

//EU HYDROGEN  
RESEARCH DAYS  
15-16 NOVEMBER

# ANIONE

## Anion Exchange Membrane Electrolysis for Renewable Hydrogen Production on a Wide-Scale

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the European Union

# Project Overview

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- Call year: **2019**
- Call topic: **FCH-02-4-2019 New Anion Exchange Membrane Electrolysers**
- Project dates: **01-01-2020 - 30-09-2023**
- % stage of implementation 01/11/2023: **100%**
- Total project budget: **1 999 995.00 €**
- Clean Hydrogen Partnership max. contribution: **1 999 995.00 €**
- Other financial contribution: **0 €**
- Partners: CNR-ITAE, CNRS, HYDROLITE (formerly POCELLTECH), TFP (formerly PV3), IRD, CUMMINS (formerly HYDROGENICS), UNIRESEARCH BV



# Project Summary

## ➤ *Overall objective:*

- ✓ Develop **high-performance** (energy consumption  $< 50$  kWh/kg H<sub>2</sub>), **cost-effective** (0.75 M€ / t/d H<sub>2</sub>) and **durable** (degradation  $< 5$  μV/h at 1 A cm<sup>-2</sup>) **anion exchange membrane water electrolysis technology**.

## ➤ *Approach:*

- ✓ Advanced **CRM-free electrocatalysts**, **hydrocarbon anion exchange membrane (AEM)** and ionomer dispersion in the catalytic layers for hydroxide ion conduction in a **system operating with diluted KOH**.
- ✓ ANIONE has validated, as **proof-of-concept**, a **2 kW AEM electrolyser** with a hydrogen production rate of approximately **0.4 Nm<sup>3</sup> H<sub>2</sub>/h**.

## ➤ *Goal:*

- ✓ Allow a **scalable production of low-cost hydrogen** from renewable sources through a **reduction of capital costs**, while assuring **high conversion efficiency** and proper **life-time**.

# Project Focus on AEM

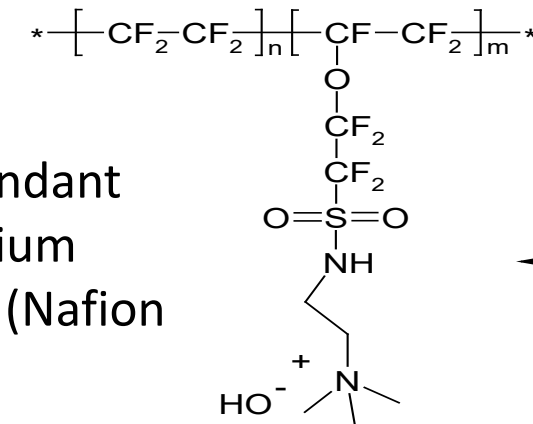
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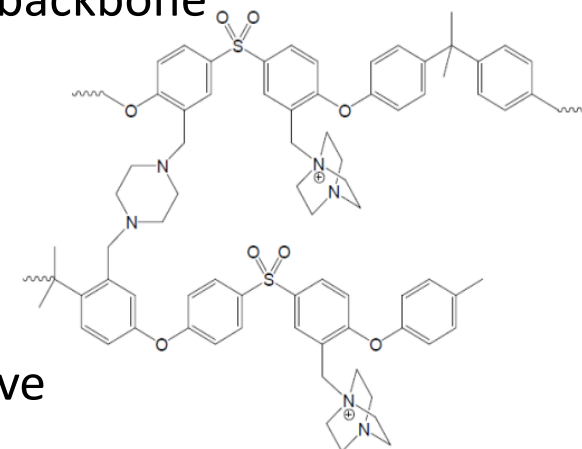
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Parallel approaches for the anion exchange membrane:



- ✓ Short side chain **perfluorinated AEM** comprising a perfluorinated backbone and pendant chains, covalently bonded to the perfluorinated backbone, with quaternary ammonium groups to achieve conductivity and stability comparable to their protonic analogous (Nafion®)
- ✓ **Hydrocarbon AEM membranes** consisting of either poly(arylene) or poly(olefin) backbone with quaternary ammonium hydroxide groups carried on tethers anchored on the polymeric backbone
- ✓ **Modified hydrocarbon membranes and ionomers based on DABCO** (1,4-diazabicyclo[2.2.2]octane  $N_2(C_2H_4)_3$ ) cross-linked poly(sulfone) resins as alternative membranes (back-up solution).



Tal-Gutelmacher et al., *Membranes* 2021, 11, 686

Carbone et al. *Chemical Engineering Journal* (2022) 140765



# Project Progress/Actions: Cell performance and faradaic efficiency

Project start value

Project target value

Achievement to-date

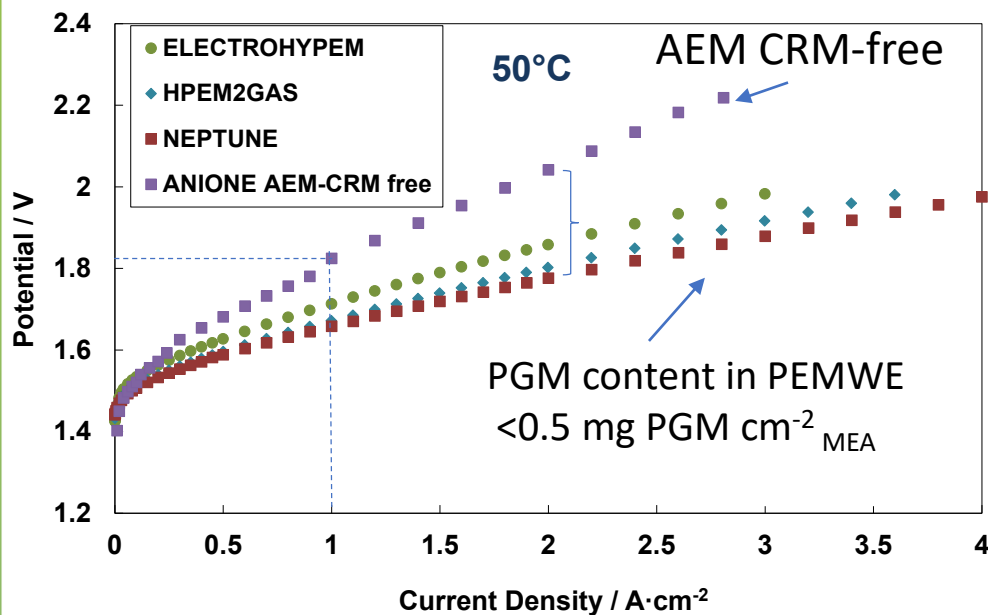
0.3 A cm<sup>-2</sup> at  
1.8 V /cell

1 A cm<sup>-2</sup> at  
~1.8 V /cell  
99% faradaic  
efficiency

25%

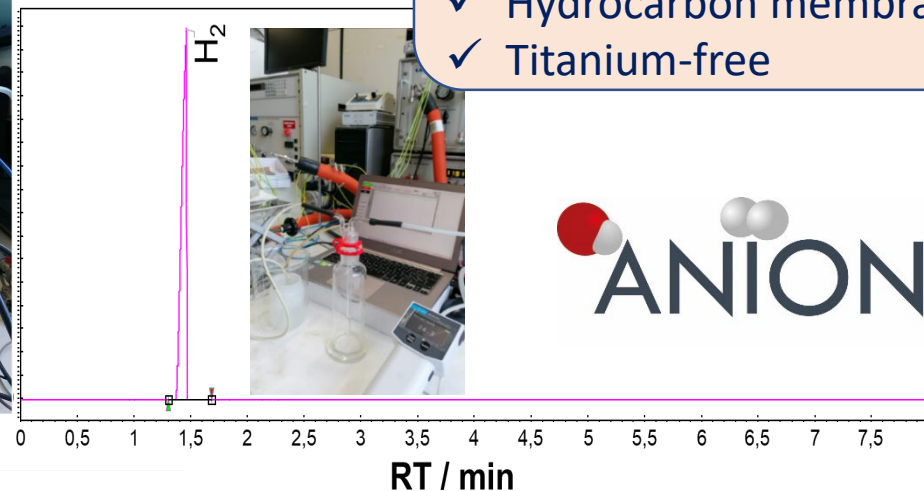
50%

75%



Zignani et al. *Electrochim. Acta* 413 (2022) 140078

AEM ELECTROLYSIS single cell testing in ANIONE



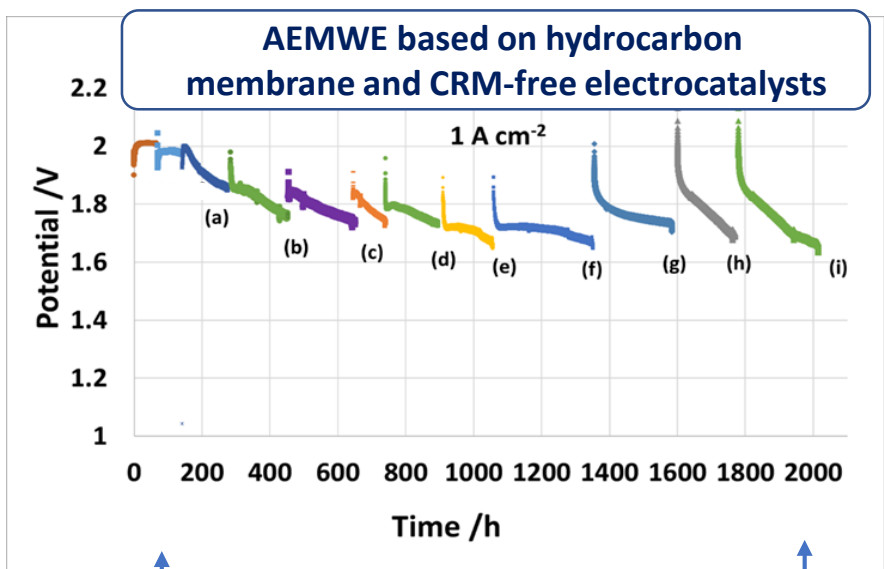
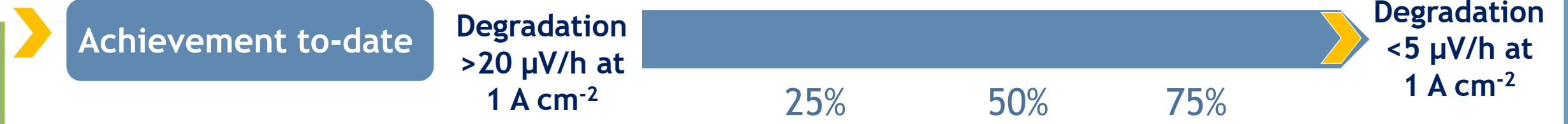
- ANIONE AEM technology:
- ✓ Non-PGM electrocatalysts
  - ✓ CRM-free materials,
  - ✓ Hydrocarbon membrane
  - ✓ Titanium-free



# Project Progress/Actions: Cell performance and faradaic efficiency

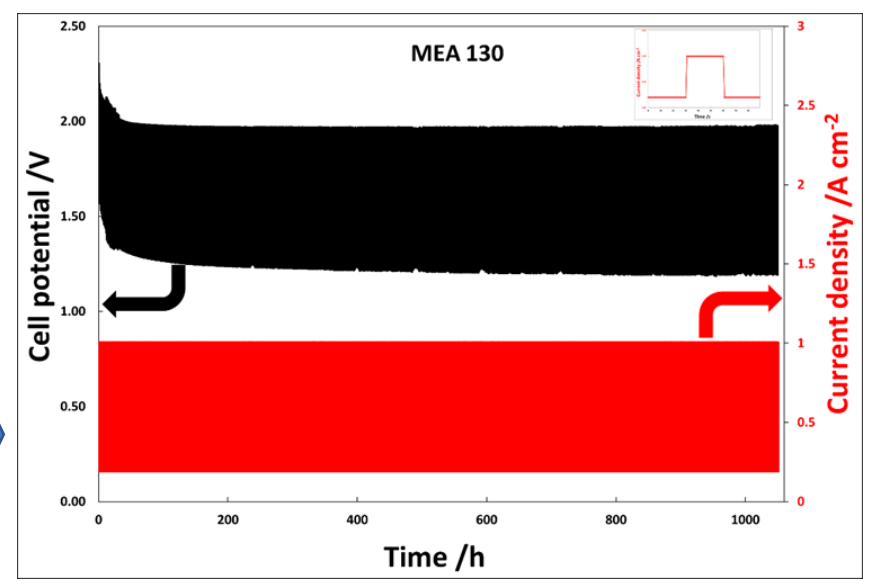
Project start value

Project target value



Steady-state operation at  $1 \text{ A cm}^{-2}$

Reversible losses recorded during shut down and start-up cycles



Cycled operation Step cycles between  $0.2$  and  $1 \text{ A cm}^{-2}$

Faradaic efficiency >99%

Faradaic efficiency >96%

Zignani et al. Electrochim. Acta 413 (2022) 140078



# Project Progress/Actions: MEA scaling-up and stack engineering

Project start value

Project target value

Achievement to-date

Small 5 cm<sup>2</sup>  
Single cell

~2 kW stack  
~0.4 Nm<sup>3</sup> H<sub>2</sub>/h

25%

50%

75%

Compact stack configuration: 10 cells of 100 cm<sup>2</sup> operating at 1 A cm<sup>-2</sup>, 50°C and pressurised mode

27 wet membranes for stack assembly



25 Anodes: NiFe uniformly coated on 1 side

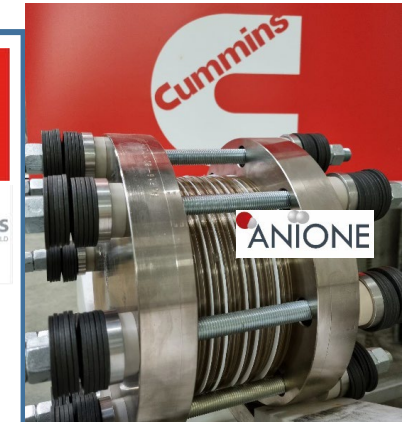
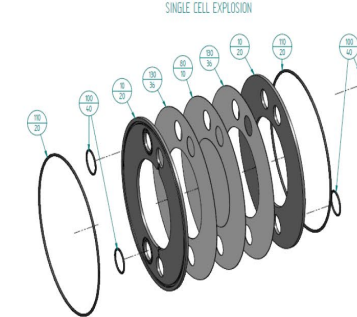
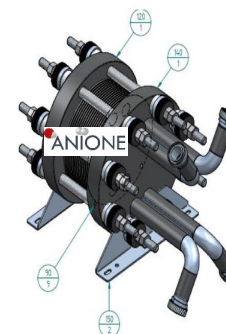
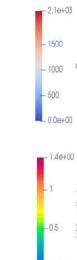
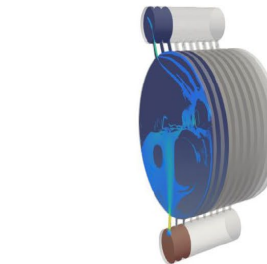


Anode 2.5 mg<sub>NiFe</sub>/cm<sup>2</sup> on densified Ni-felt GDE



Cathode 5 mg<sub>CoMo</sub>/cm<sup>2</sup> on SGL GDE

- Computational Fluid Dynamics
  - Pressure drop
  - Porous properties
  - Flow
- Full stack assembly
  - MEA received
  - Pressure drop to be measured
  - Leak & pressure test
    - External (Hydrostatic)
    - Internal (N<sub>2</sub>)
    - Short stack



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# Project Progress/Actions: Stack testing

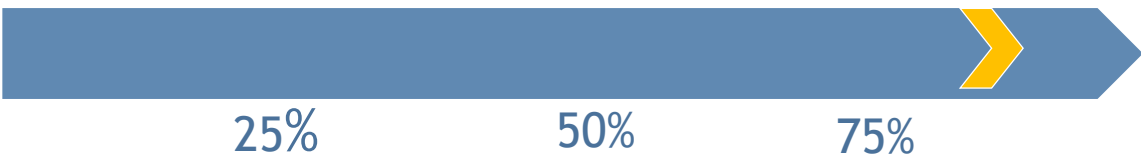


Project start value

Project target value

Efficiency <60%  
@1 A cm<sup>-2</sup>

~2 kW stack  
~70% efficiency  
@1 A cm<sup>-2</sup>

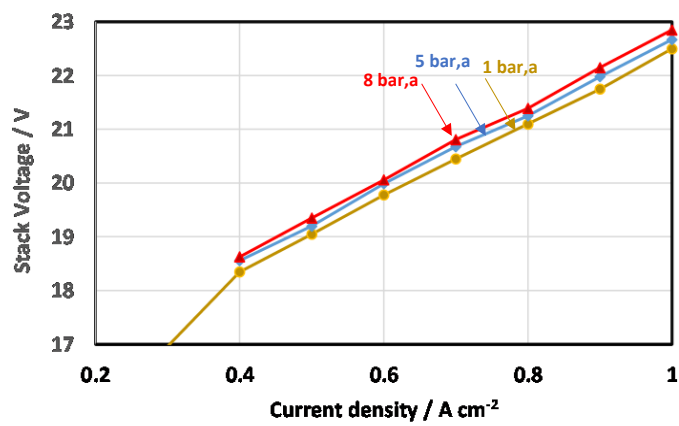


Achievement to-date



Differential pressure  
Horizontal Stack, anode feed 1 M KOH, flow 0.5 l/min

Parameter	Result	Target
Stack Performance	21 V for the stack (i.e. ~2.1 V/cell) at 1 A cm <sup>-2</sup> (100 A) at ~ 50 °C with recirculation rate of 1M KOH 1.25 ml/min/cm <sup>2</sup>	1.8-2 V/cell at 1 A cm <sup>-2</sup> -MS10
Voltage efficiency	71% vs. HHV at 1 A cm <sup>-2</sup> (100 A) at temperatures up to 50 °C with recirculation rate of 1M KOH 1.25 ml/min/cm <sup>2</sup>	86% vs. HHV -MS10
Stack Capacity	0.398 ± 0.005 Nm <sup>3</sup> /h at 1 A cm <sup>-2</sup> (100 A)	Hydrogen production rate > 0.4 Nm <sup>3</sup> /h -MS10
Faradaic efficiency	97 % at 1 A cm <sup>-2</sup> (100 A)	>99 % at 1 A cm <sup>-2</sup> -MS7
Stack Energy efficiency	69 % vs HHV	80 % vs HHV -MS11
Stack energy consumption of about 57 kWh/kg H <sub>2</sub>	57 kWh/kg H <sub>2</sub>	50 kWh/kg H <sub>2</sub> -MS11
Stack power	>2 kW	2 kW (10-cells with 100 cm <sup>2</sup> active area) -MS10





# Risks, Challenges and Lessons Learned

- **Gas cross-over management for thin anionic membranes in the presence of high differential pressure.**
  - ✓ *Mitigation strategies: membrane and MEA engineering to include a recombination catalyst integrated in the anode layer and membrane reinforcement increasing the tortuosity path for gas permeation.*
- **Demonstrating the capability of advanced membrane-electrode assemblies and related components to operate in a wider operating temperature and pressure ranges.**
  - ✓ *MEA performance and durability has been assessed at 50°C and moderate pressures (<20 bar). Operation above 50°C has been demonstrated ; however it may compromise stability of AEM ionomers; performance targets have been already achieved at 50°C.*

# Synergies With Other Projects And Programmes

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The AEM-HUB  
webpage is available  
via each of the [project  
websites](#).

- Activities with Project Group:
  - Visual identity → logo + colour scheme
  - AEM Hub [Webpage](#)
  - [Flyer](#)
  - [Video](#)
  - Joint webinar (July 2021, March 2023, Sept. 2023)
    - Latest development in AEM field
    - Definition of common vocabulary for the field
    - Possible interactions with industry on technology adaptation and future partnerships
  - Harmonised MEA assessment in single cell (ANIONE, CHANNEL and NEWLY)



- Ongoing collaboration with other FCH JU AEM projects: NEWLY, CHANNEL
- Horizon Booster activities with Project Group:
  - Completed Module A - Identification of R&I results and creation of portfolio → [report available on METT](#)
  - April – Nov 2021: Module B - Portfolio dissemination plan and execution



AEM-HUB – Reshaping green hydrogen production



[www.anione.eu](http://www.anione.eu)

# Thank you for your kind attention!

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