

CHANNEL

Development of the most cost-efficient hydrogen production unit based on anion exchange membrane electrolysis

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RESEARCH DAYS

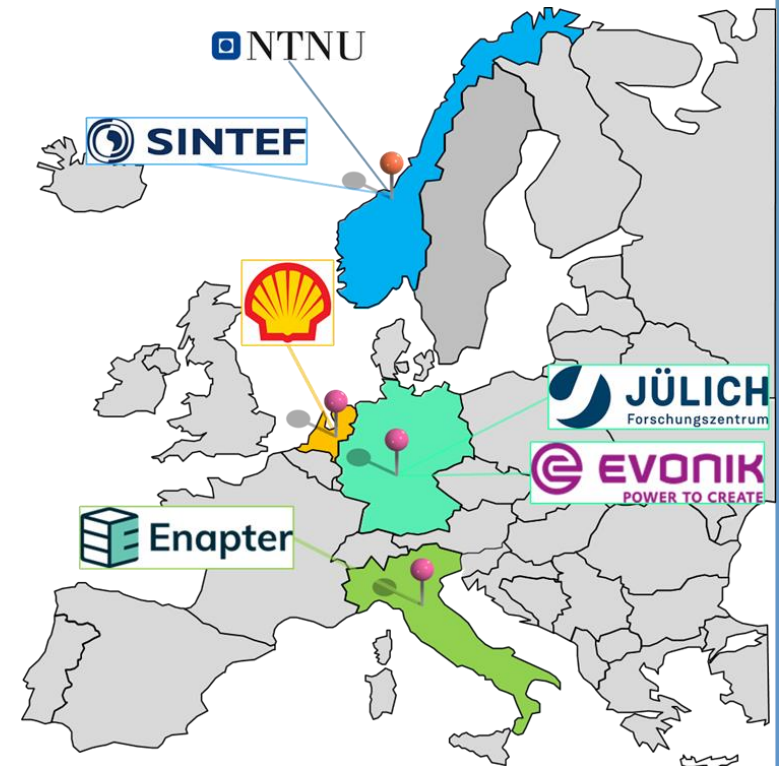
15-16 NOVEMBER



Co-funded by
the European Union

Project Overview

- Call year: 2019
- Call topic: FCH-02-4-2019: New Anion Exchange Membrane Electrolyzers
- Project dates: 01.2020 - 30.2023
- Total project budget: 1 999 906,25 €
- Clean Hydrogen Partnership max. contribution: 1 999 906,25 €
- Partners: SINTEF; NTNU; FZJ; SHELL; EVONIK; ENAPTER



Project Objectives

Starting point

- SoA AEM membranes and ionomers



- SoA non-PGM HER and OER catalysts

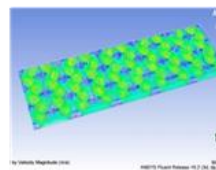
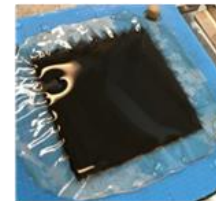
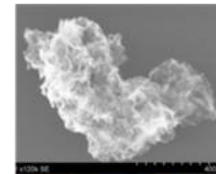
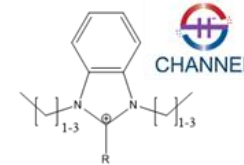


- SoA electrolyser designs, components and AEM systems



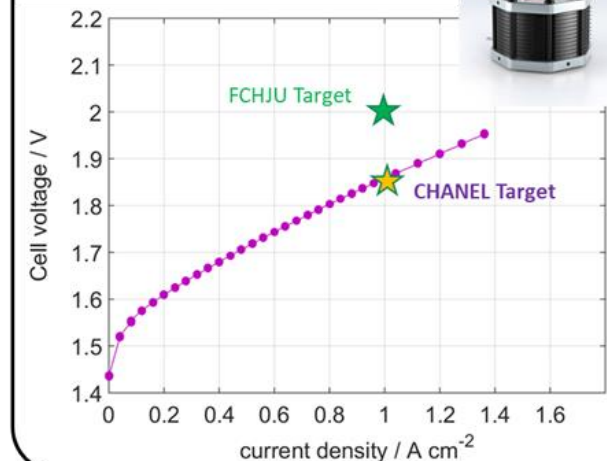
Concepts developed within CHANNEL

- Optimisation cQA-PAEK based polymers structural parameters, e.g. MW, block-co-polymer ratios, thickness.
- Optimisation of Ni-based catalysts, NiMo, NiFe by surface stabilisation, shape control and study of catalyst ionomer interactions.
- Electrode optimisation (ionomer and catalyst type and loadings), different coating methods and different MEA approaches guided by electrochemical AEM modelling
- New AEM advanced pressurised electrolyser design, low-cost PTLs, assisted by CFD flow simulations in porous media.

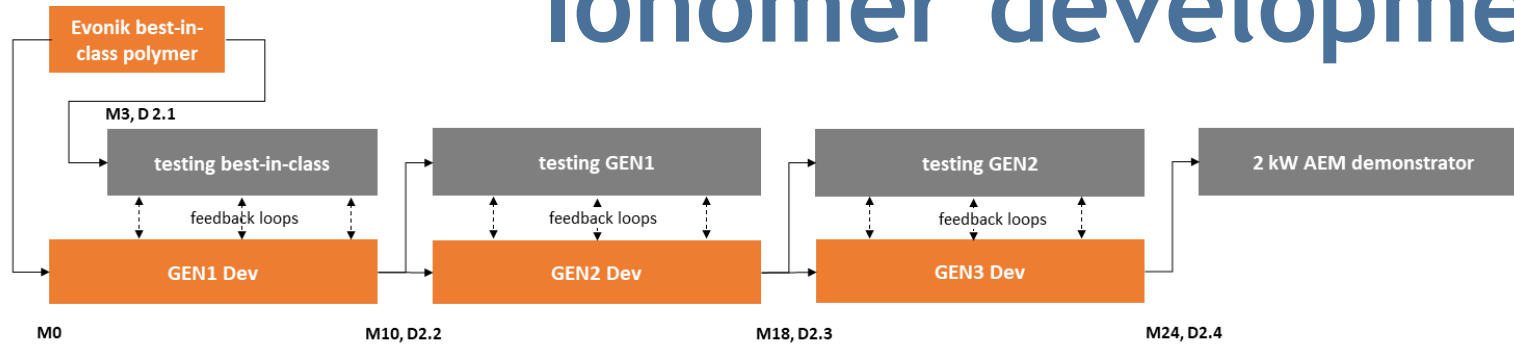


Outcome

- Beyond SoA 30 bar 2kW AEM electrolyser with performance of 1.85 V @ 1 A cm⁻² in diluted electrolyte
- 2000 h operation < 50 mV degradation
- <600 EUR/kW



Project results - Membrane and Ionomer development



KPI	UNIT	OBJECTIVE	
		FCHJU 2.4-2019	CHANNEL
Area specific resistance ASR, T = RT	Ωcm^2	< 0,07	< 0,06
OH conductivity, T = RT	mS/cm	50	> 50
OH conductivity, T = 60°C	mS/cm	not specified	> 90
Ex-situ stability (AST protocol, 1 M KOH, T = 60 °C, 600 hr)	mS/cm	not specified	> 80
hydrogen crossover (T = 60°C)	$[\text{mol}/\text{m}\cdot\text{s}\cdot\text{Pa}]\times 10^{-15}$	not specified	< 15
water uptake, T = RT	w-%	not specified	< 10
Dry/wet swelling machine Direction (MD)	%	< 1	< 1
Dry/wet swelling traverse Direction (TD)	%	< 4	< 4
Mechanical strength (in dry conditions, T = RT, RH = 50%)	MPa	15	15
Elongation at break (in dry conditions, T = RT, RH = 50%)	%	100	100
Mechanical strength (DMTA, in fully hydrated, swollen conditions, T = 30°C)	MPa	not specified	> 0,1
Mechanical strength (DMTA, in fully hydrated, swollen conditions, T = 60°C)	MPa	not specified	> 0,1
ionomer OH conductivity, T = 60°C	mS/cm	20	> 60
In-situ stability ASR remains	h	2000	> 5000

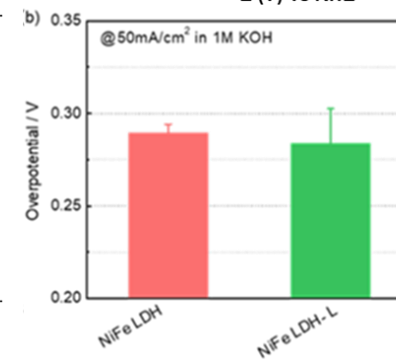
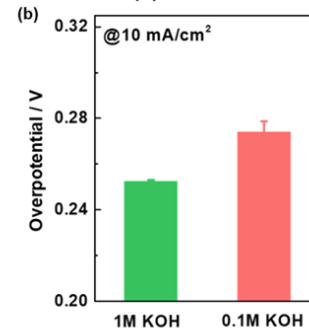
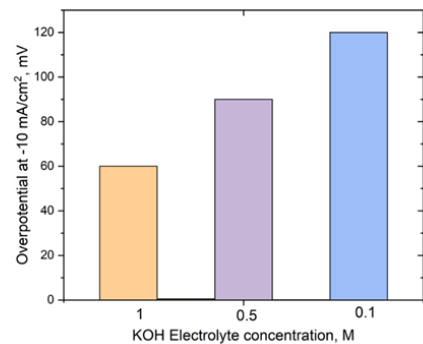
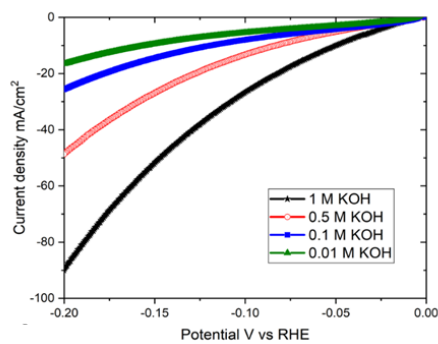
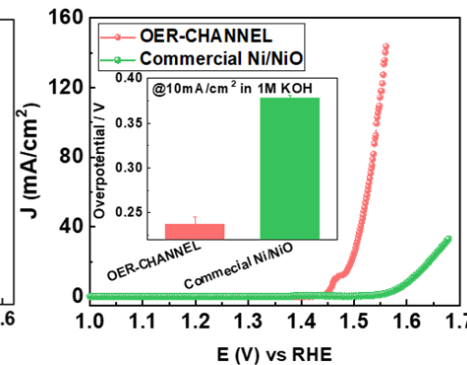
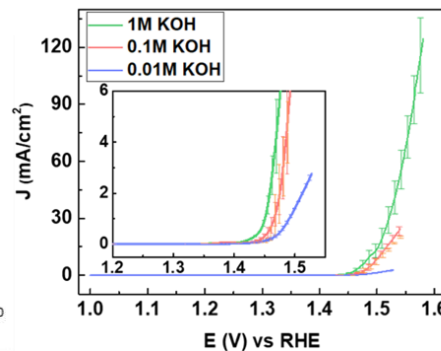
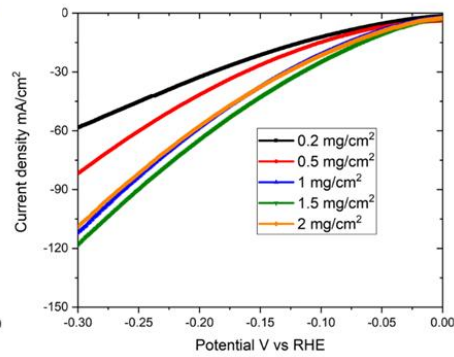
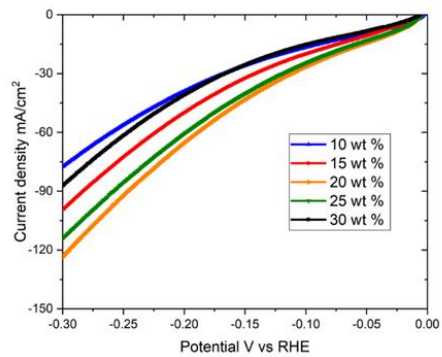
To Take Away:

1. AEM is good enough in terms of their KPIs, however, the question is related to their durability.
2. A better understanding of the in-operando membrane degradation mechanics is needed.
3. Thinner AEM can be manufactured, but questions concerning gas crossover, mechanical strength, and durability should be addressed properly.

Project results - HER/OER Catalysts

CHANNEL Catalysts Target at 10 mA·cm⁻²:

- **HER**: <150 mV overpotential and **OER**: <300 mV overpotential
- Both catalysts achieved performance and stability targets at 1M KOH besides to be scalable



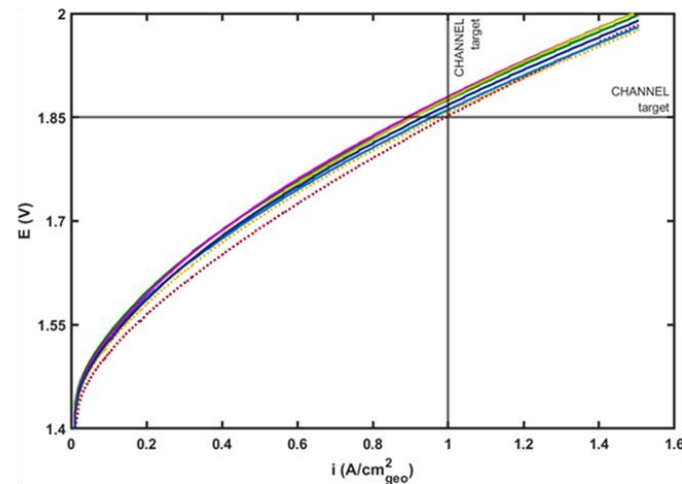
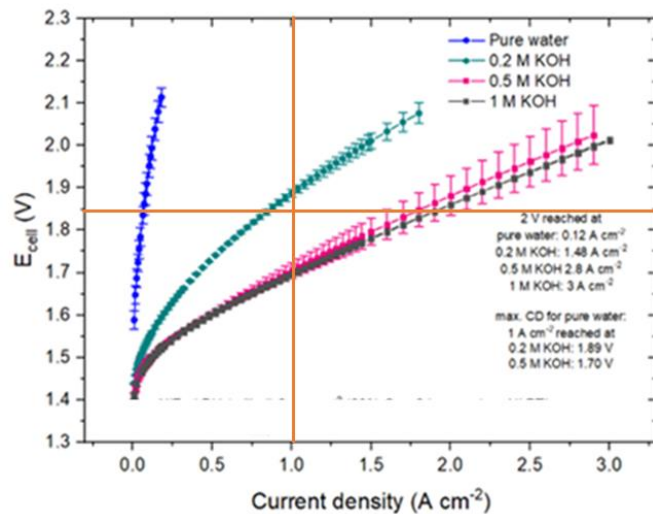
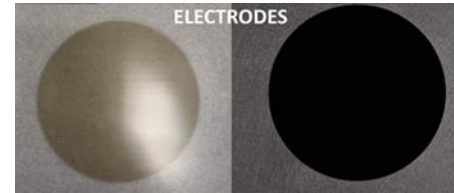
To Take Away:

1. A better understanding of the ionomer role and optimal ratio AEI-catalyst is needed as a function of the hydroxide concentration.
2. For PGM/CRM-free catalysts, the catalyst utilization would be more relevant than mass activity (cost-related), however high catalyst loading (thick electrodes) to compensate for lower mass activity (low-cost catalyst) needs to be carefully tuned to minimize mass transport constraints.
3. The development of in-situ methods for a better understanding of the catalyst activity and stability is recommended.

Project results - Single Cell Performance

CHANNEL Target: 1.85 V at 1 A/cm², 60°C, 1M KOH

Components long-term stability demonstrated over 1000 h

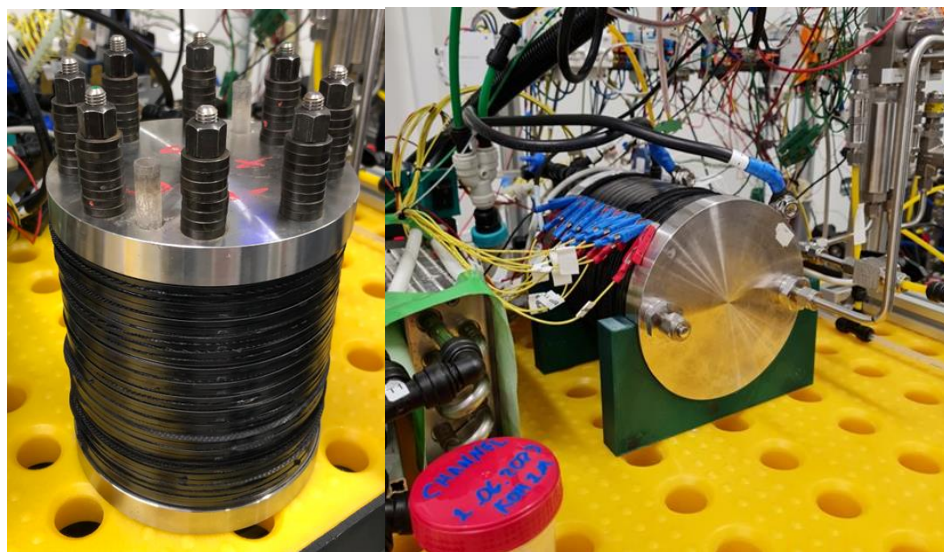


To Take Away:

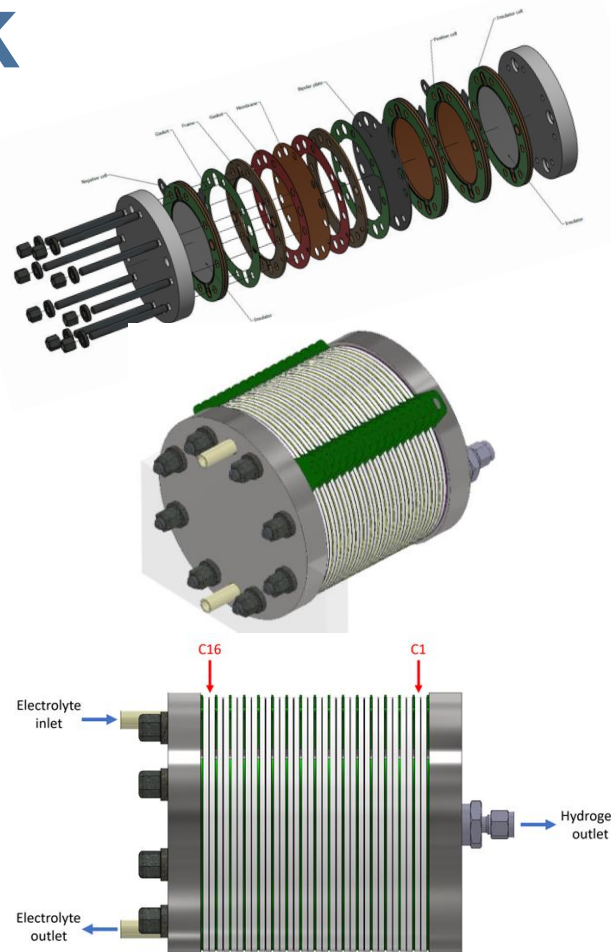
1. The electrode performance is quite sensitive to the ionomer content in the catalyst layer.
2. Crucial to understand the role of the AEI within the catalytic layer.
3. The electrodes to be used must be also optimized for the chosen KOH concentration since the optimal ratio AEI to catalyst may vary as a function of the hydroxide concentration.
4. The binding properties of the AEI must be considered as well.

- Developing a AEMWE model to predict local effects (e.g. pH change, water concentration gradients, etc.), degradation (cat's dissolution)

Project results - 2 kW Stack



16 cells with active area of 64 cm^2
BoP for stack testing was also designed and optimized



To Take Away:

1. CHANNEL stack demonstrator was validated over 260 h at atmospheric pressure, 0.25 A/cm^2 and $55 \text{ }^\circ\text{C}$ resulting in a degradation rate of $38 \mu\text{V/h}$.
2. Unfortunately, the performances expected for the stack were not fully reached at the end of the project.
3. Components dimensioning and manufacturing, methodology transferring from lab scale to stack level, and design/engineering of the final prototype is not a simple task to commit.

Project results - Dissemination

ACS APPLIED ENERGY MATERIALS

www.acsaem.org

Tuning Ni–MoO₂ Catalyst–Ionomer and Electrolyte Interaction for Water Electrolyzers with Anion Exchange Membranes

Alaa Y. Faid,^{*} Alejandro Oyarce Barnett, Frode Seland, and Svein Sunde

Cite This: ACS Appl. Energy Mater. 2021, 4, 3327–3340

Read Online

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Research Article | Open Access

The Influence of Loadings and Substrates on the Performance of Nickel-Based Catalysts for the Oxygen Evolution Reaction

Wulyu jiang, Prof. Dr. Werner Lehnert, Dr. Meital Shviro

First published: 02 January 2023 | <https://doi.org/10.1002/celc.202200991>

International Journal of Hydrogen Energy

Volume 47, Issue 56, 1 July 2022, Pages 23483–23497

Ternary NiCoFe nanosheets for oxygen evolution in anion exchange membrane water electrolysis

Alaa Y. Faid^a, Alejandro Oyarce Barnett^b, Frode Seland^a, Svein Sunde^a

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Research Article | Open Access

Composition-Dependent Morphology, Structure, and Catalytical Performance of Nickel–Iron Layered Double Hydroxide as Highly-Efficient and Stable Anode Catalyst in Anion Exchange Membrane Water Electrolysis

Wulyu Jiang, Alaa Y. Faid, Bruna Ferreira Gomes, Irina Galkina, Lu Xia, Carlos Manuel Silva Lobo, Morgane Desmau, Patrick Borowski, Heinrich Hartmann, Artjom Maljus, Astrid Besmehn, Christina Roth, Svein Sunde, Werner Lehnert, Meital Shviro ... See fewer authors

First published: 13 July 2022 | <https://doi.org/10.1002/adfm.202203520> | Citations: 8

Journal of Applied Electrochemistry (2022) 52:1819–1826

Unveiling hydrogen evolution dependence on KOH concentration for polycrystalline and nanostructured nickel-based catalysts

Alaa Y. Faid¹ · Farnak Foroughi^{1,2} · Svein Sunde¹ · Bruno Pollet^{2,3}

Received: 4 April 2022 / Accepted: 14 August 2022 / Published online: 2 September 2022

- The results haven presented in 10 conferences
- A patent application has been submitted
- Creation of the AEM Hub for promoting the AEM technology in cooperation with the other EU granted AEMWE projects (NEWELY and ANIONE)

- Two more manuscripts under revision

Project - Summary

- ✓ CHANNEL successfully developed alternative low-cost non-PGM catalysts exhibiting excellent performance and durability. *A patent application on cathode catalyst was submitted by NTNU.*
- ✓ The project achieved a good generation of anion exchange membranes and ionomers with excellent chemical and mechanical properties.
- ✓ The optimized membrane and electrodes allowed to reach a full non-PGM single-cell performance target of <1.85 V at 1 A/cm² with a good stability after 1000 h (@1A/cm²) long-term test.
- ✓ Due to the low TRL of the stack prototype, manufacturing strategies, and cost forecast for a 500kW system were calculated based on estimations of the stack manufacturer.

Acknowledgements

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Thank you for your attention



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