OxiGEN Next-generation Solid Oxide Fuel Cell stack and hot box solution for small stationary applications





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## **Project Overview**

- Call year: 2017
- Call topic: H2020-JTI-FCH-2017-1
  - Development of fuel cell system technologies
- Project dates: Jan 2018- Sept 2021
- % stage of implementation 01/11/2021: 100%
- Total project budget: 2,996,873.75 €
- FCH JU max. contribution: 2,996,873.75 €
- Other financial contribution: 0







European

Commissio



#PRD2021 #CleanHydrogen

2021 ogen

European Commission





### Hotbox: definition

Achievement to-date

25%

**75**%

engic

00%

#### Hotbox Simulation Results Single Family Houses

- Power output of 0.6 kW can fit all countries (0.5 for Italy)
- High power efficiency minimizes on/off cycles
- For most countries, a maximum of stack related CAPEX of 4000€/kW is compulsory, assuming 10 years lifespan

#### Multi Family Houses

- SOFC can be operated all year long
- Power output of 2 kW can fit all countries
- This market seems easier to address, from a cost point of view.

#### Commercial sector

- Retail, offices and education are tricky regarding on/off cycles limitations of SOFC
- Health and Hotels sectors appears attractive with 5 kW and 50% eff.



50%









0.4

0,3

0,2

0.1

Reference electrolyte

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Commission

Innovative electrolyte





# Material Development: integration into short stacks



#### **Short Stack Testing**

- OCV: Innovative materials are compatible with scaling the co-sintering process to full stack cross section
- Efficiency: 50% in simulated reformate, 65% Fuel Utilization @300 mA/cm<sup>2</sup>
- **Output:** verifies 650W achievable for full stack
- Resistance, Ohmic shows expected reduction
- **Resistance, Polarization** potential for further performance increase, did not have time to optimize the microstructure in this project

Average per cell	Rs (Ω.cm²)	Rp (Ω.cm²)
GEN1.1 – Wet H <sub>2</sub> /N <sub>2</sub> - CEA	0.22	1.77
GEN1.3 – Wet H <sub>2</sub> /N <sub>2</sub> - CEA	0.36	2.52
GEN3 – Dry H <sub>2</sub> /N <sub>2</sub> - CEA	0.06-0.08*	2.07-2.09











#### **Durability**

- 2900 hrs tested in steady state operation
- Multiple gas and current conditions probed
- Using simulated reformate and 30% Uf, degradation measured as -0.36 %/1000 hrs per cell







## **Exploitation Plan/Expected Impact**

#### **Exploitation**

	Planned results in the initial proposal	Partner owner
1	Hot box specifications, in particular regarding size and operation mode	Engie
2	New stack design for improved interface with hot box allowing extended lifetime	Saint-Gobain
3	Scale-up of new materials (anode functional layer and electrolyte) into short stack	Saint-Gobain,
		Eifer, SINTEF
4	Hot box for Saint-Gobain stack	IKTS
5	Testing results of stack/hot box combination under application specific conditions	CEA, IKTS, ICI
6	SOFC system setup & operation strategy	ICI
7	Methodology to determine total cost of ownership	Saint-Gobain
	Novel electrolyte composition with improved conductivity and stability than YSZ	SINTEF, Saint-
•		Gobain
9	New anode functional layer composition, resistant to power loss after emergency	Saint-Gobain,
	shutdown (redox)	Eifer



#### **Impact**

**Stack performance** in commercially relevant assembly (note : not individual cell performance): DC efficiency of at least 55%, for example by achieving voltage 0.83 V/cell at current density 0.30 A/cm2 under reformed natural gas and air. Operating conditions : air utilization >35% and fuel utilization >65%

Lifetime > 90 000 hours (defined as accumulated performance loss reaching 20%):

- Steady state degradation rate <0.1% per thousand hours, proven over a test duration of at least 5000 hours
- Resistance to normal cycling : <0.01% per cycle (controlled shut-down with stack brought to T<125°C) proven over at least 50 cycles
- Resistance to emergency shut-down : <0.25% per cycle (redox cycle such as fuel loss at operational temperature, specific to the system outlay) proven over at least 10 cycles

**Stack Cost:** below 1000  $\notin$  kWe ultimately, as manufactured in a production plant with a capacity of > 50 MWe/y. This stack cost includes not only the cells but also the gas manifold, current collectors, compression systems, and potentially insulations and heat exchangers depending on the design







## Risks, Challenges and Lessons Learned

Non-technical learnings

- Project segmentation allowed quick progress along many fronts
- Open communication with a high frequency was critical to move the project forward and solve issues
- Full team 'on-site' meetings kept work packages aligned, virtual meetings not as successful
- Stability (in testing infrastructure, personnel, and production) is an important factor to success

#### Technical learnings

- The optimal hotbox size is strongly correlated to required system shut downs.
- A unique hotbox was designed to optimize thermal, gas, and electrical controls
- Innovative material sets were incorporated into button cells and then demonstrated at the short stack scale







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