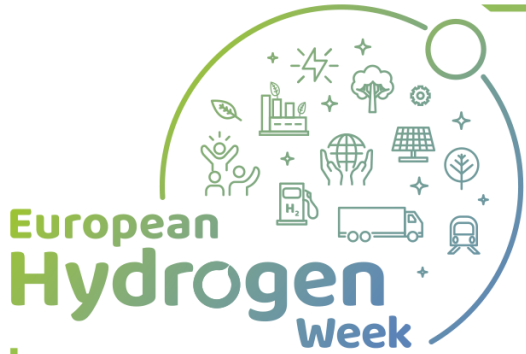
# Project Overview

- Call year: 2016
- Call topic: H2020-JTI-FCH-2016-1 - FCH-02-2-2016 - Development of compact reformers for distributed bio-hydrogen production
- Project dates: 01/07/2017- end date
- % stage of implementation 30/11/2021: 100 %
- Total project budget: 3.813.536 €
- FCH JU max. contribution: 3.813.536 €
- Partners: POLITECNICO DI TORINO, KARLSRUHER INSTITUT, SCUOLA UNIVERSITARIA PROFESSIONALE DELLA SVIZZERA ITALIANA, CENTRE NATIONAL DE LA RECHERCHE SCIENTIFIQUE, ETHNIKO KENTRO EREVNAS, DBI - GASTECHNOLOGISCHES INSTITUT, ENGICER SA, HYSYTECH SRL, UAB MODERNIOS ETECHNOLOGIJOS, ACEA PINEROLESE, JOHNSON MATTHEY PLC.

# Objectives

- Design and manufacturing of an integrated processor consisting of:
  - REFORMER module
  - Purification module
  - Off-gas burner module
  - Steam module
- Cost-effective GREEN H<sub>2</sub> production
- Minimization of the different environmental category impacts assessed through LCA





# Example And Explanation of Project Progress/Actions - Catalyst performance



Achievement to-date

>98% of conversion



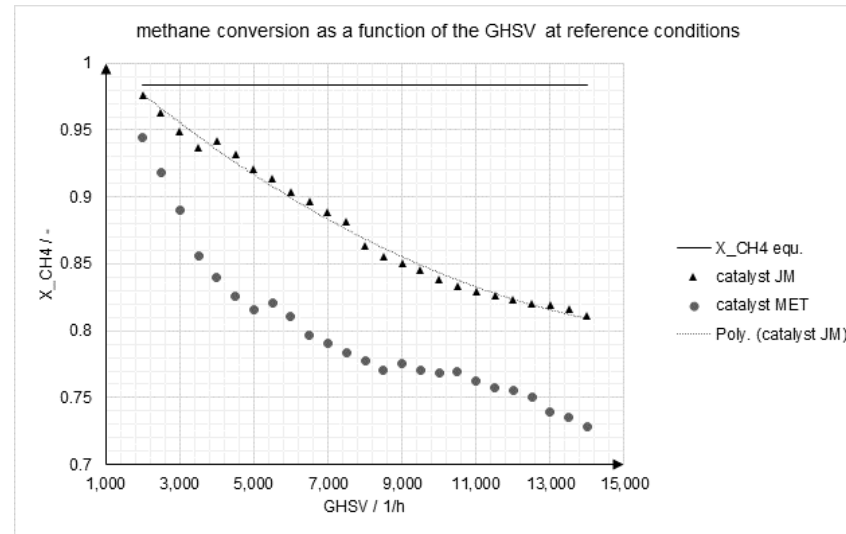
92% of conversion

25%

50%

75%

Status at month 54 of a 54 months project at date 30/11/2021



# Example And Explanation of Project Progress/Actions - Prototype productivity



Achievement to-date

30 Nm<sup>3</sup>/H<sub>2</sub>/h  
99.9 % purity



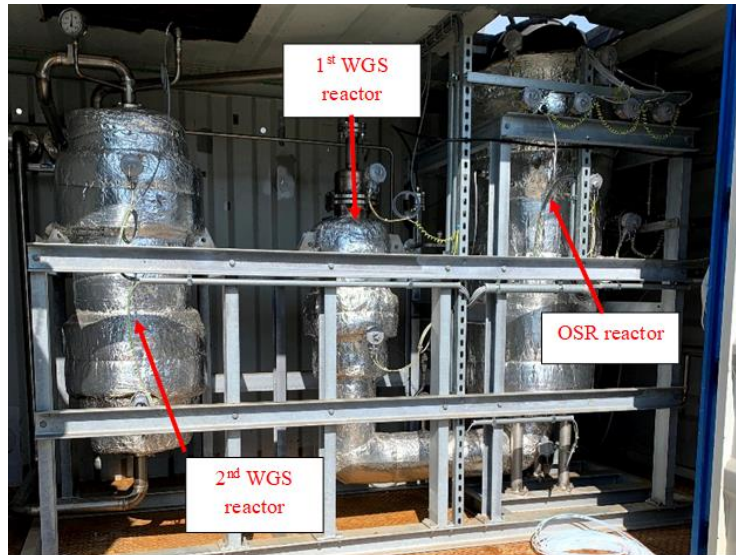
30 Nm<sup>3</sup>/H<sub>2</sub>/h  
99.9 % purity

25%

50%

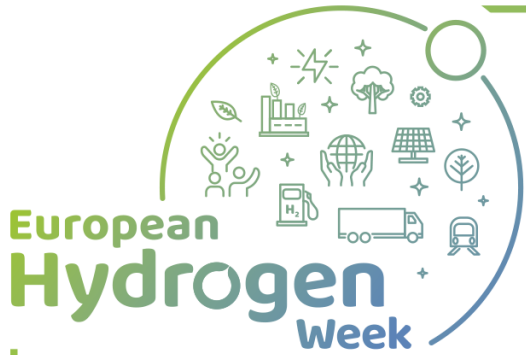
75%

Status at month 54 of a 54 months project at date 30/11/2021



# Risks, Challenges and Lessons Learned

Exploitation Result from Table 1	Type of risk	Description of risk. Severity?	Mitigation strategy	Who is responsible	Outcome: Risk contained? Yes/No
1	Performance not improved compared to state of the art porous ceramics	Medium	Re-design	SUPSI	Yes
2	Catalyst is too expensive	Medium	Additional catalyst development to reduce PGM loading if necessary	JM	Yes
2	Catalyst does not meet customer requirements	Low	Additional catalyst development based on customer requirements	JM	Yes
2	No (biogas reforming) market for catalyst	Medium	Look for alternative markets for catalyst	JM	Yes
3	Performance not improved compared to the state of the art	Medium	Evaluation of further adsorbent materials and/or better design of heat integration.	HST POLITO	Yes
4	Non-competitive production costs within the EU market of H <sub>2</sub> .	Medium	Evaluation of varying the process parameters according to the sensitivity analysis of costs.	HST	Yes



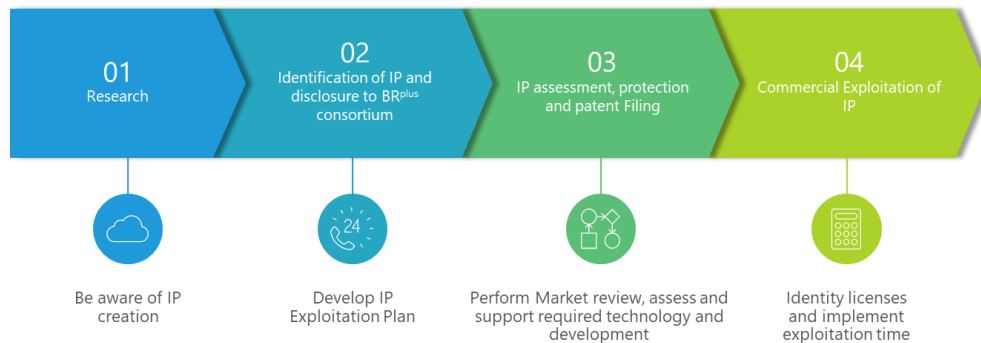
# Exploitation Plan/Expected Impact

## Exploitation

The Exploitation Plan (EP), included in the PUEF, will be designed to multiply the impact of the proposed solutions and prepare the transition towards industrial and commercial uptake to fully achieve the expected impact.

### Exploitable results:

- Ceramic media with continuous porosity gradient
- Reforming catalyst stable under biogas reforming conditions
- Cost-effective and efficient PSA technology for hydrogen purification



## Impact

- New sales
- More sustainable process
- Higher revenues

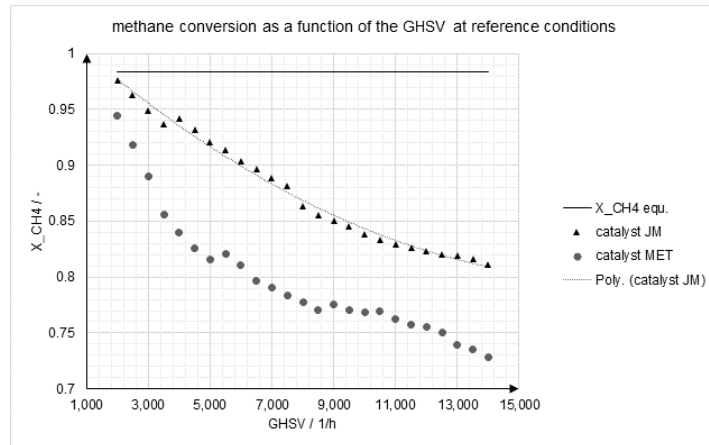
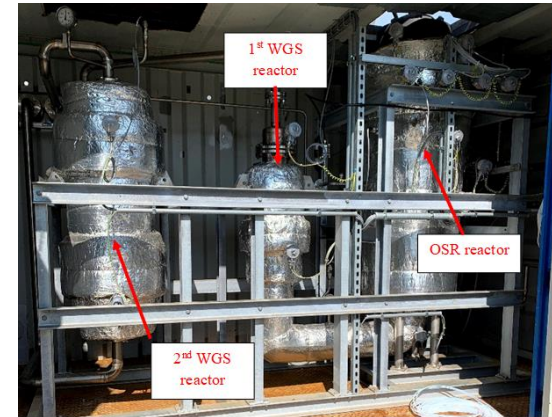


# Catalyst development

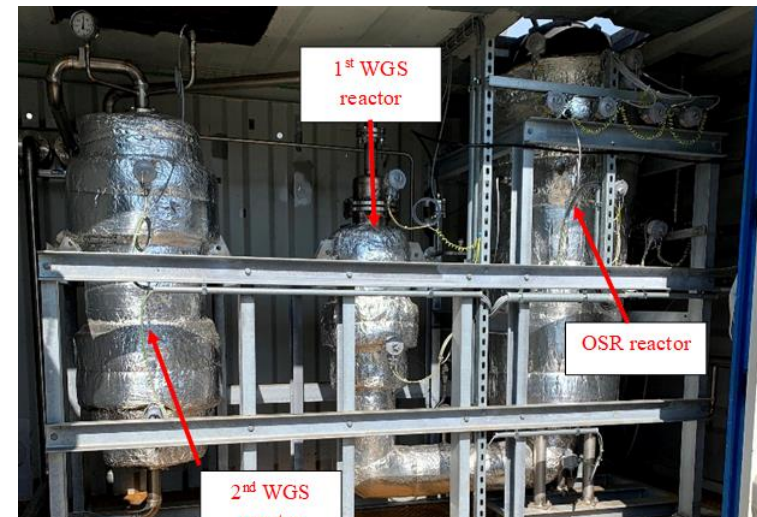
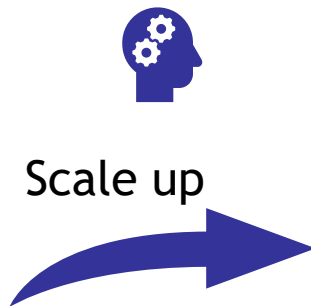
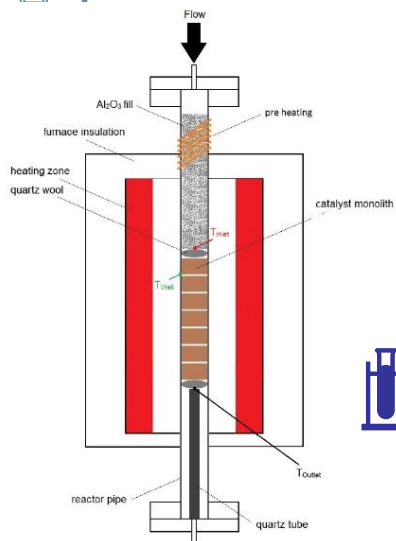
- From lab scale



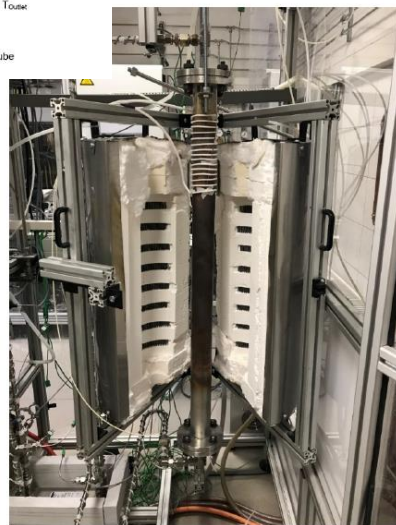
- To pilot scale



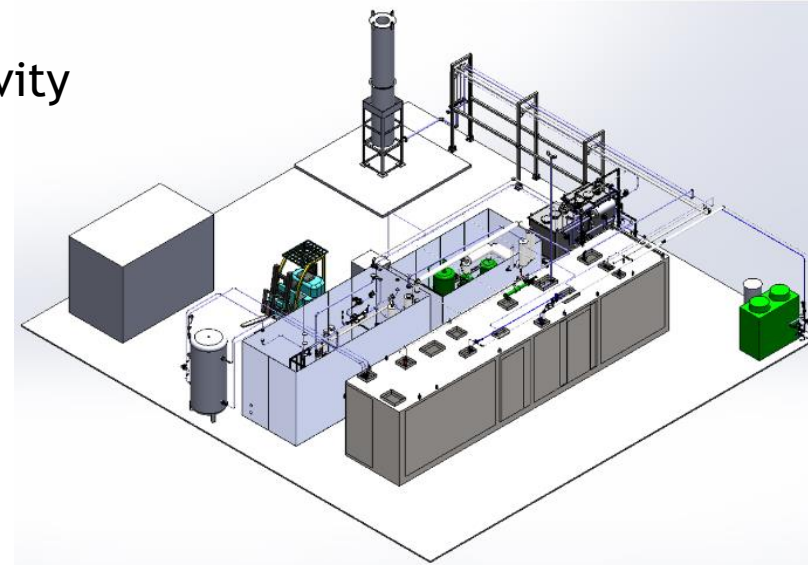
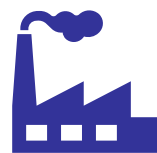
# Scale up - Design



Lab scale H<sub>2</sub> productivity  
0.5 m<sup>3</sup>/h

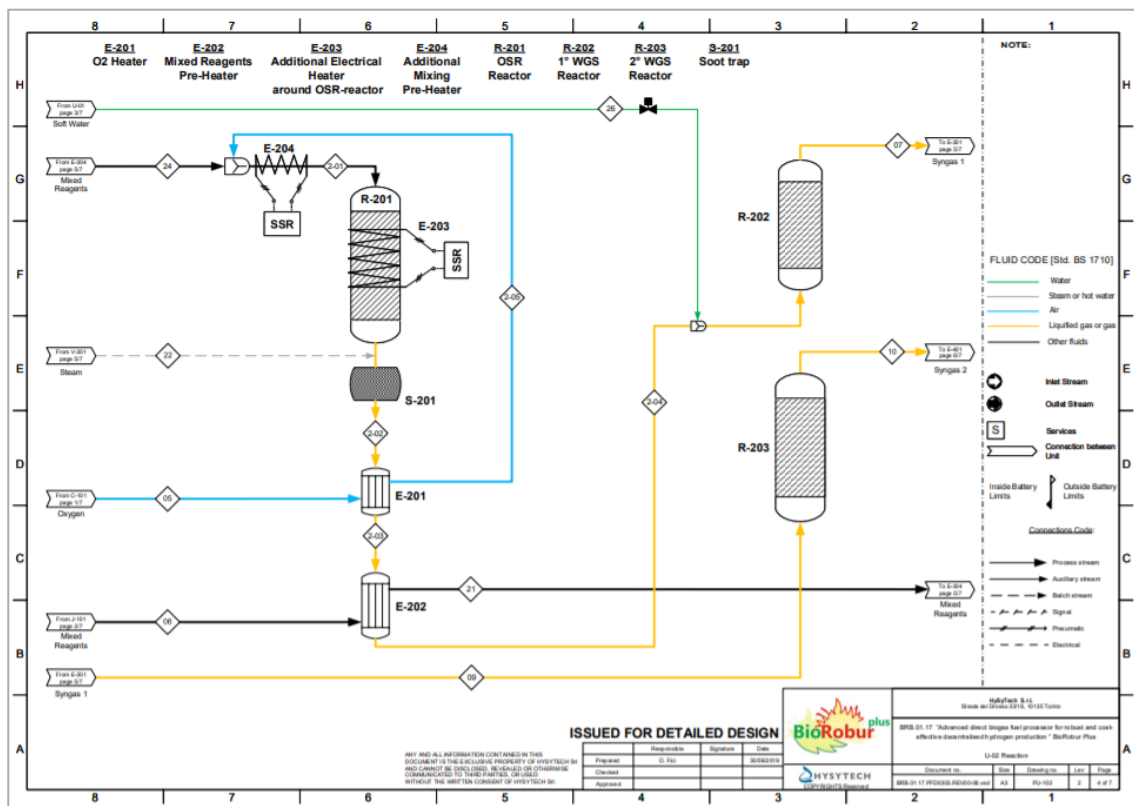


Prototype  
Pure H<sub>2</sub> productivity  
50 m<sup>3</sup>/h



# Design and Manufacturing

## Feeding Section



Water Softening System



Sulphur removal



Air buffer



Air compressor



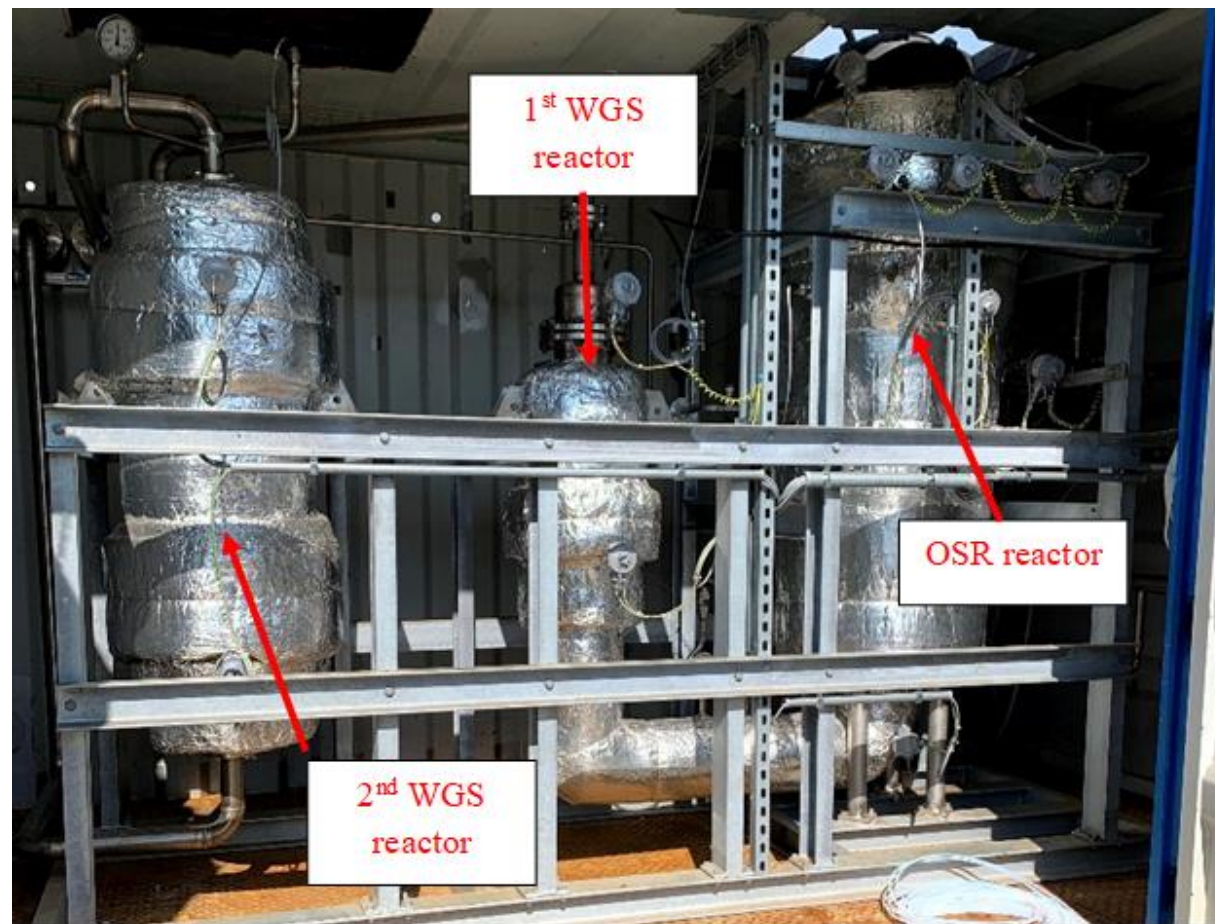
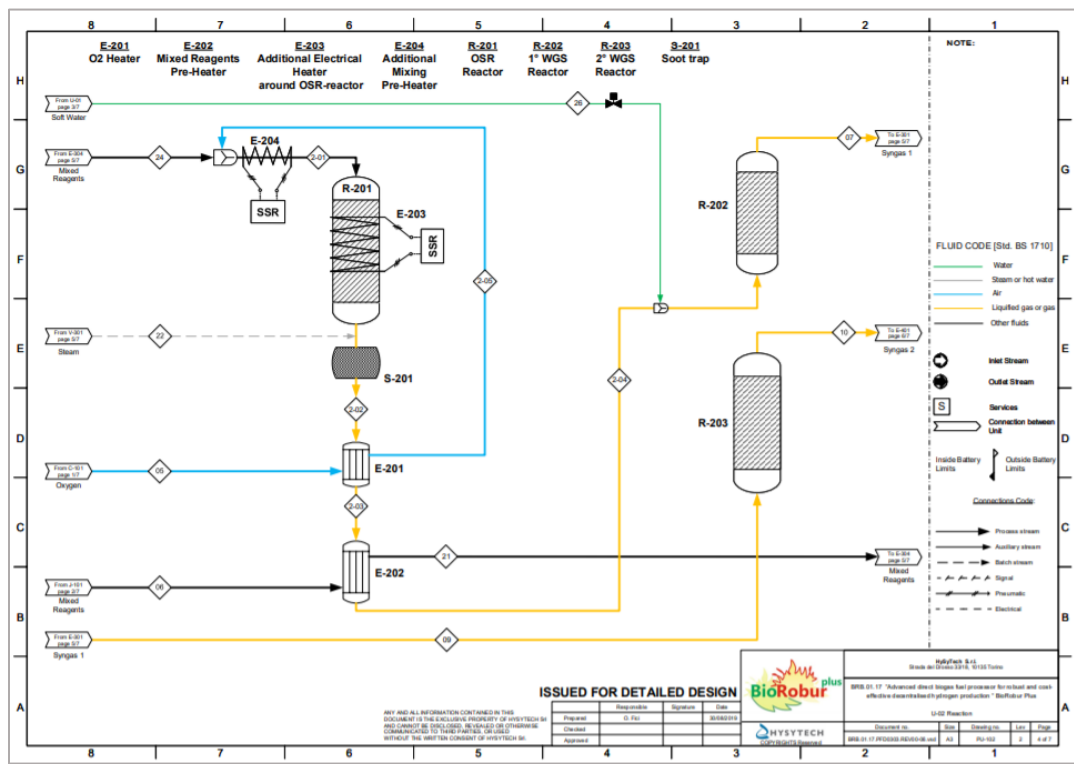
Oxygen Generator



Steam ejector

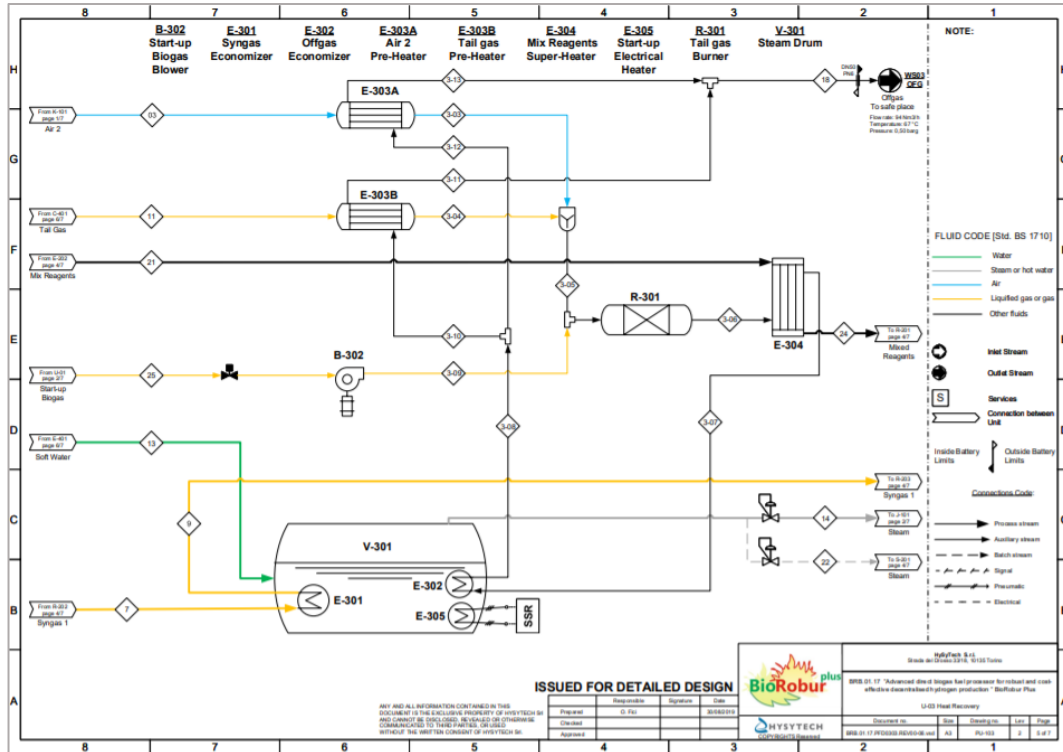
# Design and Manufacturing

## Reaction Section



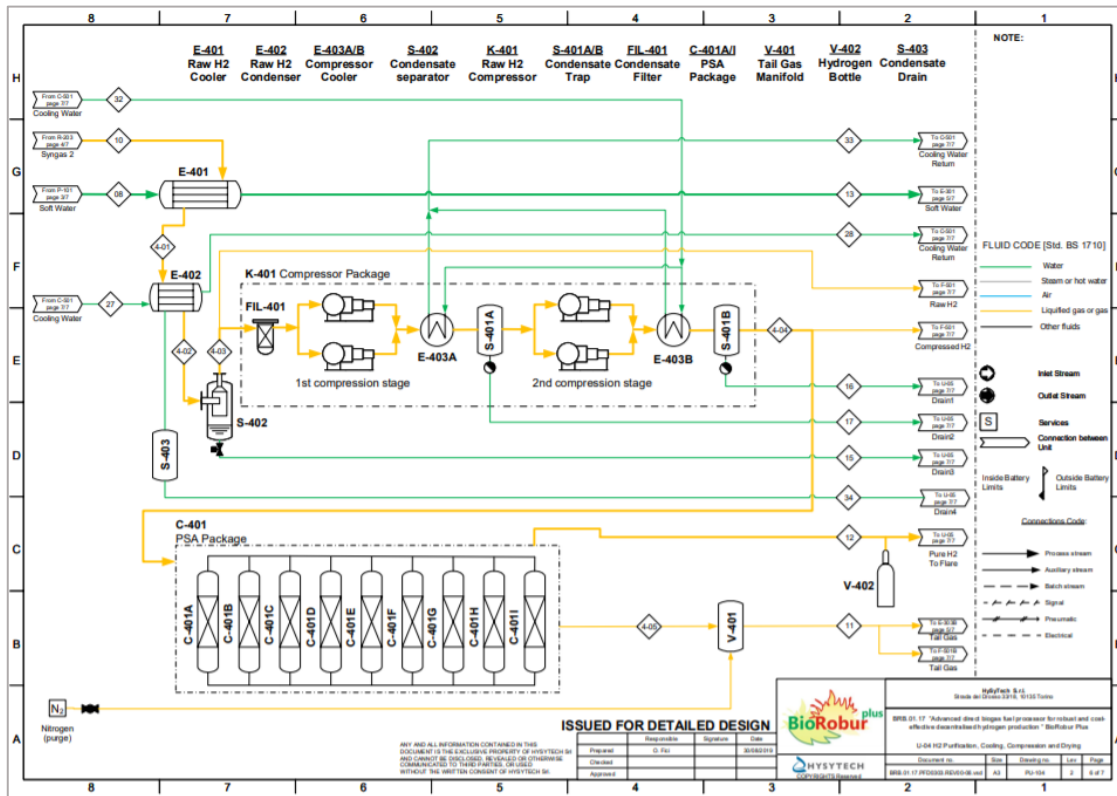
# Design and Manufacturing

## Steam Drum and Burner System



# Design and Manufacturing

## H<sub>2</sub> Compressor and PSA Section

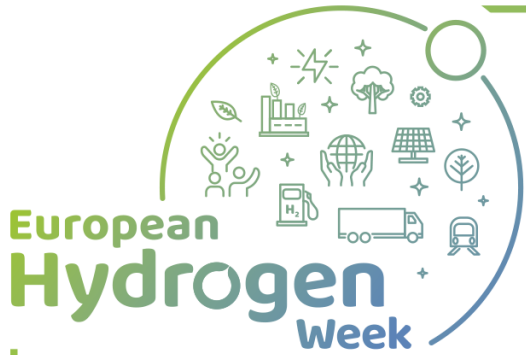


H<sub>2</sub> Compressor



PSA columns





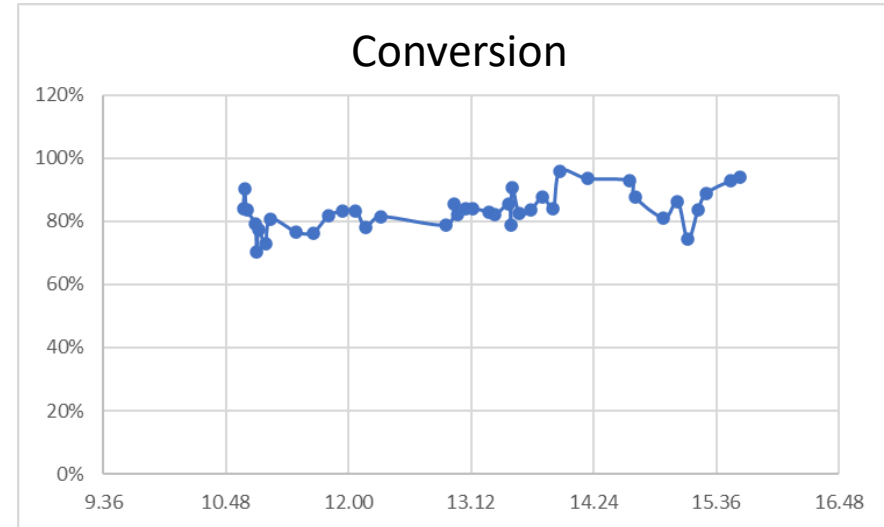
# Prototype testing campaign

Biogas treated:  
Up to 50 Nm<sup>3</sup>/h

Component	Biogas feed
CH <sub>4</sub> [% vol]	56.7
H <sub>2</sub> S [ppm]	327
CO <sub>2</sub> [% vol]	42.84
O <sub>2</sub> [% vol]	0.1

Pressure and Temperature of  
the reaction conditions:  
>600 °C ; 0.5 barg

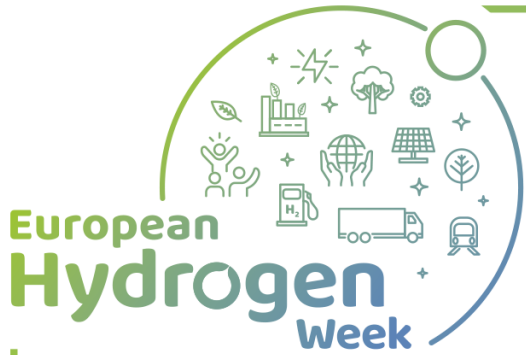
PSA conditions:  
Feed : 12 barg  
Temperature: 35 °C



**50 Nm<sup>3</sup>/h**  
Purity: 99.9%



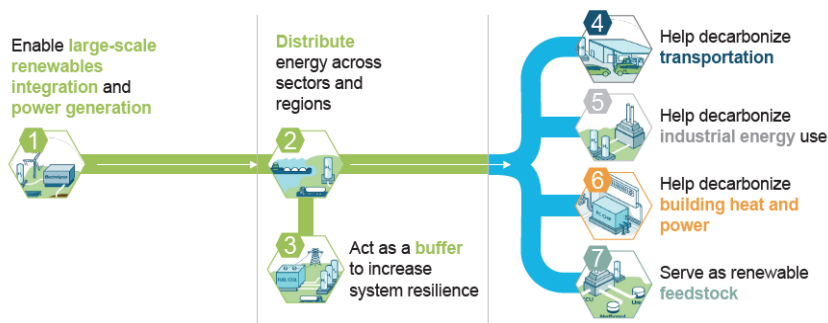




# Hydrogen market vision

- Hydrogen can link different energy sectors and energy transmission and distribution networks,
- It is a flexible energy carrier that can be produced from any regionally-prevalent primary energy source.
- It can be effectively transformed into any form of energy for diverse end-use applications
- Hydrogen has been identified as a central pillar of the required energy transition [1].

Enable the renewable energy system → Decarbonize end uses

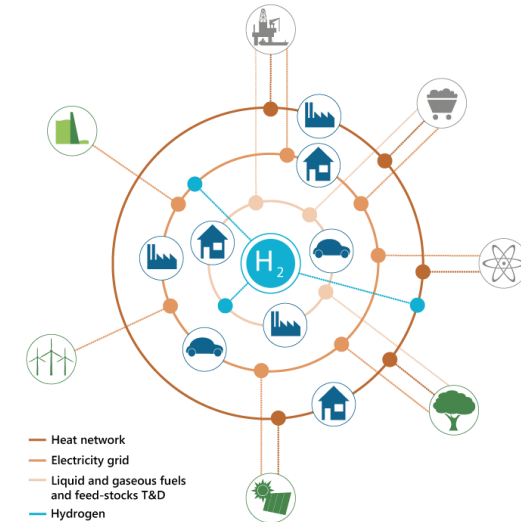


[1] Hydrogen scaling up (Hydrogen Council, 2016)

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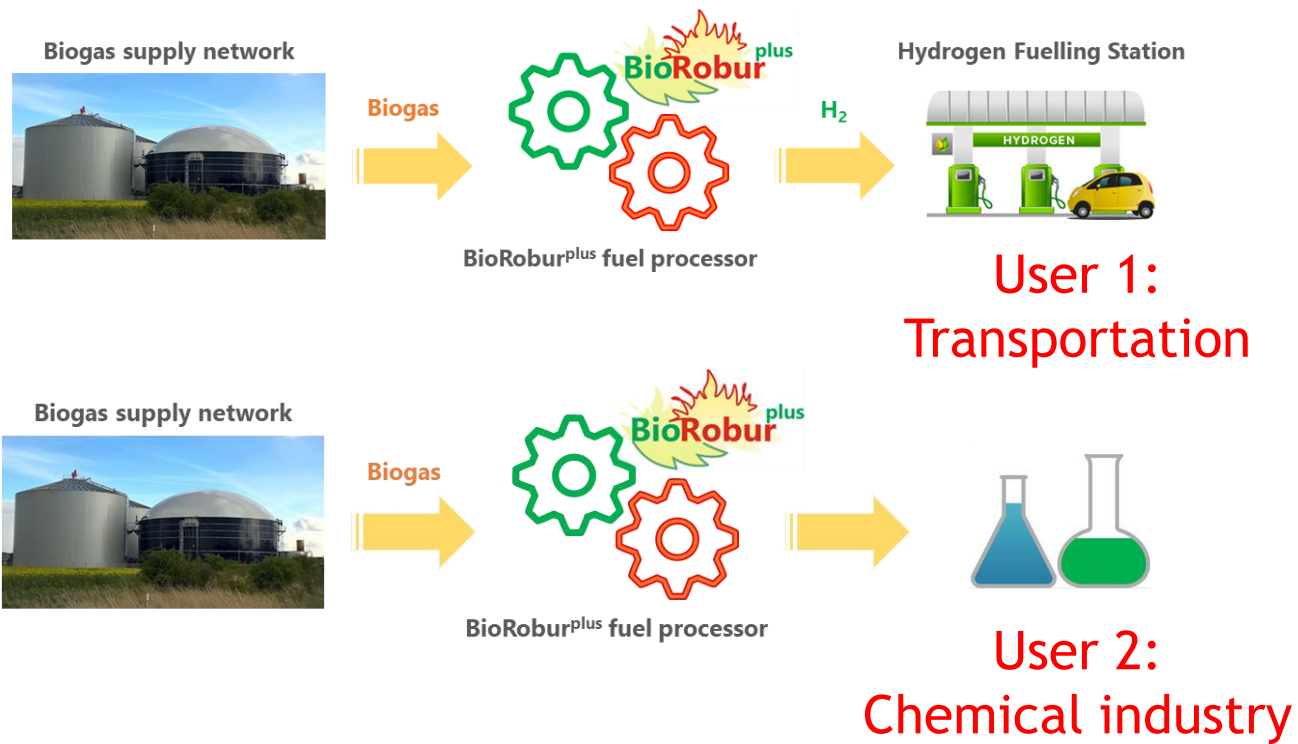


H<sub>2</sub> has a portfolio end-uses.



Hydrogen vision for 2050 [1].

# Distributed Hydrogen Production



✓ H<sub>2</sub> cost at different sizes application

# Economic feasibility of the process

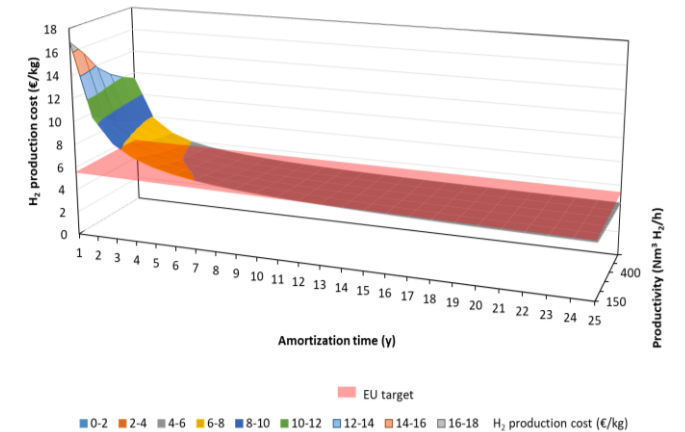
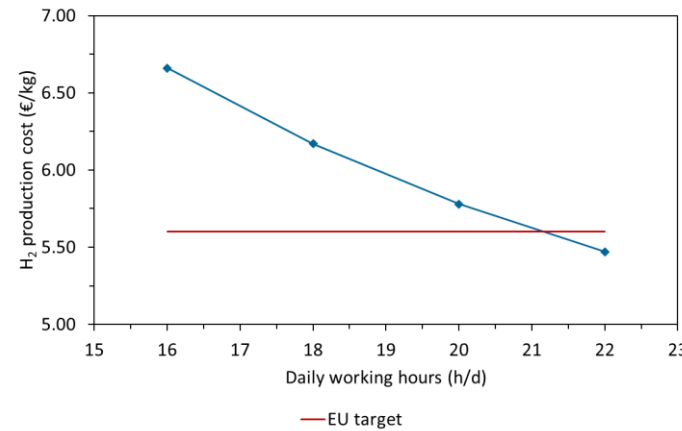
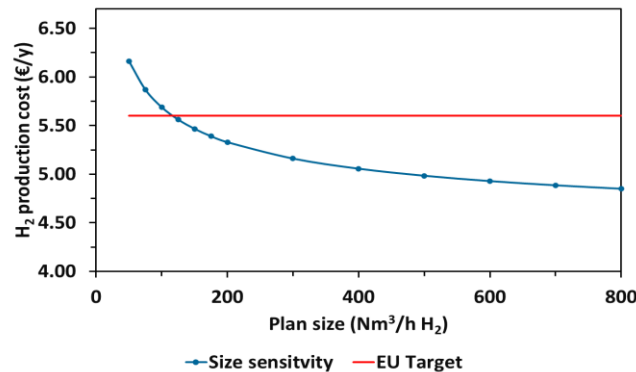
Proof of concept:  
Prototype case (50 Nm<sup>3</sup> H<sub>2</sub>/h)

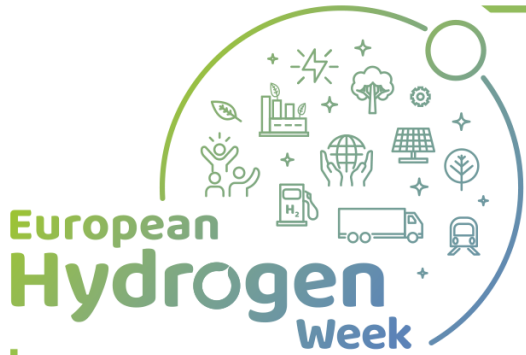
CAPEX	OPEX	H <sub>2</sub> cost
700 k€	150 k€/y	6.16 €/kg

EU target:  
5.6 €/kg H<sub>2</sub>



## Sensitivities

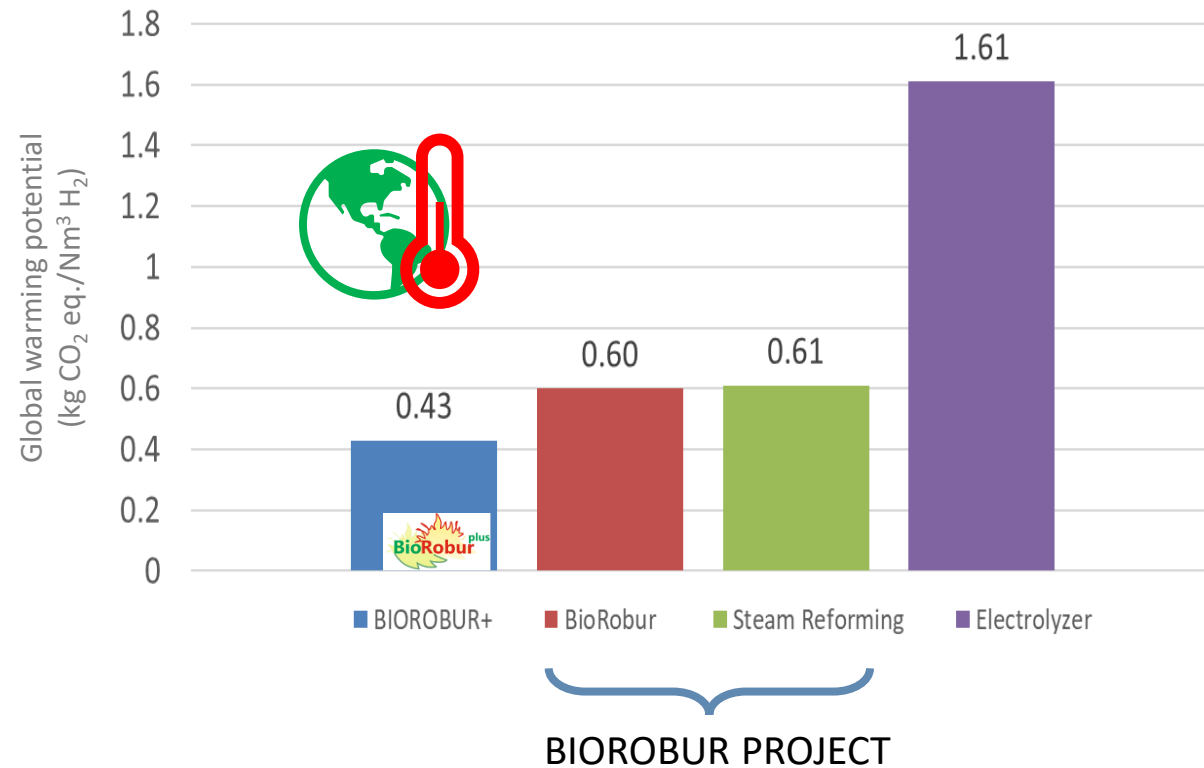




# Environmental feasibility of the process

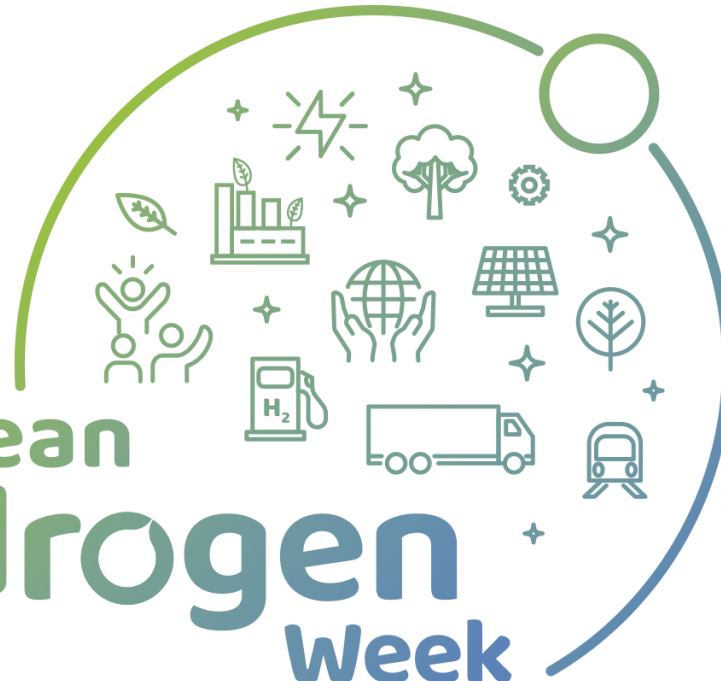
Life Cycle Assessment

Lower impact than previous innovative actions



F. Battista, Y.S. Montenegro Camacho, S. Hernández, S. Bensaid, A. Herrmann, H. Krause, D. Trimis, D. Fino, LCA evaluation for the hydrogen production from biogas through the innovative BioRobur project concept, International Journal of Hydrogen Energy, Volume 42, Issue 19, 2017.

# European Hydrogen Week



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